

# Preliminary Feasibility Study & Technical Report Summary

## 5E Advanced Materials Fort Cady Project



**Report Date**  
August 7, 2025

**Report Effective Date**  
August 4, 2025

## List of Qualified Persons

	<b>Section(s)</b>	<b>Date</b>
Alan E. White, P. E., Miocene, Inc. /s/ Alan E. White	<b>12, 13 and 18</b> (18.1.5 through 18.1.8)	August 7, 2025
Kevin R. Martina, P.Eng., Fluor Corporation /s/ Kevin R. Martina	<b>10, 14 and 18</b> (18.1.1 through 18.1.4, 18.1.9 and 18.2)	August 7, 2025
Martin Roth, P.G., Geomega, Inc. /s/ Martin Roth	<b>7.3</b>	August 7, 2025
Steven Kerr, P.G., C.P.G., Principal, Escalante Geological Services, LLC /s/ Steven Kerr	<b>2, 3, 4, 5, 6, 7</b> (except 7.3), <b>8, 9, 11, 15, 17, 20, 21 and 22</b>	August 7, 2025
Paul Weibel, CPA, 5E Advanced Materials, Inc. /s/ Paul Weibel	<b>1, 16, 19, 23, 24 and 25</b>	August 7, 2025

## Table of Contents

<a href="#">List of Qualified Persons</a> .....	2
<a href="#">Table of Contents</a> .....	3
<a href="#">List of Figures</a> .....	7
<a href="#">List of Tables</a> .....	8
<a href="#">Glossary of Terms</a> .....	11
<a href="#">1 Executive Summary</a> .....	13
<a href="#">2 Introduction</a> .....	14
<a href="#">2.1 Registrant for Whom the Technical Report was Prepared</a> .....	14
<a href="#">2.2 Terms of Reference and Purpose of the Report</a> .....	14
<a href="#">2.3 Sources of Information</a> .....	14
<a href="#">2.4 Details of Inspection</a> .....	15
<a href="#">2.5 Report Version Update</a> .....	15
<a href="#">2.6 Units of Measure</a> .....	15
<a href="#">2.7 Mineral Resource and Mineral Reserve Definition</a> .....	15
<a href="#">2.7.1 Mineral Resources</a> .....	15
<a href="#">2.7.2 Mineral Reserves</a> .....	16
<a href="#">2.8 Qualified Persons</a> .....	16
<a href="#">3 Property Description and Location</a> .....	17
<a href="#">3.1 Property Location</a> .....	17
<a href="#">3.2 Area of Property</a> .....	17
<a href="#">3.3 Mineral Title</a> .....	18
<a href="#">3.4 Mineral Rights</a> .....	19
<a href="#">3.5 Incumbrances</a> .....	19
<a href="#">3.5.1 Remediation Liabilities</a> .....	19
<a href="#">3.6 Other Significant Risk Factors</a> .....	19
<a href="#">3.7 Royalties</a> .....	20
<a href="#">4 Accessibility, Climate, Local Resources, Infrastructure, and Physiography</a> .....	20
<a href="#">4.1 Topography, Elevation, and Vegetation</a> .....	20
<a href="#">4.2 Accessibility and Transportation to the Property</a> .....	20
<a href="#">4.3 Climate and Length of Operating Season</a> .....	20
<a href="#">4.4 Infrastructure Availability and Sources</a> .....	20
<a href="#">5 History</a> .....	21
<a href="#">5.1 Prior Ownership and Ownership Changes</a> .....	21
<a href="#">5.2 Exploration and Development Results of Previous Owners</a> .....	21
<a href="#">5.3 American Pacific Borates Share Exchange of Atlas Precious Metals</a> .....	22
<a href="#">5.4 Historic Production</a> .....	22
<a href="#">6 Geological Setting, Mineralization and Deposit</a> .....	26
<a href="#">6.1 Regional Setting</a> .....	26
<a href="#">6.1.1 Mineralization</a> .....	27
<a href="#">6.2 Mineral Deposit</a> .....	27
<a href="#">6.3 Stratigraphic Column</a> .....	28
<a href="#">7 Exploration</a> .....	29
<a href="#">7.1 Non-drilling exploration</a> .....	29
<a href="#">7.2 Drilling</a> .....	29

7.2.1	<a href="#">Historic Drilling</a>	29
7.2.2	<a href="#">Company Drilling</a>	31
7.3	<a href="#">Hydrogeology</a>	33
7.3.1	<a href="#">Hydraulic Setting</a>	33
7.3.2	<a href="#">Project Area Groundwater Levels</a>	34
7.3.3	<a href="#">Hydrogeology External to the Ore Block</a>	35
7.3.4	<a href="#">Formation Hydraulic Properties</a>	35
7.3.4.1	<a href="#">Duval 1980-1982</a>	35
7.3.4.2	<a href="#">In-Situ 1990</a>	36
7.3.4.3	<a href="#">Hydro-Engineering 1996</a>	36
7.3.4.4	<a href="#">Geomega 2023</a>	36
7.3.5	<a href="#">Water Quality Compliance Monitoring</a>	36
8	<a href="#">Sample Preparation, Analysis and Security</a>	37
8.1	<a href="#">Sampling Method and Approach</a>	37
8.2	<a href="#">Sample Preparation, Analysis and Security</a>	37
9	<a href="#">Data Verification</a>	44
9.1	<a href="#">Data Verification Procedures</a>	44
9.2	<a href="#">Data Limitations or Failures</a>	44
9.3	<a href="#">Data Adequacy</a>	44
10	<a href="#">Mineral Processing and Metallurgical Testing</a>	44
10.1	<a href="#">Metallurgical Testing</a>	44
10.2	<a href="#">Representative Samples</a>	45
10.3	<a href="#">Testing Laboratory</a>	45
10.4	<a href="#">Relevant Results</a>	45
10.4.1	<a href="#">Feedstock Assay Results</a>	45
10.4.2	<a href="#">PLS Characterization</a>	47
10.4.3	<a href="#">Crystallization Results</a>	49
10.4.4	<a href="#">Impurity Removal Test Results</a>	54
10.5	<a href="#">Adequacy of Data</a>	55
11	<a href="#">Mineral Resource Estimates</a>	55
11.1	<a href="#">Key Assumptions</a>	55
11.2	<a href="#">QP's Estimate of Resource</a>	56
11.2.1	<a href="#">Resource Database</a>	56
11.2.2	<a href="#">Geologic Model</a>	58
11.2.3	<a href="#">Grade Estimation &amp; Resource Classification</a>	58
11.3	<a href="#">Model Validation</a>	59
11.3.1	<a href="#">Density Measurements</a>	60
11.4	<a href="#">Cut-off Grade</a>	60
11.5	<a href="#">Mineral Resource Estimation</a>	62
11.6	<a href="#">Uncertainties</a>	66
11.7	<a href="#">Individual Grade for Each Commodity</a>	66
11.8	<a href="#">Disclose Required Future Work</a>	66
12	<a href="#">Mineral Reserve Estimates</a>	66
12.1	<a href="#">Conversion Assumptions, Parameters, and Methods</a>	66
12.2	<a href="#">Mineral Reserve Estimate</a>	67

12.3	<a href="#">Relevant Factors</a>	67
13	<a href="#">Mining Methods</a>	68
13.1	<a href="#">Geotechnical and Hydrological Model Contribution to Mine Design</a>	68
13.2	<a href="#">Artificial Lift</a>	69
13.3	<a href="#">Wellfield Operating Strategy</a>	70
14	<a href="#">Processing and Recovery Methods</a>	75
14.1	<a href="#">Processing Summary</a>	75
14.2	<a href="#">Processing Design Criteria / Usages</a>	77
14.2.1	<a href="#">Basis for Boric Acid (BA) Head Grade</a>	78
14.3	<a href="#">Work Breakdown Structure and Plant Layout</a>	78
14.4	<a href="#">Description of Processing Facilities</a>	83
14.5	<a href="#">Equipment Selection — Processing Facilities</a>	85
15	<a href="#">Infrastructure</a>	88
15.1	<a href="#">Access and Local Communities</a>	88
15.2	<a href="#">Site Facilities and Infrastructure</a>	90
15.3	<a href="#">Security</a>	90
15.4	<a href="#">Communications</a>	90
15.5	<a href="#">Logistics Requirements and Off-site Infrastructure</a>	90
15.5.1	<a href="#">Rail</a>	90
15.5.2	<a href="#">Port and Logistics</a>	90
15.5.3	<a href="#">Off-site storage and distribution</a>	90
16	<a href="#">Market Studies and Contracts</a>	91
16.1	<a href="#">General Market Overview</a>	91
16.2	<a href="#">Borates</a>	91
16.2.1	<a href="#">Market Overview</a>	91
16.2.2	<a href="#">Historical Pricing</a>	91
16.2.3	<a href="#">Market Balance</a>	93
16.2.4	<a href="#">Market Costs</a>	93
16.2.5	<a href="#">Boric Acid Market</a>	94
16.2.6	<a href="#">Boric Acid Specifications</a>	95
16.3	<a href="#">Calcium Chloride</a>	95
16.3.1	<a href="#">Market Overview</a>	95
16.3.2	<a href="#">Historical Pricing</a>	95
16.3.3	<a href="#">Market Balance</a>	95
16.3.4	<a href="#">Market Cost</a>	96
16.3.5	<a href="#">Calcium Chloride Market</a>	96
16.3.6	<a href="#">Calcium Chloride Specifications</a>	97
16.4	<a href="#">Gypsum</a>	97
16.4.1	<a href="#">Market Overview</a>	97
16.4.2	<a href="#">Historical Pricing</a>	97
16.4.3	<a href="#">Market Imbalance</a>	98
16.4.4	<a href="#">Market Costs</a>	98
16.4.5	<a href="#">Gypsum Market</a>	98
16.4.6	<a href="#">Gypsum Specifications</a>	99
16.5	<a href="#">Conclusions</a>	99

<a href="#"><u>16.6 Contracts</u></a>	100
<a href="#"><u>17 Environmental Studies, Permitting, and Closure</u></a>	100
<a href="#"><u>17.1 Environmental Requirements for Solution Mining</u></a>	100
<a href="#"><u>17.2 Environmental Study Results</u></a>	100
<a href="#"><u>17.3 Required Permits and Status</u></a>	100
<a href="#"><u>18 Capital and Operating Costs</u></a>	102
<a href="#"><u>18.1 Capital Cost Estimates</u></a>	102
<a href="#"><u>18.1.1 Capital Cost Estimate - Processing Facility and Infrastructure</u></a>	102
<a href="#"><u>18.1.2 Processing Facility and Infrastructure - Basis and Methodology</u></a>	103
<a href="#"><u>18.1.3 Capital Cost Estimate - Evaporative Ponds</u></a>	106
<a href="#"><u>18.1.4 Capital Cost Estimate - Cogeneration Combined Power &amp; Heat (CHP) Plant</u></a>	106
<a href="#"><u>18.1.5 Capital Cost Estimate - Wellfield</u></a>	106
<a href="#"><u>18.1.6 Other Sustaining Capital</u></a>	107
<a href="#"><u>18.1.7 Wellfield Basis</u></a>	107
<a href="#"><u>18.1.8 Closure Costs</u></a>	107
<a href="#"><u>18.1.9 Owner's Costs</u></a>	107
<a href="#"><u>18.2 Operating Cost Estimates</u></a>	107
<a href="#"><u>18.2.1 Variable Operating Cost</u></a>	107
<a href="#"><u>18.2.2 Fixed Operating Cost</u></a>	108
<a href="#"><u>18.2.3 Other Operating Costs</u></a>	108
<a href="#"><u>18.2.4 Basis for Operating Cost Estimates</u></a>	109
<a href="#"><u>19 Economic Analysis</u></a>	109
<a href="#"><u>19.1 General Description</u></a>	109
<a href="#"><u>19.2 Basic Model Parameters</u></a>	109
<a href="#"><u>19.3 External Factors</u></a>	110
<a href="#"><u>19.3.1 Pricing</u></a>	110
<a href="#"><u>19.3.2 Taxes and Royalties</u></a>	110
<a href="#"><u>19.3.3 Working Capital</u></a>	110
<a href="#"><u>19.4 Technical Factors</u></a>	110
<a href="#"><u>19.4.1 Mining and Production Profile</u></a>	110
<a href="#"><u>19.4.2 Operating Costs</u></a>	111
<a href="#"><u>19.4.3 Variable Costs</u></a>	112
<a href="#"><u>19.4.4 Fixed Costs</u></a>	112
<a href="#"><u>19.4.5 Other operating costs / (credits)</u></a>	112
<a href="#"><u>19.4.6 Capital Costs</u></a>	112
<a href="#"><u>19.4.7 Infrastructure and Logistics</u></a>	112
<a href="#"><u>19.4.8 Economic Results</u></a>	113
<a href="#"><u>19.4.9 Sensitivity Analysis</u></a>	115
<a href="#"><u>19.4.10 Cash Flow Snapshot</u></a>	115
<a href="#"><u>20 Adjacent Properties</u></a>	117
<a href="#"><u>21 Other Relevant Data and Information</u></a>	117
<a href="#"><u>22 Interpretation and Conclusions</u></a>	117
<a href="#"><u>23 Recommendations</u></a>	118
<a href="#"><u>24 References</u></a>	119
<a href="#"><u>25 Reliance on Information Provided by the Registrant</u></a>	120

## List of Figures

<a href="#">Figure 3.1 General location map</a>	17
<a href="#">Figure 3.2 Property ownership</a>	18
<a href="#">Figure 6.1 Surface geology in the Newberry Springs area</a>	26
<a href="#">Figure 6.2 Topographic map with faults and infrastructure</a>	27
<a href="#">Figure 6.3 Long-section and cross-section through the Fort Cady deposit</a>	28
<a href="#">Figure 6.4 Generalized lithological column for the Fort Cady deposit</a>	29
<a href="#">Figure 7.1 Cross-section through the Fort Cady deposit</a>	32
<a href="#">Figure 7.2 Core photo, 17FTCBL-014</a>	32
<a href="#">Figure 7.3 Project area groundwater basins and surrounding area wells, Fort Cady Project</a>	33
<a href="#">Figure 8.1 Assay results of Standard SRM1835</a>	38
<a href="#">Figure 8.2 Assay results of Standard SRM97b</a>	39
<a href="#">Figure 8.3 Assay results for SRC Standard CAR110/BSM</a>	39
<a href="#">Figure 8.4 Assay results for SRC Standard CAR110/BSH</a>	40
<a href="#">Figure 8.5 Sample blank assay results for boron</a>	40
<a href="#">Figure 8.6 Sample blank assay results for lithium</a>	40
<a href="#">Figure 8.7 Duplicate sample results for boron</a>	41
<a href="#">Figure 8.8 Duplicate sample results for lithium</a>	42
<a href="#">Figure 8.9 HARD diagram for 5E duplicate samples</a>	42
<a href="#">Figure 8.10 SRC duplicate results</a>	43
<a href="#">Figure 8.11 SRC duplicates HARD diagram</a>	43
<a href="#">Figure 10.1 Boric acid solubility curve at various temperatures for CRZ1-1, CRZ1-2, and CRZ1-3</a>	50
<a href="#">Figure 10.2 Boric acid continuous crystallization set-up including an agitated feed tank</a>	50
<a href="#">Figure 10.3 Boric acid crystals after continuous crystallization test (CRZ1-4)</a>	51
<a href="#">Figure 10.4 Boric acid crystals after continuous crystallization test (CRZ1-4) and centrifugation</a>	51
<a href="#">Figure 10.5 Boric acid crystals after re-crystallization</a>	52
<a href="#">Figure 10.6 Boric acid crystals after re-crystallization and dewatering process</a>	52
<a href="#">Figure 11.1 Grade variation swath</a>	60
<a href="#">Figure 11.2 Cash costs, \$/st of boric acid</a>	62
<a href="#">Figure 11.3 Resource classification</a>	65
<a href="#">Figure 13.1 Jet pump assembly</a>	70
<a href="#">Figure 13.2 Year 1 production rates per cycle</a>	71
<a href="#">Figure 13.3 LSBF block 2 mine plan</a>	73
<a href="#">Figure 13.4 Block 2 mining cross section – MMH wells vertical spacing</a>	73
<a href="#">Figure 13.5 Block 2 mining cross section – MMH wells later spacing</a>	74
<a href="#">Figure 13.6 Micro-defamation results</a>	74
<a href="#">Figure 14.1 Small-Scale Facility</a>	75
<a href="#">Figure 14.2 Block flow diagram of the Small-Scale Facility</a>	76
<a href="#">Figure 14.3 LSBF plant layout</a>	81
<a href="#">Figure 14.4 LSBF detailed layout</a>	82
<a href="#">Figure 15.1 Fort Cady Project Infrastructure</a>	89
<a href="#">Figure 16.1 Project market capacity versus demand</a>	92
<a href="#">Figure 16.2 Forecasted boric acid pricing, per Kline</a>	92
<a href="#">Figure 16.3 Boric acid demand by end use, per Kline</a>	94
<a href="#">Figure 16.4 U.S. calcium chloride market demand and growth 2024 – 2034</a>	96
<a href="#">Figure 16.5 Average market price for uncalcined gypsum by grade and application, per Kline</a>	97
<a href="#">Figure 16.6 Gypsum USA production</a>	98

[Figure 16.7 U.S. gypsum market demand and growth, 2024 – 2034](#) ..... 99

[Figure 18.1 Summary of equipment pricing](#) ..... 104

[Figure 19.1 Resource Extraction Profile](#)..... 111

[Figure 19.2 Operating costs \(first ten years\)](#)..... 111

[Figure 19.3 Capital profile of the mine](#) ..... 113

[Figure 19.4 Cash flow projection](#) ..... 113

[Figure 19.5 Sensitivity Analysis](#) ..... 115



## List of Tables

<a href="#">Table 3.1 5E mineral holdings</a>	19
<a href="#">Table 3.2 Current financial assurance obligations</a>	19
<a href="#">Table 5.1 Duval testing results</a>	22
<a href="#">Table 5.2 Mountain States testing injection summary</a>	22
<a href="#">Table 5.3 Mountain States testing recovery summary</a>	22
<a href="#">Table 5.4 Fort Cady Mineral Corporation production summary</a>	23
<a href="#">Table 5.5 5E injection – recovery summary per cycle (IR-1, IR-2, and IR-3)</a>	23
<a href="#">Table 5.6 5E injection – recovery summary per cycle (IR-4)</a>	25
<a href="#">Table 7.1 Historic drilling summary</a>	30
<a href="#">Table 7.2 2017 5E drilling summary</a>	31
<a href="#">Table 7.3 Recent 5E drilling</a>	31
<a href="#">Table 8.1 Summary of QA/QC control samples</a>	38
<a href="#">Table 10.1 Kemetco metallurgical analysis for the five brine samples</a>	46
<a href="#">Table 10.2 Kemetco metallurgical analysis for the five boric acid samples</a>	47
<a href="#">Table 10.3 Simulated crystallizer feed conditions</a>	48
<a href="#">Table 10.4 Amended PLS feed compositions for batch crystallization tests (CRZ1-1 through CRZ1-3)</a>	48
<a href="#">Table 10.5 Feed solutions for continuous crystallization</a>	49
<a href="#">Table 10.6 Boric acid re-crystallization results</a>	53
<a href="#">Table 10.7 Particle size distribution for batch crystallization test CRZ1-1 through CRZ1-3</a>	53
<a href="#">Table 10.8 Particle size distribution for continuous crystallization test CRZ1-4</a>	54
<a href="#">Table 10.10 Boric acid crystal particle size distribution for re-crystallization</a>	54
<a href="#">Table 10.11 Boric acid crystal particle size specification</a>	54
<a href="#">Table 11.1 Summary of drilling database</a>	57
<a href="#">Table 11.2 Modelled horizons</a>	58
<a href="#">Table 11.3 Modelled variograms</a>	59
<a href="#">Table 11.4 Basis of design ratios</a>	61
<a href="#">Table 11.5 Cut-off grade input costs</a>	61
<a href="#">Table 11.6 Cut-off grade analysis</a>	62
<a href="#">Table 11.7 Fort Cady Project mineral resource estimate, March 10, 2025</a>	64
<a href="#">Table 12.1 Proven mineral reserves</a>	67
<a href="#">Table 12.2 Probable mineral reserves</a>	67
<a href="#">Table 12.3 Mineral reserve statement</a>	67
<a href="#">Table 13.1 Wellfield operating strategy mining parameters</a>	71
<a href="#">Table 13.2 Horizontal well program ICP-OES results (July 7, 2025)</a>	72
<a href="#">Table 14.1 LSBF design criteria</a>	77
<a href="#">Table 14.2 LSBF WBS processing facilities</a>	78
<a href="#">Table 14.3 Major plant equipment selections</a>	86
<a href="#">Table 18.1 Capital summary</a>	102
<a href="#">Table 18.2 Detailed breakdown of process facility and infrastructure</a>	103
<a href="#">Table 18.3 Bid summary</a>	104
<a href="#">Table 18.4 5E project deliverables versus standard AACE Class 4 criteria</a>	105
<a href="#">Table 18.5 Mining capital cost estimate</a>	106
<a href="#">Table 18.6 Owner’s cost breakdown</a>	107
<a href="#">Table 18.7 Variable materials cost</a>	108

<a href="#">Table 18.8 Other operating costs</a> .....	109
<a href="#">Table 19.1 Basic model parameters</a> .....	109
<a href="#">Table 19.2 Life of mine summary</a> .....	111
<a href="#">Table 19.3 Variable operating cost over life of mine</a> .....	112
<a href="#">Table 19.4 Total fixed operating cost over life of mine excluding depreciation</a> .....	112
<a href="#">Table 19.5 Total other operating costs / (credits) over life of mine</a> .....	112
<a href="#">Table 19.6 Results of economic analysis</a> .....	114
<a href="#">Table 19.7 Summary of annual cash flow, US\$ millions</a> .....	116

## Glossary of Terms

Abbreviation	Definition
5E	5E Advanced Materials, Inc.
amsl	Above mean sea level
AOR	Area of Review
APBL	American Pacific Borate & Lithium
BA	Boric acid
B <sub>2</sub> O <sub>3</sub>	Boron oxide
bgs	Below ground surface
BLM	US Bureau of Land Management
B <sub>2</sub> O <sub>3</sub>	Boron trioxide (chemical formula)
BMI	Benchmark Mineral Intelligence
C	Celsius
CaCl <sub>2</sub>	Calcium Chloride (chemical formula)
CAGR	Compound annual growth rate
CEQA	California Environmental Quality Act
cm/sec	Centimeters per second
CSTR	Continuous Stirred-Tank Reactor
Duval	Duval Corporation
DXF file	Drawing Interchange Format File
E	East
EIR	Environmental Impact Report (California lead)
EIS	Environmental Impact Statement (BLM lead)
EPA	United States Environmental Protection Agency
F	Fahrenheit
FACE	Financial Assurance Cost Estimate
FCMC	Fort Cady Mineral Corporation
FEL	Front End Loading, a stage gated project management system (with a number to the corresponding stage, e.g., FEL-2)
ft	Foot or Feet
Gal	Gallon(s)
g/l	Gram per liter
Gal/min	Gallons per minute
gpm	gallons per minute
H <sub>2</sub> SO <sub>4</sub>	Sulfuric acid (chemical formula)
H <sub>3</sub> BO <sub>3</sub>	Boric acid (chemical formula)
B(OH) <sub>3</sub>	Boric acid (chemical formula)
HCl	Hydrochloric acid (chemical formula)
ICP	Inductively Coupled Plasma
ID2	Inverse Distance Squared algorithm
IRR	Internal Rate of Return
ISL	In-Situ Leaching
JORC	Australian Joint Ore Reserves Committee
K	Hydraulic coefficient
k	Thousand
kg	Kilogram
kWh	Kilowatt Hour
Kline	Kline & Company, Inc.
lb(s)	Pound(s) mass

LCE	Lithium carbonate equivalents
Li <sub>2</sub> CO <sub>3</sub>	Lithium Carbonate
m	Meters(s)
mm	Millimeter(s)
MDAQCD	Mojave Desert Air Quality Control District
MMBTU	Millions of British Thermal Units
MSME	Mountain States Mineral Enterprises Inc.
Mt	Million tons
M	Million
N	North
NAD 83	North American Datum 83 is a unified horizontal or geometric datum providing a spatial reference for mapping purposes
NEPA	National Environmental Policy Act
NN	Nearest neighbor
NPV	Net present value
pH	Potential Hydrogen – a numeric scale to specify the acidity or alkalinity of an aqueous solution
PLS	Pregnant leach solution
Ppm	Parts per million
psi	Pounds per square inch of pressure
QA/QC	Quality Assurance and Quality Control
QP	Qualified Person per SK1300 definition
ROD	The 1994 Record of Decision for the Fort Cady Project was issued after the EIS/EIR evaluations.
S	Storage coefficient
SBC-LUS	San Bernardino County Land Use Services Department
SBM	San Bernardino Meridian
SCE	SoCal Edison
SEC	Securities and Exchange Commission
SOP	Sulphate of Potash
stpa	Short tons per annum
tpy	Tons per year
UIC	Underground Injection Control Class III Area Permit
USDW	Underground source of drinking water
US	United States
US\$	United States dollars
UTM	Universal Transverse Mercator coordinate system for mapping
XRF	X-Ray Fluorescence Spectrometry

# 1 Executive Summary

This report was prepared as a pre-feasibility level Technical Report Summary in accordance with the Securities and Exchange Commission (SEC) S-K regulations (Title 17, Part 229, Items 601 and 1300 through 1305) for 5E Advanced Materials, Inc. and its subsidiary 5E Boron Americas, LLC, (together 5E or the Company) Fort Cady Project (the Project). The Project described herein is part of 5E's strategy to become a globally integrated supplier of industrial minerals through in-situ extraction of colemanite. Once extracted, the Company will produce and refine boron and calcium-based products. The Project is in the Mojave Desert, near the town of Newberry Springs, California.

Using the volumes, market inputs, and anticipated operating and capital costs, a detailed economic model was created with a forecasted net present value (NPV<sub>7</sub>) of approximately US\$725M and internal rate of return (IRR) of 19.2%. Further details, including key model assumptions, are included in Section 19. This Technical Report Summary includes Phase 1 of the Project, and while the resource base provides the opportunity for expansion that could include additional production tonnage or value-added boron derivatives, they are excluded from this Technical Report Summary.

The Project includes six parcels of private land owned by 5E, federal land owned by the United States Bureau of Land Management, and an electrical transmission corridor runs through the Project where Southern California Edison (SCE) has surface and subsurface control to a depth of 500 ft. While this limits surface access to the area within the right-of-way of the transmission lines, mineral rights are owned by 5E, and mineralization remains accessible as the ore body occurs at depths greater than 1,000 ft. The Project also includes 13 unpatented lode claims, 117 unpatented placer claims and two unpatented millsite claims from the Bureau of Land Management within the U.S. Department of the Interior. On the southwestern side of the Project, the State of California owns the mineral rights for 272 acres of land where 5E owns the surface rights. These mineral rights can be leased from the state.

Major mining permits were obtained in 1994, with a Record of Decision issued by the United States Bureau of Land Management and a Condition Use Permit issued by the State of California. In 2020, an Underground Injection Control Permit was obtained by the United States Environmental Protection Agency and approval to commence mining operations was obtained in 2023. The mining permits allow for 90,000 short tons of borate, defined as boron oxide or boron oxide equivalent, thus permitting up to approximately 160,000 short tons of boric acid.

5E believes the resource is the second largest deposit of borate globally with a history of exploration and mining of the ore body, beginning in 1964 with the resource discovery and includes production of boric acid and synthetic borates by Duval Corporation (Duval) and Fort Cady Mineral Corporation (FCMC). Geologically, the deposit is bounded by faults on both east and west sides and is the site of prior volcanic activity from the Pishah Crater. Mineralization occurs in a sequence of lacustrine lakebed sediments ranging in depths from 1,300 ft to 1,500 ft below ground surface.

Exploration drilling has led to a geologic interpretation of the deposit as lacustrine evaporite sediments containing colemanite, a hydrated calcium borate mineral. The deposit also contains appreciable quantities of lithium. Geologic modeling based on drilling and sampling results depicts an elongate deposit of lacustrine evaporite sediments containing colemanite. The deposit is approximately 2.1 mi. long by 0.6 mi. wide and ranging in thickness from 70 to 262 ft. Mineralization has been defined in four distinct horizons defined by changes in lithology and B<sub>2</sub>O<sub>3</sub> analyses.

A mineral resource and mineral reserve statement has been estimated and reported using a cut-off grade of 2.0% B<sub>2</sub>O<sub>3</sub>. Measured, indicated, and inferred resources for the Project total 135.8 Mt of ore and 18.1 Mt of boric acid. Proven reserves total 1.4 Mt and probable reserves total 4.0 Mt of boric acid, respectively. The initial life of mine for Phase 1 is 39.5 years based on the current mine plan and 41% of the resource has been converted to reserves. The southeastern side of the property includes an exploration target and there is additional resource potential with this target.

The colemanite resource is to be mined via in-situ leaching (ISL) using a hydrochloric acid solution. The leachate will be processed in the commercial-scale facility to initially produce 130,000 short tons per annum (k stpa) of boric acid along with calcium-based by-products calcium chloride and gypsum. A Class 4 or FEL-2 level engineering estimate for the phase 1 plant was prepared as part of this Technical Report Summary. In November 2023, the Company received

approval to commence in-situ mining operations from the United States Environmental Protection Agency (EPA) and began mining in January 2024. The Company's small-scale facility (SSF) began operation in April 2024, has achieved production and has achieved a steady state of approximately one short ton per day of boric acid.

Global boric acid demand remains robust across established markets and future-facing industries while supply continues to be tight across the industry operating network. The supply deficit is expected to continue to materially worsen in the future and lead to elevated pricing. This outlook, along with a pricing forecast for boric acid and its calcium by-products, was assessed in a preliminary market study detailed in Section 16.

Capital cost expectations for a 130,000 stpa boric acid plant (inclusive of co-product processing and COGEN power) were determined to be \$367M for the first stage plus a contingency of \$55M and owner's cost estimate of \$13M for a total capital estimate of \$435M. Operating costs are built upon detailed material and energy balances and recent historical pricing of raw materials and utilities.

Operation of the Company's SSF has provided many of the parameters and scoping items for FEL-2 engineering and the mine plan, while also confirming historical data from operations in the 1980's. Product produced from the SSF has been sent to various customers for qualification and sampling. Progression to Front End Loading Stage 3 Process Design Package (FEL-3) engineering will further refine the accuracy of the capital cost estimates for the chemical processing plant. Additionally, operation of horizontal directional wells is expected to confirm the mine plan for the commercial facility. Once these steps are completed, the Company will be well positioned to advance this pre-feasibility study to a full-feasibility study.

## 2 Introduction

### 2.1 Registrant for Whom the Technical Report was Prepared

This report was prepared as a pre-feasibility study level Technical Report Summary in accordance with the Securities and Exchange Commission S-K regulations Title 17, Part 229, Items 601 and 1300 through 1305 for 5E Advanced Materials, Inc. and its subsidiary 5E Boron Americas, LLC. The report was prepared by Qualified Persons (QPs) from third-party independent companies Fluor Corporation (Fluor), Miocene, Inc. (Miocene), Escalante Geological Services, LLC (Escalante), and Geomega, Inc. (Geomega) and Company management.

### 2.2 Terms of Reference and Purpose of the Report

The quality of information, conclusions, and estimates contained herein is based on the following:

- a) information available at the time of preparation, and
- b) assumptions, conditions, and qualifications set forth in this report.

This Technical Report Summary is based on a Class 4 or FEL-2 pre-feasibility study level engineering. This report is intended for use by 5E Advanced Materials, Inc. and its subsidiary 5E Boron Americas, LLC, subject to the terms and conditions of its agreements with Escalante, Fluor, Geomega, and Miocene and relevant securities legislation. Escalante, Fluor, Geomega, and Miocene permit 5E to file this report as a Technical Report Summary with the U.S. Securities and Exchange Commission (SEC) pursuant to the SEC S-K regulations, more specifically Title 17, Subpart 229.60, Item 601(b)(96) – Technical Report Summary and Title 17, Subpart 229.1300 – Disclosure by Registrants Engaged in Mining Operations. Except for the purposes specified under U.S. securities law, any other uses of this report by any third party are at that party's sole risk. The responsibility for this disclosure remains with the Company.

The purpose of this Technical Report Summary is to report on mineral resources and reserves as well as inform parties with potential financial interests in 5E and the Project.

### 2.3 Sources of Information

This report is based in part on external consultants' expertise and their technical reports, internal Company technical reports, previous technical reports, maps, published government reports, company letters and memoranda, and public information cited throughout this report and listed in Section 25.

Reliance upon information provided by the registrant is listed in Section 25, when applicable.

## **2.4 Details of Inspection**

Escalante, Fluor, Geomega, and Miocene have visited the property, inspected core samples, reviewed relevant intellectual property and reports, and have extensive knowledge of the Project.

## **2.5 Report Version Update**

The user of this document should ensure that this is the most recent Technical Report Summary for the property. This Technical Report Summary is an update of a previously filed Technical Report Summary filed pursuant to 17 CFR §§ 229.1300 through 229.1305 subpart 229.1300 of Regulation S-K. The previously filed Technical Report Summary has a report date of May 11, 2023, a revised report date of February 2, 2024, and an effective date of April 1, 2023.

## **2.6 Units of Measure**

The U.S. System for weights and units has been used throughout this report. Tons are reported in short tons of 2,000 pounds (lb), drilling and resource model dimensions and map scales are in feet (ft). When included, metric tons are referred to as tonnes or mt. All currency is in U.S. dollars (US\$) unless otherwise stated.

## **2.7 Mineral Resource and Mineral Reserve Definition**

The terms "mineral resource" and "mineral reserves" as used in this Technical Report Summary have the following definitions below.

### **2.7.1 Mineral Resources**

17 CFR § 229.1300 defines a "mineral resource" as a concentration or occurrence of material of economic interest in or on the Earth's crust in such form, grade or quality, and quantity that there are reasonable prospects for economic extraction. A mineral resource is a reasonable estimate of mineralization, considering relevant factors such as cut-off grade, likely mining dimensions, location, or continuity, that, with the assumed and justifiable technical and economic conditions, is likely to, in whole or in part, become economically extractable. It is not merely an inventory of all mineralization drilled or sampled.

A "measured mineral resource" is that part of a mineral resource for which quantity and grade or quality are estimated on the basis of conclusive geological evidence and sampling. The level of geological certainty associated with a measured mineral resource is sufficient to allow a qualified person to apply modifying factors, as defined in this section, in sufficient detail to support detailed mine planning and final evaluation of the economic viability of the deposit. Because a measured mineral resource has a higher level of confidence than the level of confidence of either an indicated mineral resource or an inferred mineral resource, a measured mineral resource may be converted to a proven mineral reserve or to a probable mineral reserve.

An "indicated mineral resource" is that part of a mineral resource for which quantity and grade or quality are estimated on the basis of adequate geological evidence and sampling. The level of geological certainty associated with an indicated mineral resource is sufficient to allow a qualified person to apply modifying factors in sufficient detail to support mine planning and evaluation of the economic viability of the deposit. Because an indicated mineral resource has a lower level of confidence than the level of confidence of a measured mineral resource, an indicated mineral resource may only be converted to a probable mineral reserve.

An "inferred mineral resource" is that part of a mineral resource for which quantity and grade or quality are estimated on the basis of limited geological evidence and sampling. The level of geological uncertainty associated with an inferred

mineral resource is too high to apply relevant technical and economic factors likely to influence the prospects of economic extraction in a manner useful for evaluation of economic viability. Because an inferred mineral resource has the lowest level of geological confidence of all mineral resources, which prevents the application of the modifying factors in a manner useful for evaluation of economic viability, an inferred mineral resource considered when assessing the economic viability of a mining project must be presented along with economic viability excluding inferred resources and may not be converted to a mineral reserve.

## 2.7.2 Mineral Reserves

17 CFR § 229.1300 defines a “mineral reserve” as an estimate of tonnage and grade or quality of indicated and measured mineral resources that, in the opinion of the qualified person, can be the basis of an economically viable project. More specifically, it is the economically mineable part of a measured or indicated mineral resource, which includes diluting materials and allowances for losses that may occur when the material is mined or extracted. A “proven mineral reserve” is the economically mineable part of a measured mineral resource and can only result from conversion of a measured mineral resource. A “probable mineral reserve” is the economically mineable part of an indicated and, in some cases, a measured mineral resource.

## 2.8 Qualified Persons

This report was compiled by 5E and its management, with contributions from Escalante Geological Services, LLC, Fluor Corporation, Geomega, Inc., and Miocene, Inc. The QP’s, Escalante, Fluor, Geomega, and Miocene, are third-party firms comprising mining experts in accordance with 17 CFR § 229.1302(b)(1). 5E has determined that the third-party firms and internal management listed as qualified persons meet the qualifications specified under the definition of a qualified person in 17 CFR § 229.1300.

Escalante Geological Services, LLC prepared the following sections of the report:

Sections 2, 3, 4, 5, 6, 7 (excluding 7.3), 8, 9, 11, 15, 17, 20, 21, 22

Fluor Corporation prepared the following sections of the report:

Sections 10, 14, 18 (specifically Sections 18.1.1 through 18.1.4, 18.1.9 and 18.2, which are specific to operating and capital expenditures, excluding wellfield) and contributed to sections 22, 23, and 24

Geomega, Inc. prepared the following sections of the report:

Sections 7.3

Miocene, Inc. prepared the following sections of the report:

Sections 12, 13, 18 (specifically Sections 18.1.5 through 18.1.8, which are specific to wellfield capital expenditures)

The following members of 5E management prepared the following sections of the report:

- Paul Weibel, CPA, and Chief Executive Officer  
Sections 1, 16, 19, 23, 24, 25

Section 16 Market Studies and Contracts was prepared by 5E. The company engaged Kline and Company, Inc. (Kline) to perform a preliminary market study and pricing forecast for boric acid, calcium chloride and gypsum. Forward pricing forecasts obtained from Kline were utilized as part of the financial model outlined in Section 19, Economic Analysis. Kline was not engaged as a qualified person; however, 5E has obtained permission to refer to the preliminary market study they have provided and cite accordingly.

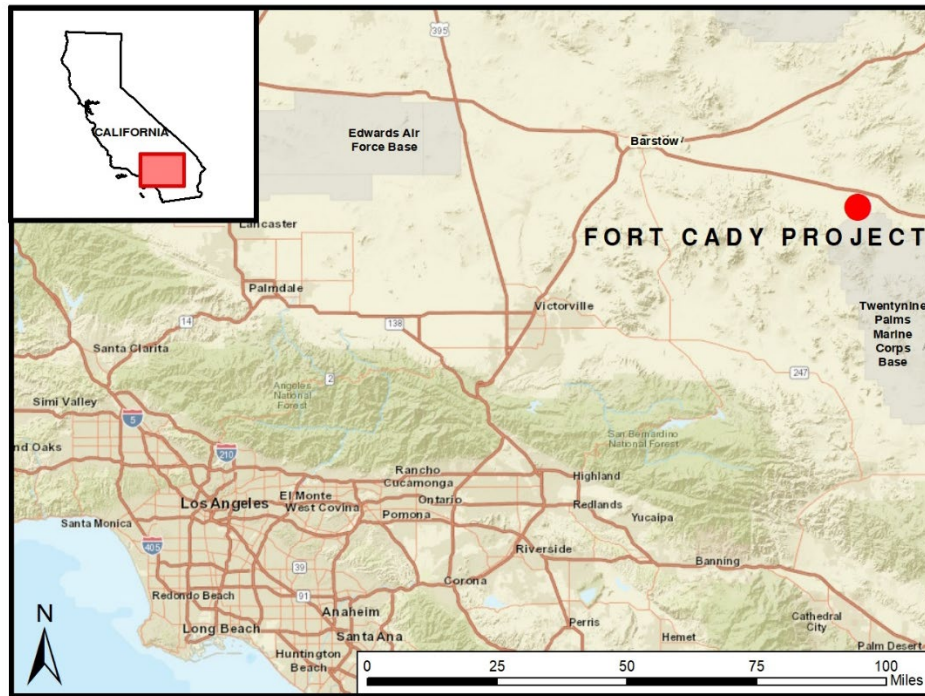


### 3 Property Description and Location

#### 3.1 Property Location

The Project is located in the Mojave Desert region in the high desert of San Bernardino County, California. Figure 3.1 outlines a map where the Project lies, which is approximately 118 mi northeast of Los Angeles, approximately 36 mi east of Barstow and approximately 17 mi east of Newberry Springs. The approximate center of the project area is  $N34^{\circ}45'25.20''$ ,  $W116^{\circ}25'02.02''$ . The Project is in a similar geological setting as Rio Tinto's U.S. Borax operations in Boron, California, and Searles Valley Minerals Operations in Trona, California, situated approximately 75 mi west-northwest and 90 mi northwest of the Project, respectively.

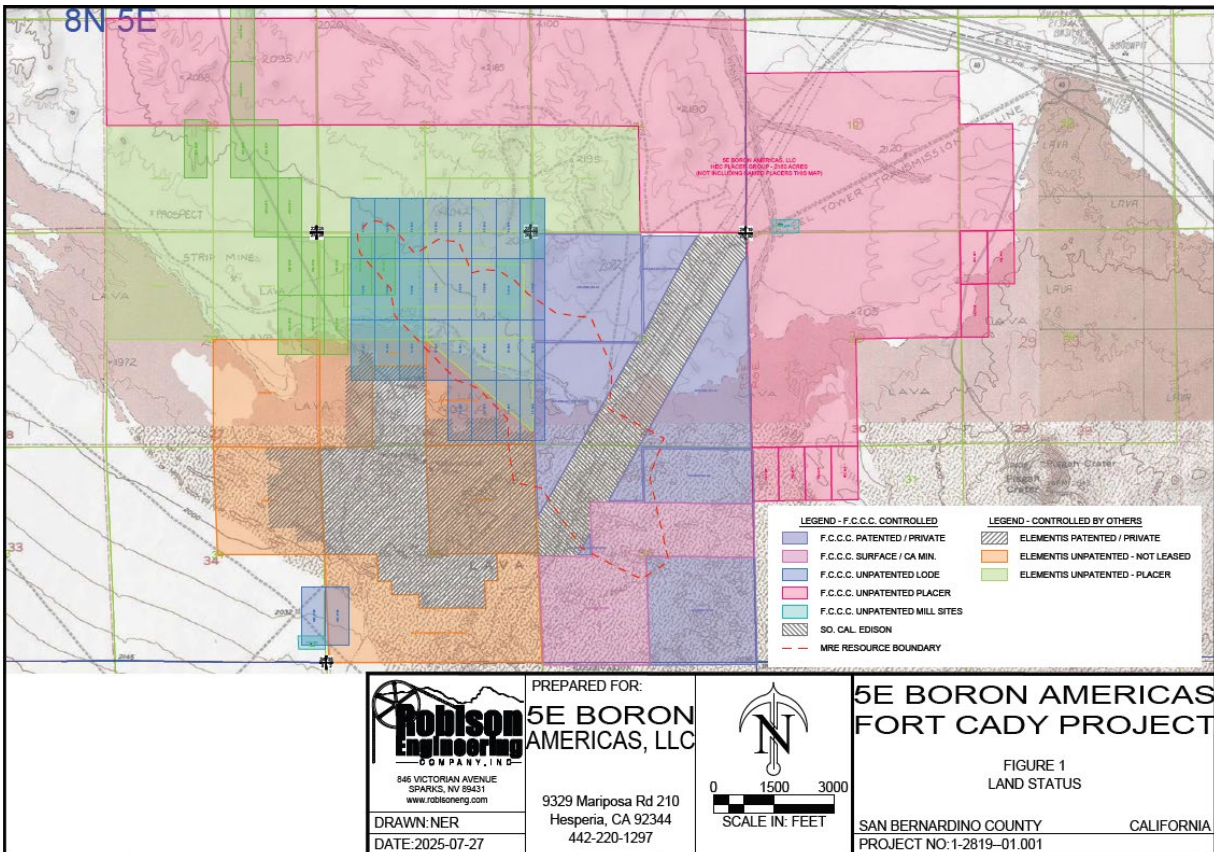
Figure 3.1: General location map



#### 3.2 Area of Property

Figure 3.2 shows the 5E property and adjacent properties.

Figure 3.2: Property ownership



### 3.3 Mineral Title

5E owns simple fee (private) lands in Sections 25 and 36, of Township 8 North, Range 5 East of the San Bernardino Principal Meridian. An electrical transmission corridor, operated by SCE, tracts from the northeast to the southwest through the fee lands with SCE having surface and subsurface control to a depth of 500 ft, affecting approximately 91 acres of surface lands in the two sections. While this limits surface access to the land, mineralization remains accessible as the ore body occurs at depths greater than 1,000 ft (~ 300 m.)

5E currently holds 13 unpatented lode claims, 117 unpatented placer claims, and two (2) unpatented millsite claims with the Bureau of Land Management within the U.S. Department of the Interior. Two lode claims were originally filed by Duval Corporation in 1978 with the 11 other lode claims filed by the Company in January 2025. Placer claims were filed between October 29, 2016, and February 24, 2017. A review of the US Bureau of Land Management (BLM) Mineral & Land Record System, the Mineral Land Record System (MLRS) database shows claim status as filed with next assessment fees due annually on September 1.

Lastly, in Section 36, Township 8 North, Range 5 East, 272 acres of land in Section 36 are split estate, with the surface estate owned by 5E and the mineral estate is owned by the State of California. These lands are available to 5E through a mineral lease from the California State Lands Commission. The remaining lands are owned by 5E, with the minerals underlying the transmission line available subsurface. Table 3.1 summarizes the mineral holdings held by 5E.

Table 3.1: 5E mineral holdings

Land Title Type	Land Titles
Private (Patented Property with surface and mineral rights in Fee Simple Title owned by 5E)	Parcels: 05-29-251-01; 05-29-251-03; 05-29-251-05; 05-29-251-12; 05-29-251-13;
Private (Patented Property with surface rights in Fee Simple Title owned by 5E; Mineral rights owned by State of California)	Parcel: 05-29-251-04
Unpatented Lode Mining Claims Recorded and Located by 5E	HEC #182, HEC #184, FC 001, FC 002, FC 003, FC 004, FC 005, FC 006, FC 007, FC 008, FC 009, FC 010, FC 011
Unpatented Millsite Claims	FCM 001, FCM 002
Unpatented Placer Mining Claims	HEC #19, HEC #21, HEC #23, HEC #25, HEC #34 thru HEC #41; HEC #43 thru HEC #67, HEC #70 thru HEC #82; HEC#85 thru HEC #93; HEC #288, HEC #290, HEC #292, HEC #294, HEC #296, HEC #297, HEC #299 thru HEC #350

### 3.4 Mineral Rights

5E holds the rights to the mineral estate underlying Sections 25 and 36, except for the portion of the mineral estate held by the State of California in Section 36.

### 3.5 Incumbrances

5E maintains financial assurance bonds for reclamation and closure for current and planned operations. Additional information on reclamation and closure liabilities is included in Section 17. The amount of bonds and certificate of deposits posted with the applicable agency are present in Table 3.2.

Table 3.2: Current financial assurance obligations

Regulatory Authority	Regulatory Obligation	Instrument	Instrument US\$
United State Environmental Protection Agency	Groundwater restoration	Bond EACX173000037	\$ 1,212,455
	Groundwater monitoring		
	Plugging and abandonment of AOR wells		
County of San Bernardino	Reclamation and Closure	Certificate of deposits	\$ 326,274

#### 3.5.1 Remediation Liabilities

5E has submitted a Final Reclamation and Closure Plan to the Lahontan Regional Water Quality Control Board for closure of ponds constructed on the property in the 1980's. The bonding for closure of these ponds is included in the certificate of deposits with San Bernardino County and upon closure of the ponds, the bond will be reduced and a portion of the deposited amount returned to the company.

### 3.6 Other Significant Risk Factors

The mineral resource estimate (Section 11) excludes BLM land where other third-parties have active lode claims for portions of the deposit.

An exploration program to expand the resource is possible in Section 36 on the southeastern portion of the property; however, this would require a mineral lease to be filed and executed with the California State Lands Commission for the State of California held mineral estate.

### 3.7 Royalties

There are no royalties associated with privately and publicly held lands in Section 25 and 36.

## 4 Accessibility, Climate, Local Resources, Infrastructure, and Physiography

### 4.1 Topography, Elevation, and Vegetation

The Project area is located on a gentle pediment with elevations ranging from approximately 1,970 ft above mean sea level (amsl) to approximately 2,185 ft amsl. Basalt lava flows cover most of the higher elevations or hilltops with flat ground and drainages covered in pale, gray-brown, silty soils. Basalt lava flows become more dominant south of the Project area with the Lava Bed Mountains located a few miles south of the Project area. The Project area's vegetation is dominated by burro weed, creosote, cactus, and scattered grasses.

### 4.2 Accessibility and Transportation to the Property

Access to the Project is via U.S. Interstate 40 (I-40), eastbound from Barstow to the Hector Road exit. From the exit, travel south to Route 66, then east approximately 1 mile to County Road 20796 (CR20796). Travel south on CR20796 for 2.2 mi to the unnamed dirt access road bearing east for another 1.1 mi to the Project.

The BNSF Railroad main line from Chicago to Los Angeles runs parallel to I-40. A BNSF rail loadout is in Newberry Springs. There are potential options to develop rail access closer to the Project.

San Bernardino County operates six general aviation airports with the closest airport to the Project being the Barstow-Daggett Airport located approximately 23 mi west of the Project off Route 66. Commercial flight service is available through five airports in the greater Los Angeles area and in Las Vegas, Nevada. A dedicated cargo service airport is located approximately 65 mi southwest of the Project.

### 4.3 Climate and Length of Operating Season

The Project is accessible year-round, located in the western Mojave Desert with arid, hot, dry, and sunny summers of low humidity and temperate winters. Based upon climate data from the nearby town of Newberry Springs, the climate over the past 30 years indicates average monthly high temperatures ranging from 55°F in December to 98.2°F in July. Monthly low temperatures range from 40.1°F in December to 74.3°F in August. Extremes range from a record low of 7°F to a record high of 117°F. Maximum temperatures in summer frequently exceed 100°F while cold spells in winter with temperatures below 20°F may occur but seldom last for more than a few days. Average rainfall is generally less than 10 inches per year with most precipitation occurring in the winter and spring.

### 4.4 Infrastructure Availability and Sources

SE continues to develop operating infrastructure for the Project in support of extraction and processing activities. A manned gate is located on the Project access road and provides required site-specific safety briefings and monitors personnel entry and exit to the site. Personnel are predominantly sourced from the surrounding area including Barstow, California, and Victorville, California.

The BNSF Railroad main line from Las Vegas, Nevada to Los Angeles, California runs parallel to I-40. A rail loadout is located approximately 1.2 mi north of the National Trails Highway on a road that bears north and located 0.4 mi west of CR20796.

The construction of the small-scale facility was performed by a construction contractor with additional local resources supporting construction contracting, construction materials, energy sources, employees, and housing. The Project has good access to I-40 which connects it to numerous sizable communities between Barstow, California and the greater Los Angeles area offering excellent access to transportation, construction materials, labor, and housing. The Project currently has limited electrical service (approximately 1 megawatt) that is sufficient for mine office, storage facilities on

site, and provides a good portion of the power for the small-scale facility. The small-scale facility operates on shore power and liquid natural gas and 5E is currently exploring options for upgrading electrical services to the Project. An electrical transmission corridor operated by SCE extends northeastward through the eastern part of the Project. The Project has two water wells located nearby to support in-situ leaching operations where unpatented millsite claims are filed. Currently there is no natural gas connected to the Project, but 5E has a proposal from Kinder Morgan to connect to the Mojave Pipeline. Two other natural gas transmission lines run along Interstate 40 near the Project.

The plant site currently has a 1,600 ft<sup>2</sup> mine office building, a control room, storage buildings, an analytical laboratory, an approximately 20-acre production facility called the small-scale facility, and an intended gypsum storage area occupying 17 acres. Gypsum is a byproduct of past pilot plant production and is intended to be a future byproduct that can be sold to the regional market.

## 5 History

Discovery of the Project borate deposit occurred in 1964 when Congdon and Carey Minerals Exploration Company found several zones of colemanite, a calcium borate mineral, between the depths of 1,330 ft to 1,570 ft (405m to 487m) below ground surface (bgs) in Section 26, Township 8 North, Range 5 East. Simon Hydro-Search, 1993.

### 5.1 Prior Ownership and Ownership Changes

In September 1977, Duval initiated land acquisition and exploration activities near Hector, California. By March 1981, Duval had completed 34 exploration holes (DHB holes), plus one 1 potential water well. After evaluation of the exploration holes, Duval considered several mining methods. Subsequent studies and tests performed by Duval indicated that in-situ mining technology was feasible. Duval commenced limited testing and pilot-scale solution mining operations in June 1981 per the Mining and Land Reclamation Plan, Fort Cady Project, 2019.

Mountain States Mineral Enterprises, Inc. (MSME) purchased the project from Duval in 1985 and, in 1986, conducted an additional series of tests. MSME eventually sold the project to Fort Cady Mineral Corporation in 1989. FCMC began the permitting process, which resulted in a 1994 Record of Decision (ROD) from the BLM and approval from San Bernardino County, the California lead agency.

### 5.2 Exploration and Development Results of Previous Owners

Duval commenced limited-scale solution mining tests in June 1981. Between 1981 and 2001, subsequent owners drilled an additional 17 wells, which were used for a series of injection testing and pilot-scale operations. In July 1986, tests were conducted by MSME, where dilute hydrochloric acid solution was injected into the ore body. The acid dissolved the colemanite and was then withdrawn from the same well.

The first phase of pilot plant operations was conducted between 1987 and 1988. Approximately 550 tons (500 tonnes) of boric acid were produced. The test results were positive; thus, the Project was viewed as commercially viable. In preparation for the permitting process, feasibility studies, detailed engineering and test works were completed with FCMC receiving the required permits for a commercial-scale operation. Final state and local approvals for commercial-scale solution mining and processing was attained in 1994.

A second phase of pilot plant operations occurred between 1996 and 2001, during which approximately 2,200 tons of a synthetic colemanite product, marketed as CadyCal 100, were produced. Commercial-scale operations were not commissioned due to low product prices and other priorities of the controlling entity. For many years, boron was used in traditional applications such as cleaning supplies and ceramics, which never formulated in a strong pull-side demand investment thesis where pricing justified further development of the Project. However, a group of Australian investors, through extensive due diligence identified green shoots that the market dynamics were fundamentally beginning to change.



### 5.3 American Pacific Borates Share Exchange of Atlas Precious Metals

In 2017, a group of Australian investors identified the Project and formed the investment thesis that the boron market had similar dynamics to the lithium market a decade earlier. Like the lithium market ten years prior, the market was dominated by a few companies with a compelling pull-side demand growth story fueled by future-facing applications targeting decarbonization and critical materials. Prior to lithium-ion batteries and electric vehicles, lithium was used in traditional everyday applications like boron's use in recent years. As a result of the investment thesis that boron is expected to experience a supply deficit relative to demand, the group of Australian investors formed American Pacific Borates and Lithium Ltd (APBL) and issued shares to Atlas Precious Metals in exchange for the Fort Cady (California) Corporation, the entity holding the permits, mineral and property rights of the Project. In 2017, APBL underwent an initial public offering on the Australian Stock Exchange and progressed exploration and development of the Project. In September 2021, APBL created a subsidiary, 5E, through a corporate reorganization which placed 5E at the top of the corporate structure. Upon 5E becoming the parent company of the organization, in March 2022 5E direct listed on Nasdaq and became an SEC issuer. Shortly before becoming an SEC issuer, 5E Boron Americas, LLC was designated as Critical Infrastructure by the Department of Homeland Security Cybersecurity and Infrastructure Security Agency.

### 5.4 Historic Production

Limited historic production data, provided to 5E by previous operators, is summarized in Table 5.1 through Table 5.4. Little other information is available for these tests; the results could not be independently verified.

Table 5.1: Duval testing results

Test No.	Volume Injected Gal	Injection Rate Gal/min	Pump Pressure PSI	Acid %	Volume Recovered Gal	Recovery Rate Gal/min	Average Concentration H <sub>3</sub> BO <sub>3</sub> %	Maximum Concentration H <sub>3</sub> BO <sub>3</sub> %
1	680	1.5	150	16% HCl	700	1.0-2.0	0.3	
	1,500	2	275	5% H <sub>2</sub> SO <sub>4</sub>	1,500	1.0-2.0	0.5	1.5
	1,400	1.5-2.0	150	5% H <sub>2</sub> SO <sub>4</sub>	2,000	1.0-2.0	1.5	4.6
	1,500	2	275	23% H <sub>2</sub> SO <sub>4</sub>	1,500	1.0-2.0	1.0	4.0
2	2,250	2	300	8% H <sub>2</sub> SO <sub>4</sub>	2,000	1.5-2.0	1.5	4.0
3	5,358	2-2.5	275	6.9% H <sub>2</sub> SO <sub>4</sub>	28,927	1.0-1.5	3.0	6.9
	6,597	2-2.5	275	17.5% HCl			3.0	6.9
4	19,311	2-2.5	230-275	6.2% HCl & 2.4% H <sub>2</sub> SO <sub>4</sub>	67,995	1.0-1.5	3.0	6.5
5	20,615	2	290	16% HCL	112,637	1.0-1.5	2.5	5.2
6	21,569	20	275	1.6% HCl	63,460	1.0-1.5	1.1	1.7

Table 5.2: Mountain States testing injection summary

Series	Date		Test Nos.	Wells SMT	Gallons		Pounds		Theoretical H <sub>3</sub> BO <sub>3</sub>	
	From	To			Series	Σ	HCl	CO <sub>2</sub>	Series	Σ
1	8/4/1986	8/23/1986	1-3	6 & 9	67,972	67,972	23,286	—	59,540	59,540
2	11/4/1986	11/10/1986	4-7	6	45,489	113,461	15,500	—	39,431	98,971
3	12/9/1986	12/18/1986	8-11	6	53,023	166,484	15,398	—	39,173	138,144
4	6/18/1986	6/27/1987	12-15	9	47,640	214,124	—	4,313	18,184	156,328
<b>Total</b>					<b>214,124</b>	<b>214,124</b>	<b>54,184</b>	<b>4,313</b>	<b>156,328</b>	<b>156,328</b>

Table 5.3: Mountain States testing recovery summary

Series	Date		Test Nos.	Wells SMT	Gallons		Pounds BA		% BA in Solution, by Surge Tank			Theoretical BA	
	From	To			Series	Σ	Series	Σ	High	End	Avg	Series	Σ
1	8/7/1986	10/17/1986	1-3	6 & 9	128,438	128,438	32,608	32,608	3.84	1.56	2.50	54.77	54.77
2	11/5/1986	11/13/1986	4-7	6	51,636	180,074	21,223	53,831	5.74	4.05	4.68	53.83	54.39
3	12/10/1986	1/13/1987	8-11	6	99,889	279,963	33,386	87,217	5.59	1.93	4.18	85.23	63.14
4	6/9/1987	7/0/1987	12-15	9	86,595	366,558	18,973	106,190	3.55	1.81	2.60	104.34	67.93
<b>Total</b>					<b>366,558</b>	<b>366,558</b>	<b>106,190</b>	<b>106,190</b>			<b>3.79</b>		<b>67.93</b>

In 2017, 5E completed an exploration drilling program to validate previous exploration efforts and expand mineral resources. Post drilling, an Australasian Code for Reporting of Exploration Results, Mineral Resources and Ore Reserves (JORC) mineral resource estimate was prepared by Terra Modelling Services. TMS updated the JORC mineral resource estimate in December 2018. The 2018 JORC mineral resource estimate identified 4.63 million tonnes of measured resource, 2.24 million tonnes of indicated resource, and 7.07 million tonnes of inferred resource using a B<sub>2</sub>O<sub>3</sub> cut-off grade of 5%.

In October 2021, 5E issued an Initial Assessment Report on the Fort Cady Borate Project reporting a measured plus indicated resource estimate of 97.55 million tons (Mt) grading at 6.53% B<sub>2</sub>O<sub>3</sub> and 324 ppm Lithium using a 5.0% B<sub>2</sub>O<sub>3</sub> cut-off grade. The Initial Assessment also identified 11.43 Mt of in Inferred resource grading at 6.40% B<sub>2</sub>O<sub>3</sub> and 324 ppm Li. The Initial Assessment was subsequently updated in February 2022 with no changes to the resource estimate.

In October 2023, 5E updated and issued the Initial Assessment Report, dated October 2023, on the Project. The October 2023 Initial Assessment Report provided an updated estimate of 74.31 Mt of measured plus indicated resources grading at 4.15 B<sub>2</sub>O<sub>3</sub> and 356 ppm Li using a 2.0% B<sub>2</sub>O<sub>3</sub> cut-off grade, following a change in mineral tenure and improvements in processing. An inferred resource of 96.9 Mt grading at 4.75% B<sub>2</sub>O<sub>3</sub> and 321 ppm LI was also identified in the estimate.

Table 5.4: Fort Cady Mineral Corporation production summary

Flow to Plant											
Date	Total Minutes	Gallons	Gal/min	pH	Free Acid g/l	Boric Acid %	Chloride g/l	Sulfate g/l	Boric Acid tons	B <sub>2</sub> O <sub>3</sub> tons	CadyCal 100 tons
Jan-01	7,215	258,556	35.8	5.83		2.33	12.54	3.76	15	9	20
Feb-01	7,785	331,886	42.6	2.54	0.35	2.36	12.13	4.94	25	14	33
Mar-01	10,470	422,922	40.4	2.41	0.23	1.90	15.84	3.23	34	19	45
Apr-01	10,290	393,824	38.3	1.86	2.60	5.43	42.11	8.18	41	23	53
May-01	7,560	296,000	39.2	2.02	2.67	5.77	44.77	8.70	31	17	40
Jun-01	3,375	120,928	35.8	0.67	1.35	3.12	27.84	5.30	12	7	16
Jul-01	2,385	77,157	32.4	1.19	0.31	2.00	12.74	2.60	7	4	9
Aug-01	3,300	142,207	43.1	4.04	0.07	3.84	19.60	3.08	15	8	19
Sep-01	4,875	247,901	50.9	2.77	0.12	3.44	23.21	3.68	21	12	28
Oct-01	10,035	478,723	47.7	2.03	0.35	3.00	15.54	4.60	37	1	49
Nov-01	9,270	371,171	40.0	1.99	0.16	2.39	14.15	4.02	23	13	30
Dec-01	12,525	353,885	28.3	1.83	0.17	2.52	14.94	2.58	29	16	38
01-Total	89,085	3,495,160	39.2	2.44	0.73	3.19	21.37	4.74	291	164	381
00-Total	87,255	3,142,413	36.0	2.14	0.25	2.70	12.42	2.54	279	157	366
99-Total	92,820	2,475,770	26.7	1.59	0.48	2.82	10.13	6.84	201	113	263
98-Total	111,468	2,715,319	24.4	1.24	0.91	2.85	7.78	10.19	217	122	284
97-Total	109,040	2,692,940	24.7	0.99	1.84	3.10	3.52	13.00	252	142	329
96-Total	101,212	2,711,044	26.8	1.33	1.32	3.01	2.96	5.76	244	137	319

In January 2024, the Company began injection after receiving approval from the EPA to commence mining in November 2024. In April 2024, the Company began operating its small-scale facility and producing borates. Table 5.5 summarizes 5E's injection – recovery summary per cycle for IR-1, IR-2, and IR-3 while and table 5.6 summarizes 5E's injection – recovery summary per cycle for IR-4.

Table 5.5: 5E injection – recovery summary per cycle (IR-1, IR-2, and IR-3)

Complete I/R Cycle	Injection Well	Volume Injected (gal)	Injection Rate (gal/min)	Pump Pressure (psi)	Recovery Well	Volume Recovered (gal)	Recovery Rate (gal/min)	Average H <sub>3</sub> BO <sub>3</sub> %
1	IR-3	5,206.99	14.89	63.28				
2	IR-1	9,230.59	11.45	24.13	IR-3	732.70	9.27	2.20
3	IR-2	4,443.94	14.86	116.50	IR-2	2,893.28	1.82	2.29
4	IR-1	18,369.41	27.61	121.20				
5	IR-2	3,571.00	15.96	67.31	IR-1	2,407.62	3.06	0.62
					IR-3	1,191.32	1.34	1.11
6	IR-1	13,745.17	18.14	67.64	IR-2	2,329.89	2.25	3.07
7	IR-3	26,375.01	39.82	42.61	IR-1	8,346.20	17.27	2.11
					IR-2	12,717.00	34.55	1.96

Complete I/R Cycle	Injection Well	Volume Injected (gal)	Injection Rate (gal/min)	Pump Pressure (psi)	Recovery Well	Volume Recovered (gal)	Recovery Rate (gal/min)	Average H <sub>3</sub> BO <sub>3</sub> %
8	IR-2	2,357.90	15.40	64.06	IR-3	3,247.43	14.60	1.60
					IR-1	707.36	4.62	0.99
					IR-2			
					IR-3	1,414.70	9.24	0.55
9	IR-1	779.53	23.01	58.10	IR-1	472.02	13.37	0.79
					IR-2	461.27	7.68	0.25
					IR-3	464.61	7.74	0.55
10	IR-2	3,516.00	11.91	115.16	IR-1	2,109.60	7.15	0.82
					IR-3	1,054.80	3.57	0.55
11	IR-1	11,620.79	20.08	25.47	IR-1			
					IR-2	3,673.40	7.91	2.09
					IR-3	5,592.49	13.09	1.48
12	IR-2	11,047.68	2.62	80.31	IR-2	19,149.02	6.65	4.53
	IR-3	16,450.00	21.08	140.30	IR-1	29,127.24	6.74	5.64
	IR-1	12,410.20	19.57	122.25	IR-3	16,107.29	7.45	4.24
	IR-3	1,815.00	12.35	103.00				
	IR-2	333.00	5.55	111.00				
	IR-1	5,209.97	43.40	28.59				
13	IR-1	27,337.13	6.70	60.57	IR-1	40,537.49	9.38	5.29
	IR-3	22,531.94	3.54	55.19				
14	IR-1	33,894.24	6.35	64.34	IR-1	31,620.99	5.92	5.18
15	IR-1	32,065.38	8.60	115.38	IR-3	2,127.05	3.94	5.55
16	IR-1	4,849.05	2.07	71.86	IR-1	41,348.82	17.67	6.13
	IR-3	11,114.78	5.61	72.84	IR-2	17,567.34	9.76	4.06
17	IR-3	2,521.19	28.19	52.33	IR-1	10,071.44	4.94	5.67
	IR-1	2,758.17	61.29	98.48	IR-3	15,981.97	7.83	4.92
					IR-2	863.74	0.25	5.67
18	IR-1	11,052.45	3.76	70.81	IR-1	19,205.31	16.01	7.07
	IR-3	18,854.36	3.74	69.45	IR-2	1,545.69	0.80	9.17
					IR-3	6,324.87	3.40	6.63
19	IR-1	4,905.86	7.43	73.67	IR-1	5,097.00	2.83	4.03
					IR-2	13,070.53	7.26	4.68
					IR-3	1,733.01	0.70	4.38
20	IR-1	5,249.52	5.15	40.20				
	IR-3	11,049.80	7.67	36.23				
	IR-1	4,078.35	6.47	70.07				
	IR-2	2,542.97	14.13	64.00	IR-1	655.19	0.91	4.12
	IR-3	8,035.73	7.44	61.25	IR-2	6,197.07	4.68	4.13
	IR-1	11,890.22	5.08	71.66	IR-3	5,450.06	4.54	5.19
21	IR-1	15,110.04	7.41	64.49	IR-1	23,296.09	3.23	7.43
	IR-3	9,455.86	4.38	62.88	IR-2	17,009.05	2.36	7.65
	IR-1	6,794.54	2.98	54.36	IR-3	4,835.47	0.67	8.21
22	IR-1	5,632.64	3.91	58.98	IR-1	986.47	0.46	8.32
	IR-3	26,175.41	3.03	112.36	IR-2	10,971.17	5.08	7.53
					IR-3	837.90	0.39	4.86
					24 Hour Recovery Pause			
					IR-1	8,663.25	6.30	3.28
					IR-2	8,831.20	4.54	3.26
23	IR-1	20,111.84	16.76	51.24	IR-3	1,189.49	0.49	3.14
					IR-1	5,338.40	1.49	7.46
					IR-2	20,262.84	8.65	6.56
24	IR-3	1,305.83	21.76	41.98	IR-3	3,839.77	4.92	4.15
					IR-1	433.72	7.22	2.12
					IR-2	6,726.29	10.19	2.79
	IR-1	4,219.55	3.91	70.26	IR-3	433.72	7.22	3.29
	IR-2	5,851.48	1.81	68.98				
	IR-3	4,589.64	1.37	71.58	7 Day Recovery Pause			
25	IR-3	10,217.39	2.94	72.65	IR-1	1,259.62	1.05	5.14
					IR-2	12,583.30	13.12	6.23
					IR-3	1,106.44	2.63	4.86
26	IR-1	6,657.38	2.71	60.05	IR-1	1,983.10	1.84	4.86
					IR-2	4,304.86	4.03	4.86
					IR-3	16,086.25	9.15	6.06
27	IR-3	4,522.27	3.77	68.32	IR-3	33,720.96	4.68	6.27
28	IR-3	15,847.10	9.78	67.88	IR-2	12,072.07	8.05	5.08
					IR-3	1,226.40	0.82	5.08
29	IR-1	7,303.31	3.38	54.68	IR-2	33,433.04	14.65	4.83
	IR-3	7,795.03	3.61	68.44				
29	IR-3	6,330.72	13.19	67.56	IR-3	25,288.41	17.56	5.49



Complete I/R Cycle	Injection Well	Volume Injected (gal)	Injection Rate (gal/min)	Pump Pressure (psi)	Recovery Well	Volume Recovered (gal)	Recovery Rate (gal/min)	Average H <sub>3</sub> BO <sub>3</sub> %
	IR-1	4,228.14	4.70	44.36				
30	IR-3	1,773.14	1.06	94.60	IR-2	12,790.93	17.76	4.63
31	IR-1	24,119.86	23.65	114.25	IR-3	15,666.38	14.51	5.49
	IR-3	13,818.41	12.79	77.86	IR-1	5,285.80	3.52	4.49
32	IR-3	8,717.51	8.07	61.45				
	IR-1	11,354.01	10.51	101.36	IR-2	13,456.27	13.68	4.04
33	IR-3	2,979.31	8.28	99.25				
	IR-3	9,673.93	4.48	78.59	IR-1	1,792.07	4.97	4.74
34	IR-1	4,181.65	3.87	85.69	IR-2	12,871.21	11.92	4.72
	IR-3	8,053.74	8.95	114.23	IR-1	6,517.74	3.62	4.73
Steam heated solution								
35	IR-1	68,518.59	63.44	74.36	IR-3	68,518.59	63.44	5.65
36	IR-1	35,022.36	32.43	68.64	IR-2	35,022.36	32.43	5.62
37	IR-1	13,988.00	12.95	61.33	IR-2	2,648.00	7.35	5.92
					IR-3	11,185.03	31.06	5.59
38	IR-1	6,021.82	5.58	57.68	IR-2	11,218.12	18.69	5.26
	IR-3	1,590.00	6.63	67.24	IR-3	8,575.53	14.29	4.55
	IR-1	19,710.28	18.25	70.25	IR-2	10,822.60	4.09	4.74
					IR-3	9,168.02	3.47	3.70
39	IR-3	9,089.95	25.25	69.58				
	IR-1	1,556.98	1.44	71.68	IR-2	24,947.90	11.67	4.28
	IR-1	3,429.60	3.18	78.36				
40	IR-1	4,545.51	4.21	64.39				
	IR-1	25,433.09	23.55	61.48	IR-3	15,245.69	5.52	5.96
Total		627,453.08				658,696.49		

Table 5.6: 5E injection – recovery summary per cycle (IR-4)

Complete I/R Cycle	Injection Well	Volume Injected (gal)	Injection Rate (gal/min)	Pump Pressure (psi)	Recovery Well	Volume Recovered (gal)	Recovery Rate (gal/min)	Average H <sub>3</sub> BO <sub>3</sub> %
1	IR-4	3,496.01	21.29	115.56	IR-4	2,663.89	10.82	0.40
2	IR-4	5,395.21	3.93	124.26	IR-4	8,136.86	22.04	3.20
3	IR-4	2,537.92	3.60	102.73	IR-4	715.80	20.92	2.69
4	IR-4	11,527.29	15.52	112.38	IR-4	8,650.70	28.63	4.60
5	IR-4	16,474.89	12.61	73.75	IR-4	3,564.96	16.50	3.01
6	IR-4	7,400.40	6.59	120.55	IR-4	8,729.30	20.19	4.78
7	IR-4	7,853.70	9.26	119.92	IR-4	7,937.90	17.94	5.55
8	IR-4	8,878.00	10.87	93.00	IR-4	15,790.90	10.34	6.01
9	IR-4	8,700.30	6.44	69.12	IR-4	12,922.89	6.05	5.90
10	IR-4	9,641.00	9.45	128.79	IR-4	21,252.32	6.78	5.39
11	IR-4	10,983.36	7.32	137.15	IR-4	28,551.44	15.17	4.74
12	IR-4	13,529.92	5.78	138.88	IR-4	14,205.00	11.80	4.81
13	IR-4	13,600.29	5.15	117.73	IR-4	15,109.93	9.33	4.88
14	IR-4	6,446.20	8.77	82.06	IR-4	20,930.95	7.75	4.90
15	IR-4	17,513.86	14.71	119.40	IR-4	18,259.44	6.34	5.51
16	IR-4	26,883.73	17.52	128.26	IR-4	13,426.25	9.32	5.30
17	IR-4	47,761.87	40.14	70.04	IR-4	12,123.06	50.51	3.20
18	IR-4	12,993.61	4.93	34.88	IR-4	33,627.47	7.57	6.13
19	IR-4	58,515.05	5.29	89.10	IR-4	7,731.22	1.30	5.05
20	IR-4	10,528.19	5.70	55.69	IR-4	10,844.75	4.11	7.35
21	IR-4	7,715.22	16.92	126.53	IR-4	8,752.76	12.16	3.97
22	IR-4	1,077.09	17.95	41.90	IR-4	17,930.93	3.11	5.69
23	IR-4	50,693.34	5.87	111.46	IR-4	25,935.29	9.01	5.85
24	IR-4	10,344.98	2.39	64.78	IR-4	13,928.74	4.84	6.31
25	IR-4	8,021.89	13.37	72.58	IR-4	34,964.89	6.07	5.18
26	IR-4	8,070.94	11.21	64.23	IR-4	5,078.17	3.53	2.92
27	IR-4	1,415.94	23.60	84.69	IR-4	13,223.72	10.50	5.08
28	IR-4	12,780.83	4.95	68.33	IR-4	10,037.30	11.15	4.86
29	IR-4	10,254.86	15.54	94.22	IR-4	10,227.39	4.73	3.39
30	IR-4	23,327.37	4.05	70.06	IR-4	16,649.16	4.62	6.32
31	IR-4	5,215.85	17.39	62.25	IR-4	15,252.04	4.24	6.92
32	IR-4	13,609.48	5.16	66.35	IR-4	14,282.18	4.96	10.93
33	IR-4	4,667.70	15.56	68.58	IR-4	17,595.95	12.22	4.33
Total		457,856.29				469,033.55		

## 6 Geological Setting, Mineralization and Deposit

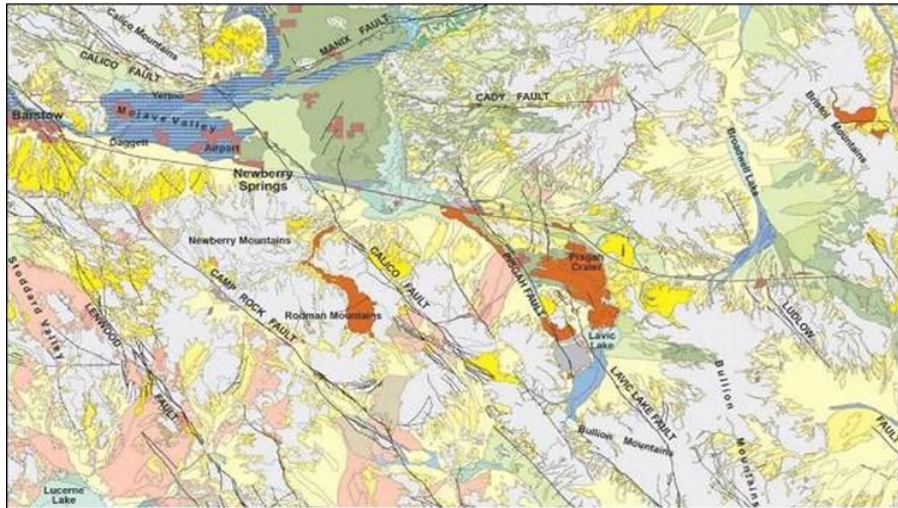
### 6.1 Regional Setting

The Project area is in the western Mojave Desert and is part of the Basin and Range Physiographic Province. The region is characterized by narrow faulted mountain ranges and flat valleys and basins, the result of tectonic extension that began approximately 17 million years ago. The Project lies within the Hector Basin of the Barstow Trough and is bounded on the southwest by the San Andreas fault zone and the Transverse Ranges, on the north by the Garlock fault zone, and on the east by the Death Valley and Granite Mountain infrastructure faults. Numerous faults of various orientations are found within the area with various orientations though the predominant trend is to the northwest.

The Barstow Trough, a structural depression, extends northwesterly from Barstow toward Randsburg and to east-southeast toward Bristol. It is characterized by thick successions of Cenozoic sediments, including borate-bearing lacustrine deposits, with abundant volcanism along the trough flanks. The northwest-southeast trending trough initially formed during Oligocene through Miocene times. As the basin was filled with sediments and the adjacent highland areas were reduced by erosion, the areas receiving sediments expanded, and playa lakes, characterized by fine-grained clastic and evaporitic chemical deposition, formed in the low areas at the center of the basins.

Exposures of fine-grained lacustrine sediments and tuffs, possibly Pliocene in age, are found throughout the Project area. Younger alluvium occurs in washes and overlying the older lacustrine lakebed sediments. Much of the Project area is covered by recent olivine basalt flows from Pisgah Crater, which is located approximately two miles east of the site as shown in Figure 6.1 and Figure 6.2. Thick fine-grained, predominantly lacustrine lakebed mudstones appear to have been uplifted, forming a block of lacustrine sediments interpreted to be floored by an andesitic lava flow.

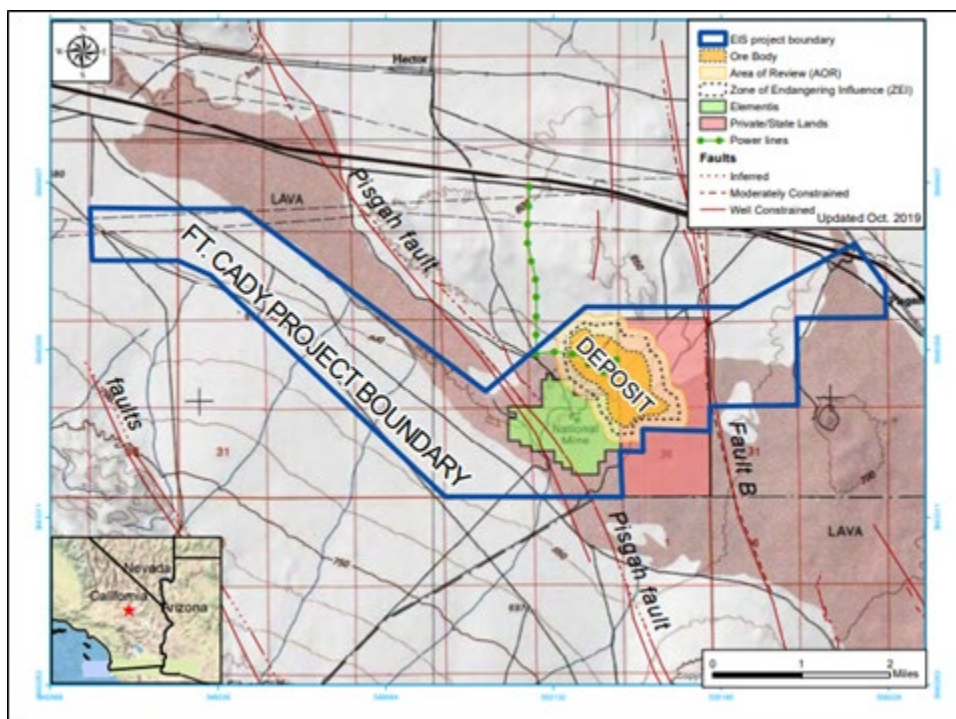
*Figure 6.1: Surface geology in the Newberry Springs area*



There are three prominent geologic features in the project area (Figure 6.2):

- Pisgah Fault, which transects the southwest portion of the project area west of the ore body;
- Pisgah Crater lava flow located approximately 2 miles east of the site: and
- Fault B, located east of the deposit.

Figure 6.2: Topographic map with faults and infrastructure



The Pisgah Fault is a right-lateral slip fault that exhibits at least 250 ft of vertical separation at the Project. The east side of the fault is up-thrown relative to the west side. Fault B is located east of the ore body and also exhibits at least 250 ft of vertical separation; however, at Fault B, the east side is down dropped relative to the west side. The uplifted zone containing the borate ore body the Wedge is situated within a thick area of fine-grained, predominantly lacustrine lakebed mudstones, east of the Pisgah Fault and west of Fault B.

### 6.1.1 Mineralization

Mineralization occurs in a sequence of lacustrine lakebed sediments ranging in depths from 1,300 ft to 1,500 ft bgs. The mineralization is hosted by a sequence of mudstones, evaporites and tuffs, consisting of variable amounts of colemanite, calcium borate  $2\text{CaO} \cdot 3\text{B}_2\text{O}_3 \cdot 5\text{H}_2\text{O}$ , and lithium. Colemanite and lithium are the target minerals. Colemanite is a secondary alteration mineral formed from borax and ulexite. The mineral is semi-hard with a Mohs hardness of 4.5 and forms as discreet monoclinic, prismatic crystals or masses. Colemanite typically forms as a translucent colorless, white, or gray crystal with a vitreous luster. Colemanite is insoluble in water but soluble in HCl and sulfuric acid ( $\text{H}_2\text{SO}_4$ ). Colemanite is associated with thinly laminated siltstone, clay and gypsum beds containing an average of 9% calcite, 35% anhydrite plus 10% celestite ( $\text{SrSO}_4$ ) per Wilkinson & Krier, 1985. In addition to colemanite and celestite, elevated levels of lithium have been found through chemical analyses of drill samples. X-ray diffraction analysis of core samples from the deposit indicates the presence of the evaporite minerals anhydrite, colemanite, celestite, and calcite. The mineralogy of the detrital sediments include quartz, illite, feldspars, clinoptilolite, and zeolite. The deposit underlies massive clay beds which appear to encapsulate the evaporite ore body on all sides as well as above and below the deposit. This enclosed setting makes the deposit an ideal candidate for in-situ mining technology affording excellent containment of the leachate solution.

## 6.2 Mineral Deposit

Boron is believed to have been sourced from regional thermal waters which flowed from hot springs during times of active volcanism. These hot springs vented into the Hector Basin when it contained a large desert lake. Borates were precipitated as the thermal waters entered the lake and cooled or as the lake waters evaporated and became saturated

with boron. Colemanite, being the least soluble mineral, would evaporate on the receding margins of the lake. The evaporite-rich sequence forms a consistent zone in which the borate-rich colemanite zone transgresses higher in the section relative to stratigraphic marker beds.

Based on drilling results, the deposit is elliptical in shape, with the long axis trending N40°W to N50°W. extending over an area of about 606-acres at an average depth of approximately 1,300 ft to 1,500 ft bgs. Beds within the colemanite deposit strike roughly N45°W and dip about 10° or less to the southwest. Using an isoline of 5% B<sub>2</sub>O<sub>3</sub>, mineralization has an approximate width of 2,800 ft and a length of 11,150 ft with thickness ranging from 70 to 262 ft exclusive of barren interbeds.

The western margin of mineralization appears to be roughly linear, paralleling the Pisgah Fault which lies approximately 1 mi to the west (Figure 6.2). Duval geologists consider this boundary to be controlled by facies change from evaporite rich mudstones to carbonate-rich lake beds, because of syn-depositional faulting. The northeast and northwest boundaries of the deposit are controlled by facies changes to more clastic material, reducing both the overall evaporite content and the concentration of colemanite within the evaporites. The southeast end of the deposit is open-ended, and additional drilling is necessary to define the southeastern limits of borate deposition per Wilkinson & Krier, 1985.

### 6.3 Stratigraphic Column

Drilling of the deposit by Duval in the late 1970's and early 1980's defined the following lithological sequence (Figure 6.3 and Figure 6.4). Four major units have been identified:

- Unit 1: is characterized by a 490 to 655 ft thick sequence of red-brown mudstones with minor sandstone, zeolitized tuff, limestone, and rarely hectorite clay beds. Unit 1 is located immediately below the alluvium and surface basaltic lavas.
- Unit 2: is a green-grey mudstone that contains minor anhydrite, limestone, and zeolitized tuffs. Unit 2 has a thickness ranging from 330 to 490 ft and is interpreted as lacustrine beds.
- Unit 3: is a 245-to-490-foot thick evaporite section which consists of rhythmic laminations of anhydrite, clay, calcite, and gypsum. Unit 3 contains the colemanite mineralization. Thin beds of air fall tuff are found in the unit which provide time continuous markers for interpretation of the sedimentation history. These tuffs have variably been altered to zeolites or clays. Anhydrite is the dominant evaporite mineral, and the ore deposit itself is made up mostly of an intergrowth of anhydrite, colemanite, celestite, and calcite with minor amounts of gypsum and howlite.
- Unit 4: is characterized by clastic sediments made up of red and grey-green mudstones and siltstones, with locally abundant anhydrite and limestone. The unit is approximately 160 ft thick and rests directly on an irregular surface of andesitic lava flows. Where drilling has intersected this boundary, it has been noted that an intervening sandstone or conglomerate composed mostly of coarse volcanic debris is usually present.



Figure 6.3 Long-section and cross-section through the Fort Cady deposit

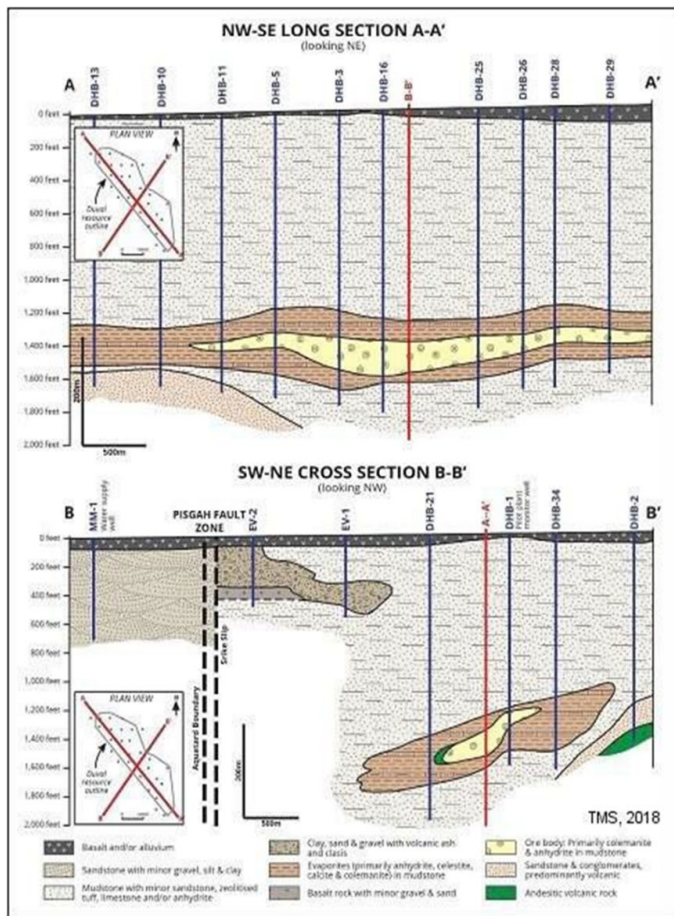
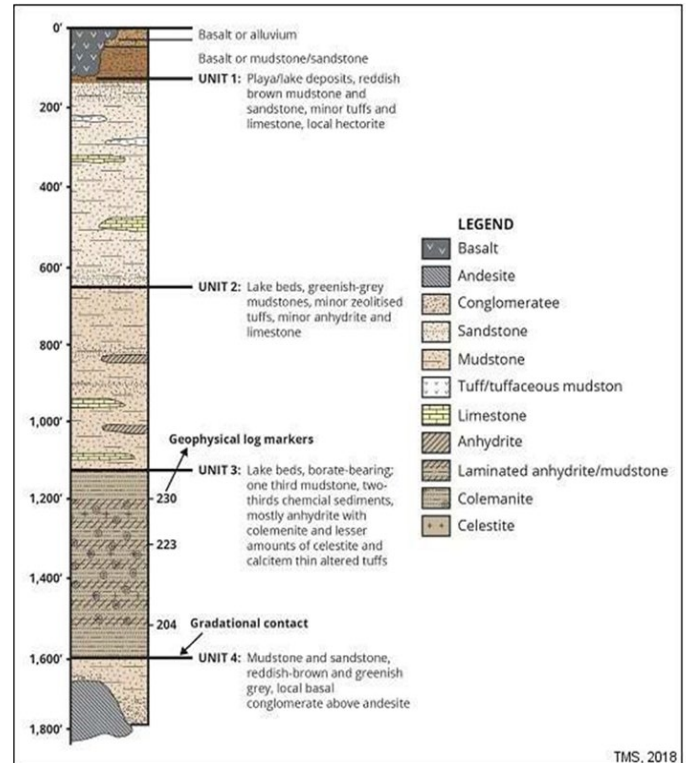


Figure 6.4: Generalized lithological column for the Fort Cady deposit



## 7 Exploration

### 7.1 Non-drilling exploration

Non-drilling exploration has not been deemed appropriate for this deposit.

### 7.2 Drilling

#### 7.2.1 Historic Drilling

As part of their exploration program, Duval completed 35 drill holes between 1979 and 1981. The DHB holes were drilled using a combination of rotary drilling through the overburden followed by core drilling through the evaporite sequence. DHB-32 was drilled as a water well southeast of the Project. Geologic logs of rotary cuttings and core were completed for all holes followed by geochemical analyses of the core. Duval paid particular attention during logging to identifying marker beds ash tuffs for correlation. In addition to geologic logging, down-hole geophysics were completed on 25 holes for gamma ray and neutron. A few holes had additional geophysical logs completed for compensated density, deviation, induction, elastic properties, and caliper.

In 1981 and 1982, after the exploration program, Duval drilled five solution mining test (SMT) wells which were used in injection/recovery (IR) tests. Like previous drilling, the wells were rotary drilled through the overburden and cored through the evaporite sequence. Following coring, a 5.5-inch casing was set through the cored interval. All SMT wells were logged, and analytical samples are available from the cored intervals of SMT-1, SMT-2, and SMT-3. Gamma ray and neutron logs were collected from all SMT wells. Caliper, compensated density, and induction logs were run on several,

but not all the SMT wells. Three additional SMT wells were established in 1992 and 1993 (SMT-92 & 93 Holes) and these three wells were rotary drilled to full depth and no geologic samples were collected.

FCMC completed two drilling campaigns during their participation in the Project. Additional P-Series holes were completed between 1987 and 1996 as rotary holes for injection/recovery test wells. Cuttings were sampled for analysis at 5-foot intervals for holes P-1, P-2, and P-3. A ten-foot sampling interval was used for sampling on P-4. No geologic samples were collected for holes P-5, P-6, and P-7. FCMC completed three S-Series wells in 1990. All three wells were rotary drilled and no geologic sampling was performed. FCMC completed down-hole geophysics on all the P and S-series wells. Historic drilling completed by Duval and FCMC is summarized in Table 7.1.

Table 7.1: Historic drilling summary

Drill Hole ID	UTM 83-11 m		Collar Elev. ft	Depth ft	Rotary Interval ft		Cored Interval ft		No. of Samples
	Easting	Northing			From	To	From	To	
DHB-01	553,336	3,846,154	2,004	1,623	—	1,090	1,090	1,623	187
DHB-02	554,062	3,846,179	2,033	1,679	—	955	955	1,443	—
DHB-03	553,089	3,845,899	1,980	1,773	—	940	940	1,773	214
DHB-04	552,855	3,845,669	1,981	1,708	—	1,194	1,194	1,708	178
DHB-05	552,848	3,846,153	1,978	1,730	—	1,043	1,043	1,730	179
DHB-06	553,115	3,846,386	2,008	1,616	—	1,040	1,040	1,616	125
DHB-07	553,736	3,845,492	2,000	1,735	—	1,063	1,063	1,735	181
DHB-08	552,575	3,846,214	1,966	1,809	—	1,072	1,072	1,809	186
DHB-09	552,391	3,846,408	1,967	1,750	—	1,137	1,137	1,750	138
DHB-10	552,349	3,846,631	1,980	1,655	—	1,148	1,148	1,655	86
DHB-11	552,599	3,846,390	1,976	1,671	—	1,150	1,150	1,671	86
DHB-12	552,824	3,846,402	1,993	1,625	—	1,130	1,130	1,625	85
DHB-13	552,104	3,846,877	1,978	1,661	-	1,140	1,140	1,661	70
DHB-14	553,089	3,846,151	1,987	1,631	—	1,105	1,105	1,631	80
DHB-15	553,580	3,846,158	2,013	1,609	—	1,177	1,177	1,609	51
DHB-16	553,263	3,845,595	1,985	1,845	—	1,193	1,193	1,845	138
DHB-17	552,843	3,845,925	1,982	1,804	—	1,178	1,178	1,804	151
DHB-18	553,238	3,845,431	1,978	1,880	—	1,212	1,212	1,878	106
DHB-19	554,141	3,845,287	2,034	1,460	—	1,060	1,060	1,460	74
DHB-20	553,006	3,845,437	1,998	1,671	—	1,207	1,207	1,671	—
DHB-21	553,292	3,845,143	2,011	1,752	—	1,118	1,118	1,828	39
DHB-22	553,275	3,845,902	1,988	1,711	—	1,196	1,196	1,711	135
DHB-23	553,508	3,845,110	2,021	1,857	—	1,208	1,208	1,857	114
DHB-24	553,523	3,845,637	1,994	1,780	—	1,202	1,202	1,780	119
DHB-25	553,699	3,845,297	2,021	1,818	—	1,248	1,248	1,818	152
DHB-26	553,891	3,845,056	2,050	1,702	—	1,106	1,106	1,702	106
DHB-27	553,698	3,844,803	2,043	1,795	—	1,228	1,228	1,795	95
DHB-28	554,004	3,844,943	2,053	1,690	—	1,185	1,185	1,690	115
DHB-29	554,164	3,844,454	2,040	1,610	—	1,203	1,203	1,610	101
DHB-30	553,873	3,844,630	2,050	1,720	—	1,250	1,250	1,720	83
DHB-31	553,865	3,844,381	2,037	1,460	—	1,195	1,195	1,625	41
DHB-32	551,770	3,843,845	2,045	870	—	870	—	—	—
DHB-33	554,045	3,844,254	2,043	1,601	—	1,124	1,124	1,860	80
DHB-34	553,746	3,845,722	2,116	1,525	—	1,150	1,150	1,620	79
DHB-35	551,249	3,848,166	2,068	1,449	—	1,194	1,194	1,459	—
P1	553,093	3,845,908	1,984	1,500	—	1,500	—	—	20
P2	553,094	3,845,969	1,984	1,510	—	1,510	—	—	21
P3	553,033	3,845,902	1,981	1,510	—	1,510	—	—	18
P4	553,033	3,845,935	1,977	1,510	—	1,510	—	—	34
P5	553,193	3,845,874	1,985	1,547	—	1,547	—	—	—
P6	553,209	3,845,946	1,989	1,525	—	1,525	—	—	—
P7	553,217	3,846,023	1,992	1,475	—	1,475	—	—	—
SMT-1	553,323	3,846,144	2,004	1,315	—	1,235	1,235	1,315	59
SMT-2	553,310	3,846,135	2,004	1,679	—	1,234	1,234	1,316	55
SMT-3	553,211	3,845,897	1,988	1,679	—	1,325	1,325	1,518	69
SMT-6	553,210	3,845,934	1,988	1,450	—	1,341	1,341	1,450	—
SMT-9	553,194	3,845,837	1,985	1,497	—	1,341	1,341	1,497	—

This data, along with company drilling discussed in Section 7.2.2 and subsequent analysis discussed in Section 8, form the basis and confirmations for the geologic model.

## 7.2.2 Company Drilling

After acquisition of the Project in May 2017, American Pacific Borates and Lithium, Ltd, a predecessor entity to 5E, completed 14 drill holes, which confirmed previous drilling results and expanded the Mineral Resource Estimate. Table 7.2 provides a summary of the 2017 drilling program. A cross-section through the deposit is also displayed in Figure 7.1. Drilling through the overburden sequence was completed using rotary air blast drilling. This was followed by drilling a 2.5-inch core through the evaporite sequence. All drill holes were completed vertically with no greater than five degrees of deviation.

Table 7.2: 2017 5E drilling summary

Drill Hole ID	UTM 83-11 m		Collar Elev. ft	Depth ft	Rotary Interval ft		Cored Interval ft		No. of Samples
	Easting	Northing			From	To	From	To	
17FTCBL-01	552,638	3,846,716	2,006	1,569	—	1,204	1,204	1,569	82
17FTCBL-02	552,711	3,846,490	1,997	1,509	—	1,208	1,208	1,509	107
17FTCBL-03	552,981	3,846,485	2,019	1,459	—	1,153	1,153	1,459	91
17FTCBL-04	552,695	3,846,268	1,978	1,738	—	1,266	1,266	1,738	162
17FTCBL-05	552,930	3,846,267	1,995	1,589	—	1,237	1,237	1,589	150
17FTCBL-06	553,145	3,846,260	2,002	1,502	—	1,189	1,189	1,502	83
17FTCBL-07	552,772	3,846,041	1,977	1,775	—	1,196	1,196	1,775	207
17FTCBL-08	552,972	3,846,042	1,984	1,625	—	1,202	1,202	1,625	153
17FTCBL-09	553,179	3,846,037	1,992	1,560	—	1,169	1,169	1,560	120
17FTCBL-10	552,831	3,845,939	1,989	1,647	—	1,208	1,208	1,647	176
17FTCBL-11	553,078	3,845,899	1,983	1,778	—	1,332	1,332	1,778	155
17FTCBL-12	552,963	3,845,801	1,973	1,750	—	1,281	1,281	1,750	212
17FTCBL-13	553,153	3,845,818	1,992	1,769	—	1,313	1,313	1,769	155
17FTCBL-14	553,270	3,845,608	1,987	1,845	—	1,328	1,328	1,845	260

Core logging was completed on all drill holes and included lithological and geotechnical logging. Downhole geophysical logs included Gam Ray, Induction, and standard caliper, and were completed on all drill holes from surface to total depth except for 17FTCBL009 where adverse hole conditions resulted in only partial geophysical logging. All core is logged and photographed according to industry standard procedures. An example of core photos is shown in Figure 7.2.

A geotechnical drill hole, APBL023, was also completed in 2017. This well was cored for its entire length and a geologic log was completed to define mineralized horizons. No splitting or analytical samples were collected from this hole to preserve the core for subsequent geotechnical testing.

In 2022, 5E drilled 13 wells as part of a monitoring well and testing program. One well, IR2-01-01, was cored and assayed and subsequently added to the drilling database as outlined in Table 7.3.

In 2023, three observation wells, OW-9, OW-10, and OW-11 were completed as part of the permitting process with the EPA. Down-hole geophysics were completed on the three wells. Rotary cuttings from the wells were logged and assayed and subsequently included into the drilling database.

The QP considers the drilling program by 5E to be of sufficient quality to support a Mineral Resource Estimate.

Table 7.3: Recent 5E Drilling

Drill Hole ID	UTM 83-11 m		Collar Elev. ft	Depth ft	Rotary Interval ft		Cored Interval ft		No. of Samples
	Easting	Northing			From	To	From	To	
IR2-01-01	552,472	3,845,807	2,006	1,931	—	1,079	1,079	1,931	135
OW-9	553,364	3,845,874	1,972	1,527	—	1,527	—	—	46
OW-9	553,619	3,845,692	1,979	1,800	—	1,800	—	—	44
OW-11	552,669	3,845,877	1,978	1,538	—	1,538	—	—	41

Figure 7.1: Cross-section through the Fort Cady deposit

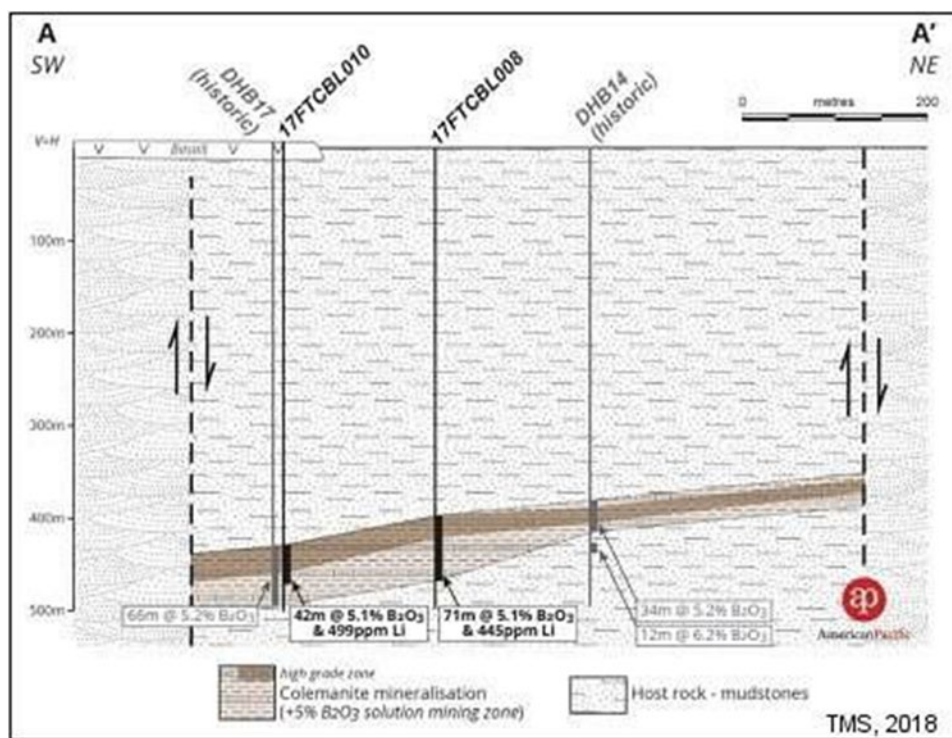


Figure 7.2: Core photo, 17FTCBL-014





## 7.3 Hydrogeology

### 7.3.1 Hydraulic Setting

The Project deposit is in the California Groundwater Bulletin 118 Unit Basin 14 Lavic Valley, and Hydrologic Unit 12 sub-basin 180902081303. There is no name associated with the sub-basin and it is located north and west of the Lavic Lake and town of Lavic hydrologic sub basins. Basin 180902081303 is approximately 39,657 acres (160.48 square kilometers) in area and extends from the Rodman Mountains south and west of the Project in a north direction towards Highway 40, terminating at a topographical divide at the highway. The basin is bound to the south and east by the Pisgah Crater and Lavic Lake Volcanic Field.

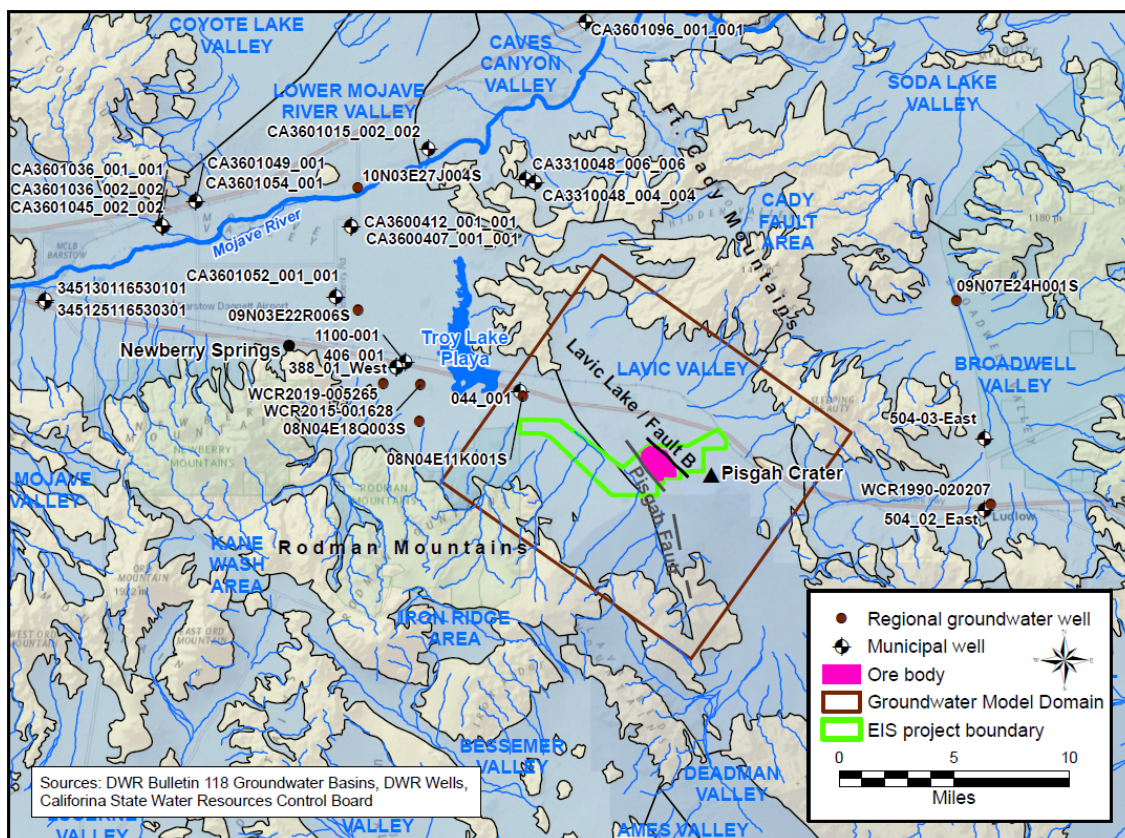
The Fort Cady Mountains constrain Basin 14 to the north and the Rodman Mountains and Lava Bed Mountains constrain Basin 14 to the south of the Project. The groundwater flow in the Lavic Valley alluvial basin is generally west towards the Mojave River, but in the project area is poorly defined. The basin outflow is interpreted to occur to the east of Broadwell Valley, with no localized groundwater discharge such as evapotranspiration or discharge to springs or a river.

The mineral deposit is bounded to the west by the Pisgah Fault and to the east by subordinate faults that include Fault B. See the UIC permit application and the Confluence Water Resources CWR, 2019 Fault B Program Results, Technical Report.

The nearest industrial well, owned by Candeo Lava Products, is 3.5 miles east of the Project ore body. No other water wells are known to exist within the vicinity of the Project. Water level measurements from the Candeo Lava Products well are not currently available but are greater than 96 ft bgs based on the CWR investigation in 2018. The next closest water well is located north and west of the Project at the Desert Oasis Highway Rest Stop providing non-potable water to the rest stop facilities. This well is located approximately 7-miles northwest of the Project. The depth to water from the Rest Stop Well (Well 1807), was measured by CWR to be 54.75 ft bgs, at an approximate elevation of 1,758 ft amsl.

The nearest municipal well is screened in the valley alluvium, west of the Pisgah fault and approximately five miles northwest of the ore body (Figure 7.3).

Figure 7.3: Project area groundwater basins and surrounding area wells, Fort Cady Project



Private domestic wells are associated with rural residences located greater than 6.5 miles west of the Project on the eastern edge of the town of Newberry Springs. Irrigation wells are located further west, the closest of which is approximately 10 miles west of the Project. The Pisgah Fault separates these residential and irrigation wells from the Project area, such that they are not within the same regional groundwater flow system and are not hydraulically connected.

The Project is located within a closed basin. Although surface water is rarely present in the vicinity of the Project, when it occurs, flow is in a northwesterly direction past the Project area from the Rodman Mountains and the Pisgah Crater topographic divide. There are no perennial springs or streams in the vicinity of the Project. Surface water-related features are seasonal, and ephemeral in response to meteorological events. These features consist of unnamed dry washes that may carry water during heavy storm events generally draining west through the Project area toward the Troy Lake playa in Newberry Springs.

### 7.3.2 Project Area Groundwater Levels

The orebody is “wedged” between the Pisgah Fault and Fault B. The static depths to groundwater in the vicinity of the orebody generally range between 240 and 350 ft bgs. Prior to injection in 2024, the measured groundwater elevation in the wedge ranged from approximately 1,500 ft amsl at MW-3A to 1,720 ft amsl at AOR-3A, although many wells were still recovering from fluid evacuation during drilling. Injection and recovery in the IR well beginning in January 2024 has caused pressure fluctuations in two wells, OW-6A and all three screens of OW-10 (nested well). The pressure response from injections causes water level fluctuations of about 35 ft in OW-6A which is about 1000 ft away from the IR wells. The deepest screen of OW-10 fluctuates ~50 ft while the middle and shallow screen fluctuate ~100 ft in response to injection and recovery at the IR wells. The water levels in the remaining wells do not show a response to injections and are either still recovering or remaining relatively flat.

The groundwater elevation outside the wedge, west of the Pisgah Fault in the quaternary alluvial fan sediments of the Lower Mojave River Valley Groundwater Basin is approximately 1,785 ft amsl in Project wells MWW-1, MWW-S1, and MWW-2.

The difference in groundwater elevation between Project wells presents a steepening of the gradient from west to east across the Pisgah Fault. There is approximately a 30 – 40 foot water level differential on the east and west sides of the Pisgah Fault, which is regionally recognized as a barrier to groundwater flow and represents one of the groundwater basin boundaries.

Groundwater in the vicinity of Fault B at Project wells TW-1, PW-1, and PW-2, is approximately 350 to 390 ft bgs in the coarser alluvial sediments to the east of Fault B (PW-1 and PW-2) and in a mix of alluvial and fine playa sediments to the west of Fault B (TW-1).

Monitoring wells drilled in 2021 by 5E as part of permit compliance did not encounter groundwater above the Unit 4 sediments except for a perched groundwater zone localized in fine sand lenses underlying surficial basalt above the contact with Unit 1. The results of the Shallow Groundwater Characterization Program, CWR, June 2022, *Shallow Groundwater Characterization Report on Mining Block 2 Near Pisgah Fault*, indicated that groundwater encountered during drilling of the Series 7 wells is of low yield, poor quality and probably low storage capacity.

Recharge to the perched zone originates from precipitation occurring in the Lava Bed Mountains, and drainage from Sunshine Peak, located southwest of the project. The upgradient precipitation drains into the shallow alluvium southwest of the Pisgah Fault with shallow groundwater flowing in a northeasterly direction through unconsolidated alluvial sediments, before draining under the basalt flow at a gradient of 0.002 ft/ft into cemented sandstone and mudstone, where it is compartmentalized within the lithology and controlled by fault B. Interpretation of chip logs for all Series 7 and Series 3 wells, and the WSW and WMW wells, indicate the shallow cemented sandstone is not uniform, decreasing in depth to the east of the project, where the mudstone is encountered higher in most wellbores due to either pre-basalt flow topography and/or offset from faulting.

Since shallow groundwater was not encountered or observed during drilling of the Series 3 monitor wells, the Pisgah Fault is interpreted as being a strong influence on the shallow groundwater system flow dynamics, influencing the groundwater quality in Block 2. The lateral extent of the shallow groundwater system is anticipated to be confined to within the area underlying the surface basalt near the Series 7 wells to the extent of the Pisgah Fault zone northwest of the Project.

The Pisgah Fault compartmentalizes the shallow groundwater system's lateral extent within the western Project area and is not the source of shallow groundwater.

Below Unit 4 is the Unit 5 andesite where groundwater was encountered in MW-3B. CWR, March 12, 2023, CWR Technical Memorandum, *Results of OW-3A and MW-3B Hydraulic Testing, Fort Cady California Project*, describe the results of groundwater testing between Unit 4 and the underlying andesite. The results of air lift testing found that the Unit 5 groundwater is under a highly confined pressure demonstrating that Unit 4 is an aquiclude up to 150 ft thick, preventing percolation of groundwater from Unit 3 to Unit 5. The current conceptual model indicates that recharge in the deep bedrock is extremely slow. This is particularly true between the Pisgah Fault and Fault B, where inflow from precipitation recharge through the alluvium or inflow from adjacent bedrock is minimal due to the bounding faults

Proven water resources have been deemed acceptable through Phase 1 of the Project.

### 7.3.3 Hydrogeology External to the Ore Block

The hydrology east of Fault B, approximately 3,500 ft east of the colemanite deposit was analyzed by CWR (2018) that found, 1) a significant groundwater resource east of Fault B, and 2) that the fault is a barrier to groundwater flow. Stable isotope analytical results compared against Nevada Meteoric Water Lines appropriate for desert terrains found that the aquifer east of Fault B and the aquifer west of the Pisgah Fault have different origins, while the limited groundwater between the two faults is of a different origin than both aquifers. Recovery rates from wells between the two faults, which includes the colemanite deposit, are less than one gpm as would be expected in mudstones and claystone with very limited groundwater present.

### 7.3.4 Formation Hydraulic Properties

Testing for hydraulic properties of the colemanite and evaporates/mudstones containing the colemanite have occurred on several occasions. Based on the pump test results in mudstone and claystone sediments above and below the ore body evaporites, CWR (2019) estimated hydraulic conductivity to be approximately  $10^{-5}$  ft/day, a very low value. Additionally, a majority of the monitoring wells have been recovering since development and have not reached a steady state value after 3+ years, a clear indicator of limited water in the confining units and low hydraulic conductivity.

The results of the testing in OW-3A indicate the contact between Units 2 and 4 is extremely low permeability, with K approximately  $4.3 \times 10^{-5}$  feet/day. Testing in MW-3B indicates the permeability of the underlying andesite is three orders of magnitude higher, approximately  $8.9 \times 10^{-2}$  feet/day (CWR, March 12, 2023, Results of OW-3A and MW-3B Hydraulic Testing, Fort Cady California Project).

#### 7.3.4.1 Duval 1980-1982

Beginning in 1980, Duval retained Core Laboratories, Inc. to run injectivity tests on one-inch cores from borehole SMT-1. The samples were extracted with toluene, salts leached with cool methanol and dried in a controlled humidity oven. Permeability to air and Boyle's Law porosity were determined for each sample.

The injectivity tests were run at the reservoir temperature of (simulated) formation water (120° F) which flowed through the core until equilibrium occurred, and a minimum of three pore volumes had been injected. Sulfuric acid and hydrochloric acid solutions were injected through the core samples after which the permeability to acid solutions was determined.

In the 1981 testing, injection pressures were up to 1,250 psi, with flow velocities predominantly  $10^7$  cm/sec with groundwater, increasing to  $10^5$  cm/sec with acid concentrations between 10-20%, indicative of the hydraulically tight nature of the claystone hosting the deposit.

While detailed information on the Core Lab testing procedures is available, quality assurance and quality control (QA/QC) procedures are not.

Based on the colemanite content in the sediments and laboratory core analyses, the end-point porosity of the ore body formation after mining was predicted by Core Lab in 1981 to be 15-19%.

#### *7.3.4.2 In-Situ 1990*

A field pilot test found that the initial permeability ranged from  $1.35 \times 10^{-9}$  to  $2.9 \times 10^{-10}$  cm/sec as part as a multiple well constant rate injection test to determine the directional tendencies of hydraulic properties in the mineral deposit. In-Situ also investigated the effects of prior injection/recovery testing using a Badger flow meter, a HERMIT data logger, and pressure transmitters. The water-level responses were measured in the injection well and six nearby observation wells and the Cooper and Jacob method used to analyze data from each well and the Papadopoulos Method to determine directional permeability. The results confirmed the earlier work that the permeability and transmissivity of the deposit are low.

#### *7.3.4.3 Hydro-Engineering 1996*

This analysis summarized some of the testing and provided interpretations of prior testing in 1981 and 1990. The mineralized sequence of rock transmissivity is estimated at 10 gal/day/ft, or 1.3 ft<sup>2</sup>/day. Assuming that the colemanite mineralized sequence occurs over an approximate 300 ft thickness, then the native hydraulic conductivity (K) was estimated at  $4.5 \times 10^{-3}$  ft/day, similar to that of Simon Hydro-Search 1993 of  $8.2 \times 10^{-3}$  to  $2.2 \times 10^{-2}$  ft/day K converted from millidarcy units. The storage coefficient (S) of the ore body was also estimated by Hydro-Engineering 1996 to be at  $2.5 \times 10^{-6}$ .

Increases in the transmissivity, hydraulic conductivity and storage coefficient will occur as colemanite is dissolved from the formation. Hydro-Engineering, 1996, estimated that the end-point permeability of the ore body formation after colemanite dissolution would be approximately 30 times higher, with a long-term storage coefficient of approximately  $1.1 \times 10^{-5}$ . The end-point hydraulic properties are still low because much of the formation is evaporites, anhydrite, and claystone that will not be dissolved.

#### *7.3.4.4 Geomega 2023*

Geomega analyzed step rate testing completed in the IR wells in block two in 2023. The step rate tests resulted in an average formation fracture pressure of 917 psi and a formation fracture gradient of 0.69 psi/ft, well aligned with prior estimates of 0.65 to 0.76 psi/ft from the Duval 1983 pilot tests. Further analysis of the data indicated that permeability ranged from 0.5 to 2 millidarcies with total porosity ranging from 27% to 34%, aligned with prior low permeability estimates.

### **7.3.5 Water Quality Compliance Monitoring**

Routine sampling of monitoring wells is ongoing for water quality purposes, with OW-6A specifically used to monitor the movement of mining related solutions. While monitoring wells installed closer to the IR wells in late 2024 do not have enough data yet to determine mining related impacts (there is a wide range of natural variability in the ore body), none of the monitoring wells show definitive indications of mining related solution impact as of Q2 2025.

## 8 Sample Preparation, Analysis and Security

### 8.1 Sampling Method and Approach

Between September 2017 and October 2017, 14 holes for a total of 23,111 ft were completed as part of a confirmatory resource drilling program. Assay results from all 14 drill holes were used in the mineral resource estimate. There are 2,113 samples from the 2017 drilling program representing 1,713 ft of core. In conjunction with the 2017 drilling program, 29 historical drill holes completed by Duval and four holes completed by FCMC have been utilized in the mineral resource estimate. There are 3,672 samples from the historic drilling representing a cumulative total 10,831.3 ft of core. The QA/QC procedures for the historic drilling are unknown though the work products compiled during the historic drilling suggest it was carried out by competent geologists following procedures considered standard practice at that time.

Discussions held with Pamela A.K. Wilkinson, who was an exploration geologist for Duval at the time of drilling and sampling, indicate that Duval had internal quality control and quality assurance procedures in place to ensure that assay results were accurate. Duval utilized their Tucson, West Texas Culberson Mine or New Mexico Duval Potash Mine laboratories for analytical work carried out at the Project. Geochemical analyses were carried out using X-Ray Fluorescence Spectrometry (XRF). XRF results were reportedly checked against logging and assay data.

Entire core sequences were sampled. Sample intervals were determined at the time of logging based on changes in lithology, mineralogy, and bedding. Sample intervals range from 0.2 to 6.6 ft with an overall average sample length of 2.66 ft. Following determination of sampling intervals, the core was split in half using a core splitter. One half of the core is used for the analytical sample with the remaining half core being returned to the core box for archiving. Samples are then placed into labeled plastic sample bags along with a pre-numbered sample tag. A companion sample tag is placed back in the core box marking the interval sampled. Samples were dispatched by commercial carrier to the Saskatchewan Research Council (SRC) for geochemical analysis. SRC has been accredited by the Standards Council of Canada and conforms with the requirements of ISO/IEC 17025:2005.

Identical sampling procedures were followed in 2022 for IR2-01-01. One hundred thirty-five (135) samples were collected from IR2-01-01 and dispatched to SRC for analysis.

For observation wells OW-9, OW-10 and OW-11, 131 chip samples were collected on 1.0 to 16 ft. intervals with the most samples through the mineral horizons at 10 ft. lengths. Sample splits weighing approximately 640 grams were dispatched to SRC for analysis.

### 8.2 Sample Preparation, Analysis and Security

Upon receipt of samples from 5E, SRC would complete an inventory of samples received, completing the chain of custody documentation, and providing a ledger system to APBL tracking samples received and steps in process for sample preparation and analysis. Core samples and chip samples are dried in their original sample bags, then jaw crushed. A subsample is split out using a sample riffler. The subsample is then pulverized with a jaw and ring grinding mill. The grinding mill is cleaned between each sample using steel wool and compressed air or by using silica sand. The resulting pulp sample is then transferred to a barcode labeled plastic vial for analysis.

All samples underwent a multi-element Inductively Coupled Plasma Optical Emission Spectroscopy (ICP-OES), using a multi-acid digestion for Ag, Al<sub>2</sub>O<sub>3</sub>, Ba, Be, CaO, Cd, Ce, Cr, Cu, Dy, Er, Eu, Fe<sub>2</sub>O<sub>3</sub>, Ga, Gd, Hf, Ho, K<sub>2</sub>O, La, Li, MgO, MnO, Mo, Na<sub>2</sub>O, Nb, Nd, Ni, P<sub>2</sub>O<sub>5</sub>, Pb, Pr, Sc, Sm, Sn, Sr, Ta, Tb, Th, TiO<sub>2</sub>, U, V, W, Y, Yb, Zn, and Zr. Boron was also analyzed by ICP-OES but undergoes a separate digestion where an aliquot of the sample is fused in a mixture of Na<sub>2</sub>O<sub>2</sub>/NaCO<sub>3</sub> in a muffle oven, then dissolved in deionized water, prior to analysis. Major oxides Al<sub>2</sub>O<sub>3</sub>, CaO, Fe<sub>2</sub>O<sub>3</sub>, K<sub>2</sub>O, MgO, MnO, Na<sub>2</sub>O, P<sub>2</sub>O<sub>5</sub> and TiO<sub>2</sub> are reported in weight percent. Minor, trace, and rare earth elements are reported in parts per million (ppm). The detection limit for B is 2 ppm and 1 ppm for Li.

For the 2017 drilling program and IR2-01-01 in 2022, a total of 2,253 core samples and 441 control samples were submitted for multi-element analysis to SRC. 5E submitted control samples in the form of certified standards, blanks and coarse duplicates bags with sample identification supplied by 5E for SRC to make duplicate samples. In addition to these control samples, SRC also submitted their own internal control samples in the form of standards and pulp duplicates. A summary of all the QA/QC control samples submitted to SRC is shown in Table 8.1. Only the internal control samples provided by SRC were included with rotary chip samples from the observation wells drilled in 2023.

Table 8.1: Summary of QA/QC control samples

Submitted By	Drilling Type	Number of Holes	Meters Drilled	Standards	Blanks	Coarse Duplicates	Pulp Duplicates	Total Frequency	Primary Samples	Total
5E	Rotary	15	5,284.24	—	—	—	—	—	—	—
	Diamond Tail	—	—	—	—	—	—	—	—	—
	Tail	15	2,472.85	153	143	144	—	—	2,253	2,693
	Total	15	7,757.09	153	143	144	—	—	2,253	2,693
	Frequency			5.68%	5.31%	5.35%	—	19.10%	83.66%	100%
SRC	SRC Internal QAQC			151			82			
	Frequency			7.10%			3.90%	11.00%		

Certified standards SRM 1835 and SRM 97b, prepared by the National Institute of Standards and Technology, were submitted as part of the APBL QA/QC procedures, the results of which are shown graphically on Figure 8.1 and Figure 8.2. Standard deviations shown are for the SRC assays. No two standards in any single batch submission were more than two standard deviations from the analyzed mean, implying an acceptable level of precision of SRC instrumentation.

Figure 8.1: Assay results of Standard SRM1835

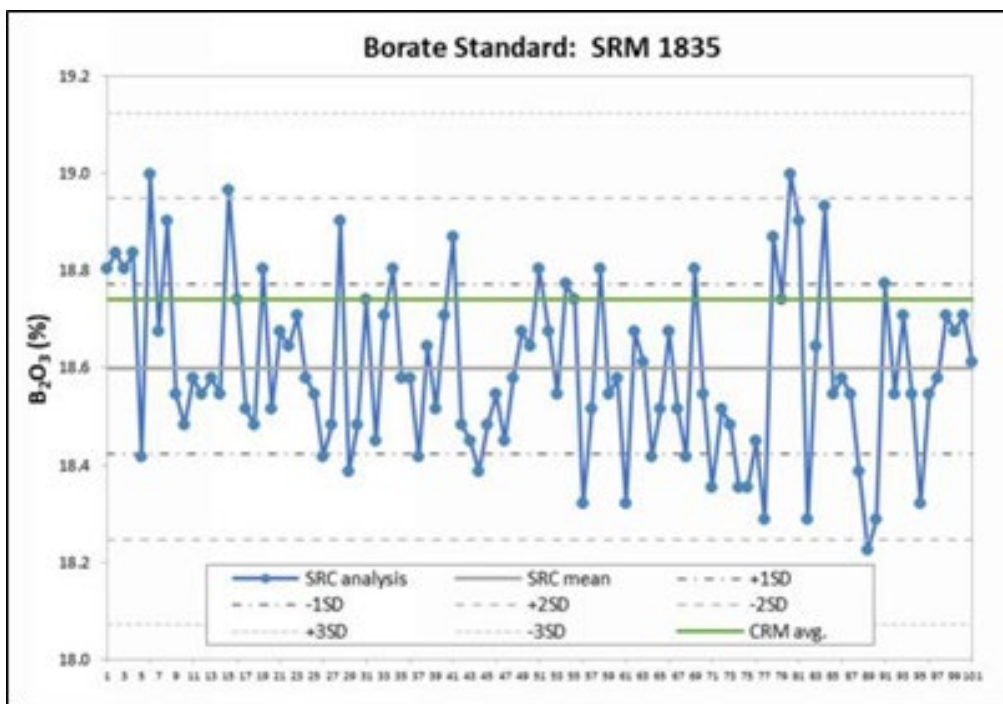
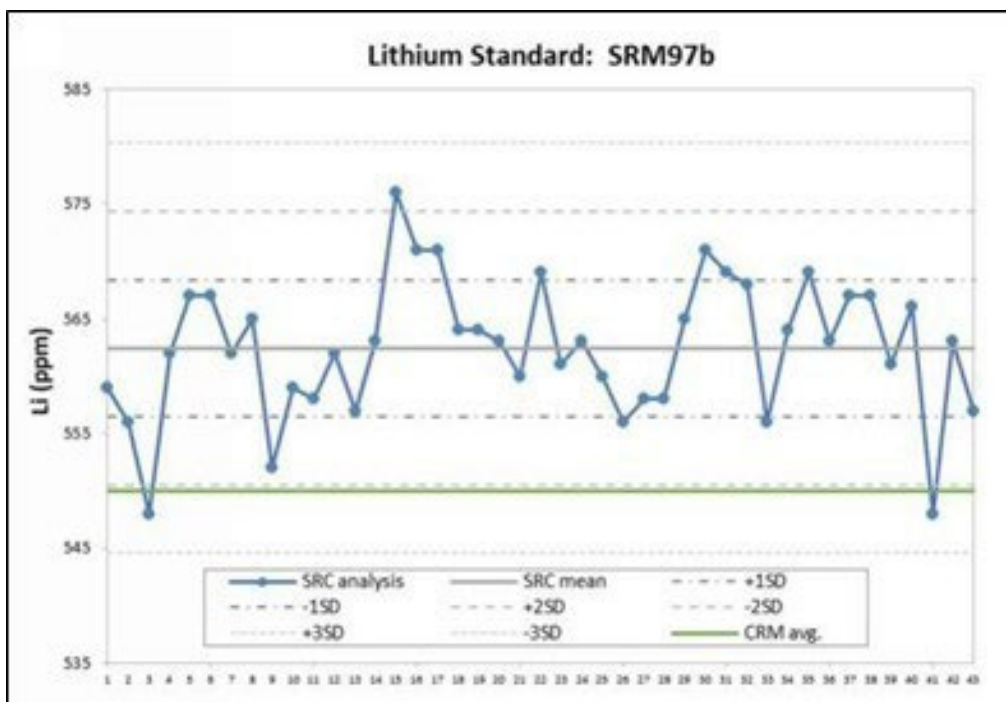




Figure 8.2: Assay results of Standard SRM97b



SRC assayed two different standards, CAR110/BSM and CAR110/BSH, for its own QC protocol. CAR110/BSM is designated as a “medium boron standard.” CAR110/BSH is designated as a “high boron standard.” Figure 8.3 and Figure 8.4 display the analytical results for the certified standards. The analytical precision for analysis of both CAR110/BSM and CAR110/BSH is also reasonable, with no two standards in any single batch submission being more than two standard deviations from the analyzed mean.

Figure 8.3: Assay results for SRC Standard CAR110/BSM

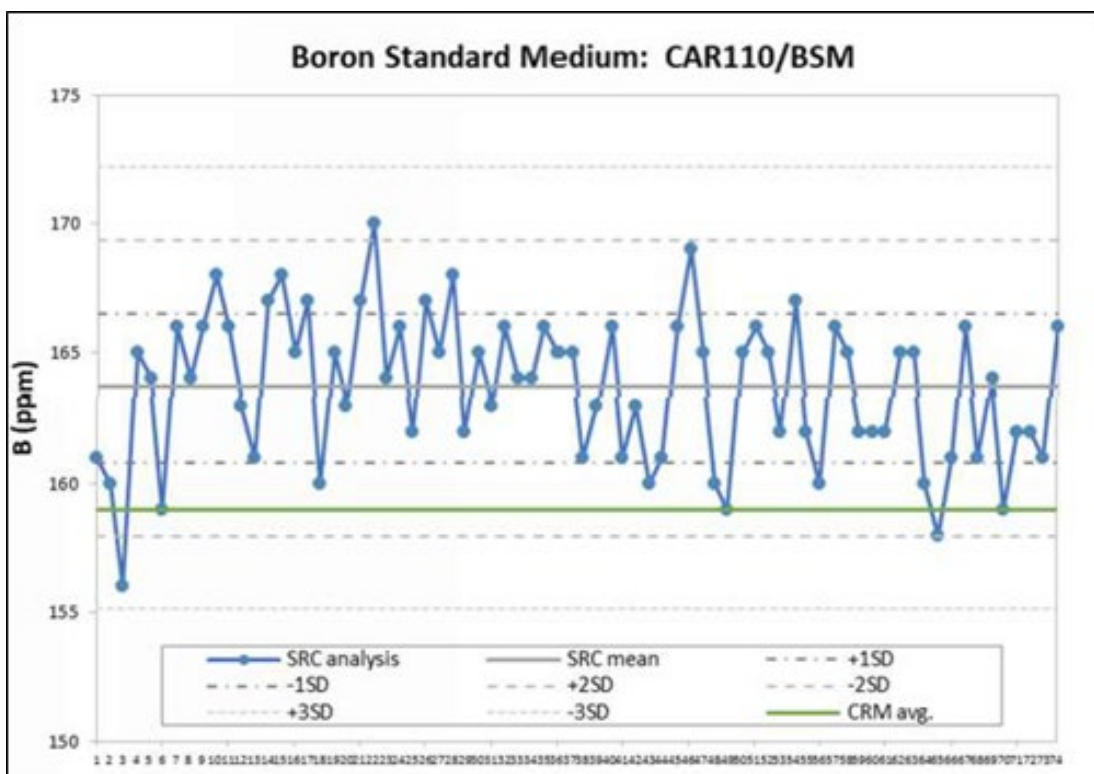


Figure 8.4: Assay results for SRC Standard CAR110/BSH

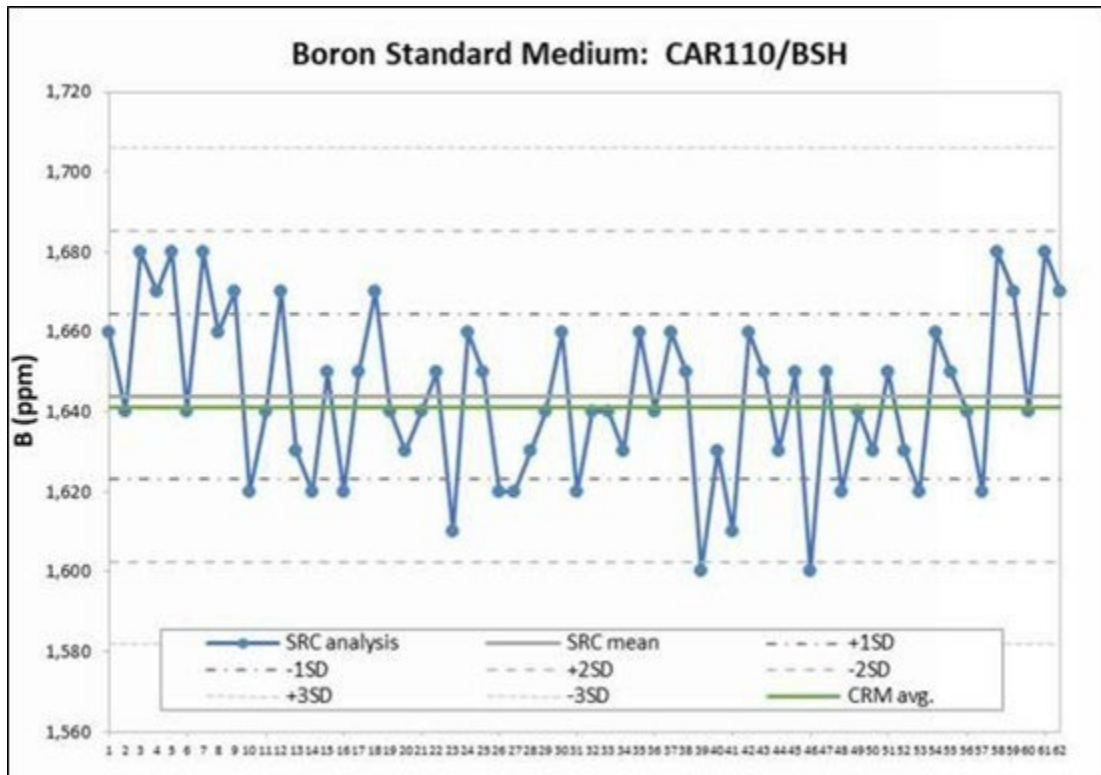
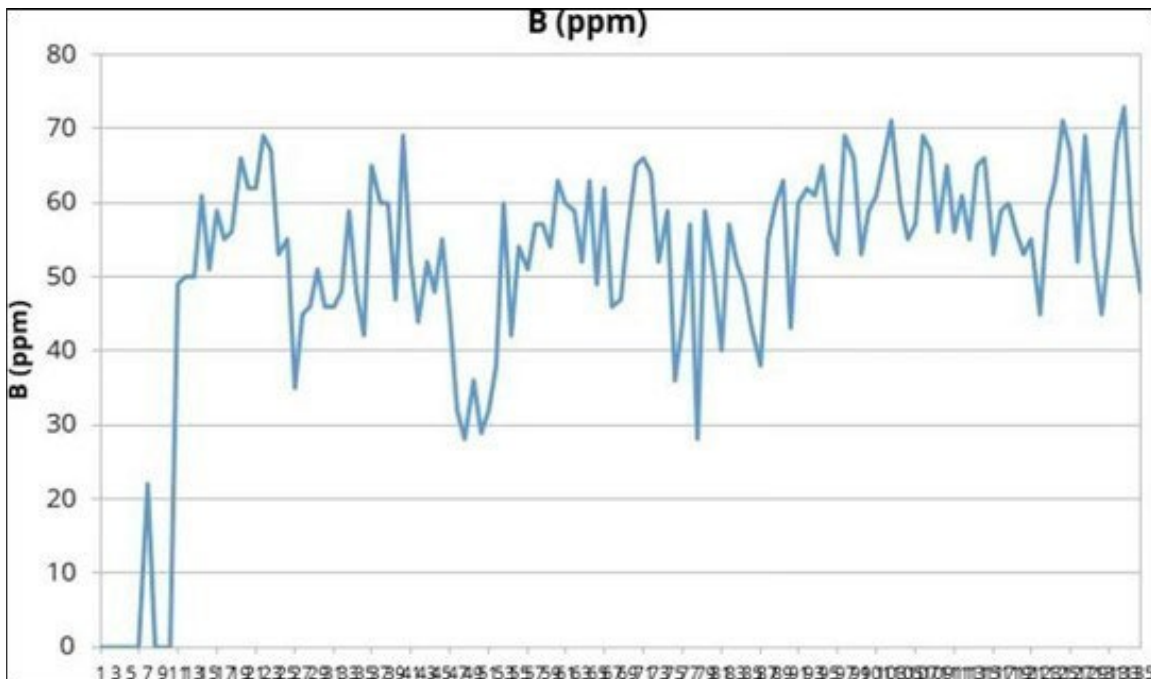


Figure 8.5: Sample blank assay results for boron

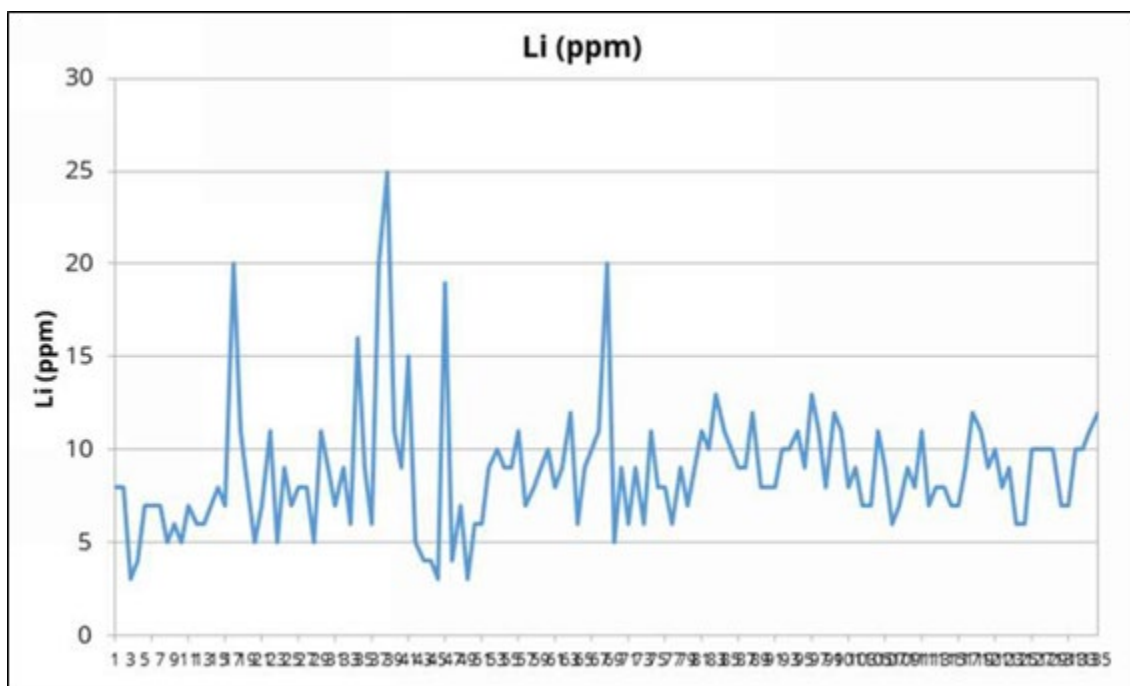


Blank samples inserted by 5E consisted of non-mineralized marble. One hundred and thirty-five blank samples were submitted, all of which had assay results of less than 73 ppm B. The level of boron detected in the blanks is likely sourced from pharmaceutical borosilicate glass used during sample digestion. These boron concentrations are considered immaterial in relation to the boron levels detected in the colemanite mineralization and do not appear to represent carryover contamination from sample preparation. Lithium levels in the blank samples are also at acceptable



levels with many assays <15 ppm Li. The four highest Li levels in the blanks immediately followed samples that contained relatively high Li concentrations. Overall, the concentration of the primary elements of interest B and Li in the blanks are at levels considered to be acceptable, implying a reasonable performance for sample preparation. The results of the blanks for B and Li are plotted in Figure 8.5 and Figure 8.6.

Figure 8.6: Sample blank assay results for lithium



A total of 136 duplicate samples were submitted to the SRC. 5E commissioned SRC to compose coarse duplicate samples using a Boyd rotary splitter. Figure 8.7 and Figure 8.8 show the assay results of duplicate samples for B and Li. As can be seen from the regressions, there is a good correlation between original and duplicate samples.

Figure 8.7: Duplicate sample results for boron

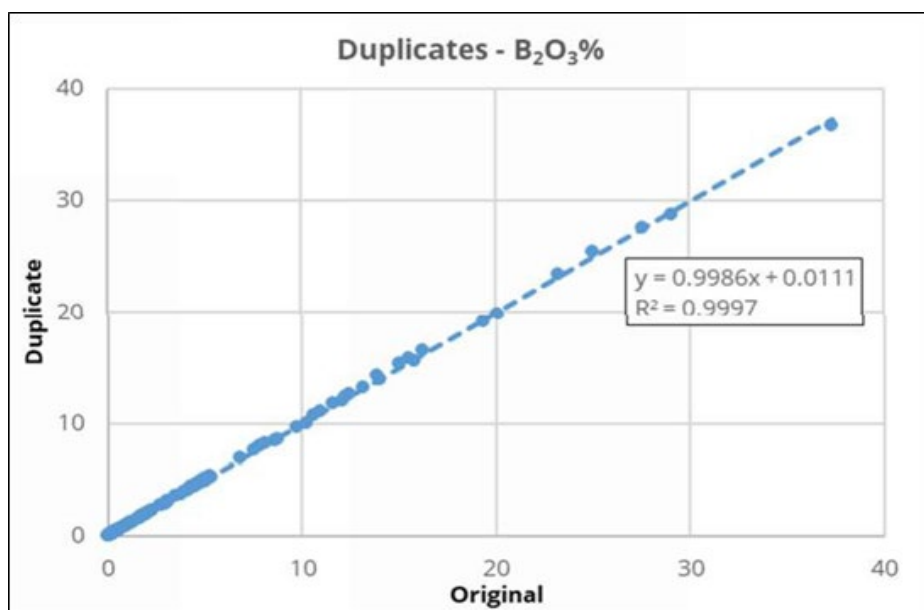


Figure 8.8: Duplicate sample results for lithium

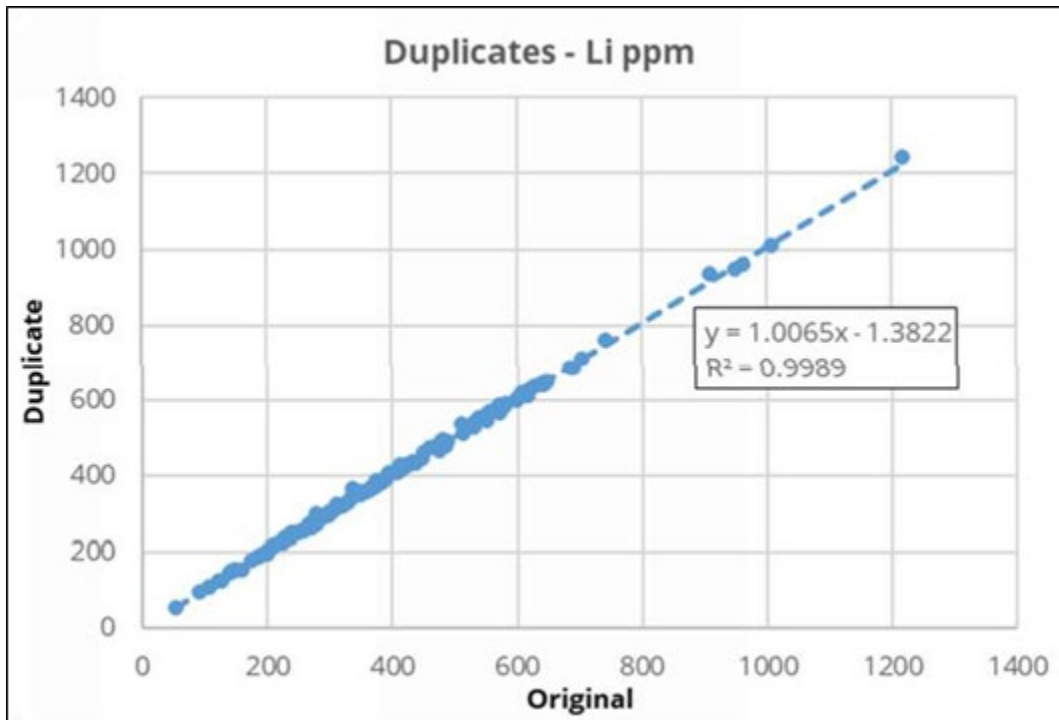


Figure 8.9 displays a HARD half absolute relative difference plot for the duplicates. This highlights reasonable precision for the duplicates. Regression and HARD results were also plotted for pulp duplicates assayed in SRC's own QC protocol shown in Figure 8.10 and Figure 8.11. These also show a reasonable level of precision.

Figure 8.9: HARD diagram for 5E duplicate samples

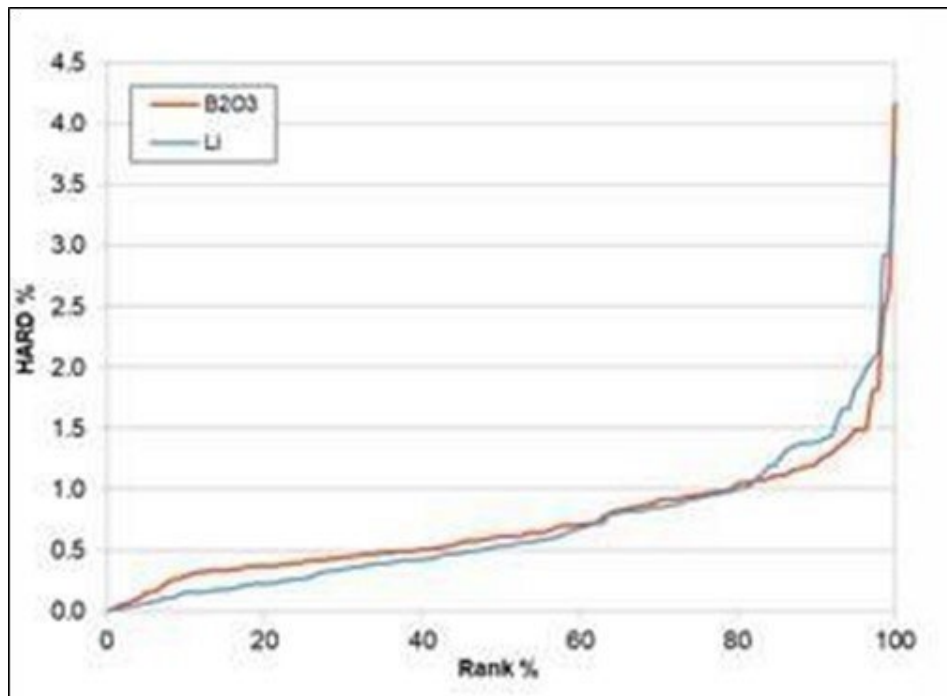


Figure 8.10: SRC duplicate results

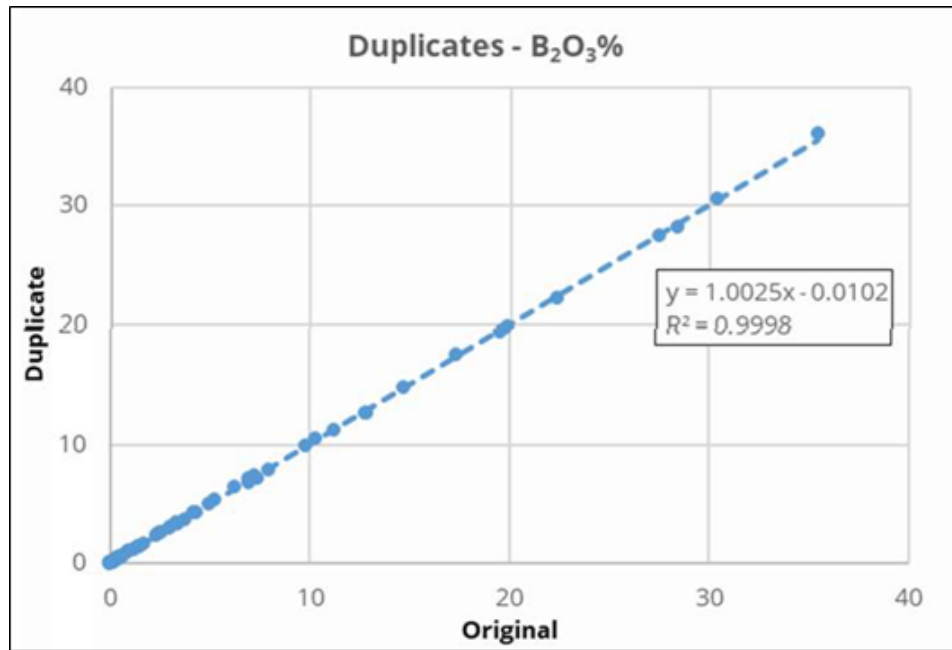
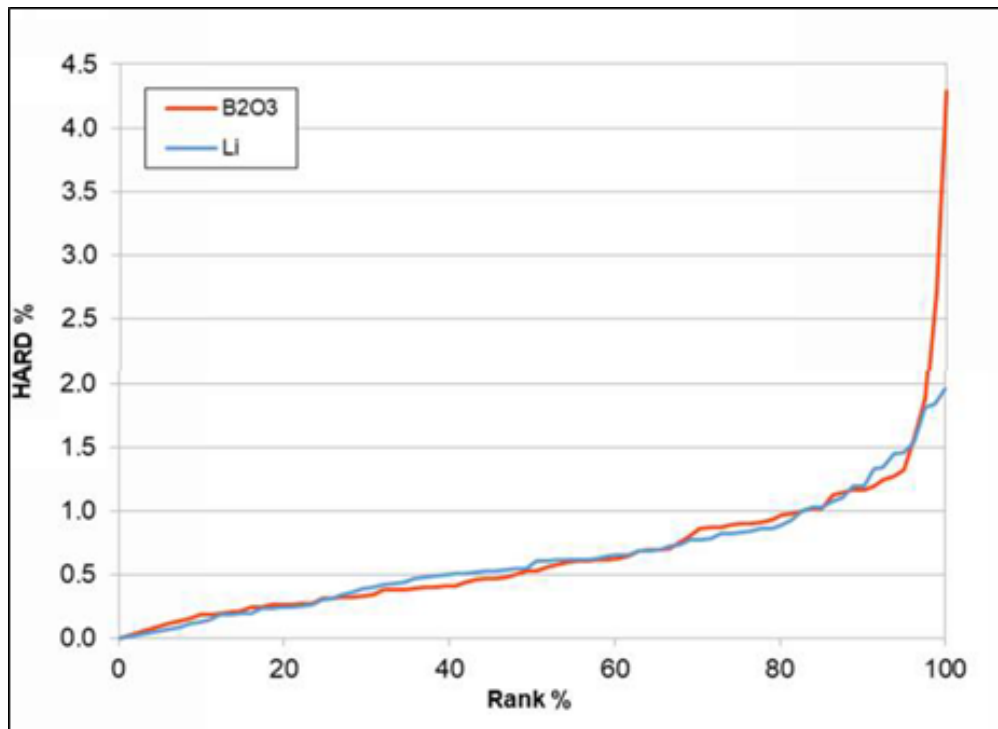


Figure 8.11: SRC duplicates HARD diagram



The QP believes reasonable care has been taken to collect and dispatch samples for analysis. The QA/QC program has shown that the analyses are viable with a minimum of dispersion or contamination errors. The QP considers the sampling program to be of sufficient quality to support a mineral resource estimate.

## 9 Data Verification

### 9.1 Data Verification Procedures

During a site visit, the QP examined the core and also visited the site in 2024. Core has been safely stored in a designated storage building near the mine site office and is in good condition. The QP examined the core and compared the core to the geologic logs and sample interval records and found good agreement with the log descriptions and with no discrepancies with sample intervals.

The QP has done a visual check of drilling locations through Google Earth. Drill sites from the 2017 drilling program are still visible in imagery. Older sites completed by Duval and FCMC are not discernible on imagery.

Historic drilling location records were originally recorded in California State Plane coordinates or in metes and bounds. The QP checked historic drilling location data to ensure these records had been properly converted to Universal Transverse Mercator (UTM) coordinates, the coordinate system used in the 2017 drilling program. All historic location data has been properly converted to the current UTM coordinate system.

The QP received drilling records, sample intervals, and assay results in excel workbook files that were used as input for the drill hole database. Through a variety of data checks drill hole information was evaluated for duplicate entries, incorrect intervals, lengths, or distance values less than or equal to zero, out-of-sequence intervals and intervals or distances greater than the reported drill hole length. Historical drill hole records were also checked against relevant Duval and FCMC data sets. A review comparing original field logs and assay reports showed the data to have been transcribed accurately into the Excel files.

### 9.2 Data Limitations or Failures

The QP did not identify any data limitations or failures.

### 9.3 Data Adequacy

The QP believes adequate care has been taken in preserving and transcribing the historic data to digital format and drill hole data accurately corresponds back to the sample ledger and assay certificates. The QP believes that the data used is adequate and suitable for a mineral resource estimate.

## 10 Mineral Processing and Metallurgical Testing

This section summarizes at a high level the overall metallurgical program and flowsheet development work completed during the PFS. This test work validates the selected options of the PFS flowsheets.

The most recent phase of metallurgical test work was primarily focused on the evaluation and optimization of the crystallization and impurity removal circuits for boric acid production. Crystallization represents a critical unit operation, directly influencing both product purity and throughput.

The impurity removal process step occurs downstream of the boric acid crystallization steps, but it is critical for the operation that impurities such as magnesium and calcium are removed. A portion of the crystallizer mother liquor is recycled back to be re-injected in the solution mining process. If the impurities are not removed, then they will build up and adversely affect the in-situ leaching process.

### 10.1 Metallurgical Testing

To support the development and design verification of the Large-Scale Borate Facility (LSBF) process, 5E initiated a comprehensive metallurgical test work program. Pregnant leach solution (PLS) from the wellfield (i.e. representative samples) was collected from the SSF and shipped to Kemetco Research Inc. (Kemetco), an independent metallurgical laboratory based in Richmond, British Columbia, Canada. Kemetco was selected based on its demonstrated expertise in crystallization technologies and other critical hydrometallurgical unit operations relevant to boric acid production. The

laboratory also brings extensive prior experience with borate systems, making it a strategic partner for validating process assumptions and optimizing key parameters. Prior to engaging Kemetco, 5E commissioned Ardent Technologies (Ardent) to perform preliminary test work. Ardent's studies, which focused on gypsum processing, impurity removal, and boric acid crystallization, which provided valuable insights and formed the basis for subsequent testing at Kemetco. The Kemetco program expanded on this foundation, incorporating process solutions and refining key parameters to inform the FEL-2 process design.

## **10.2 Representative Samples**

To ensure the test work was based on realistic process conditions, 5E shipped five drums of brine solution and five buckets of crude boric acid—both generated from the SSF—to Kemetco. These materials were used to reconstitute a representative PLS for metallurgical testing. Prior to combining the materials, Kemetco conducted a full analytical characterization of each component. The results of this analysis are presented in Section 10.4.

## **10.3 Testing Laboratory**

In March of 2025, 5E selected and engaged Kemetco, an independent and ISO-certified laboratory, to conduct the metallurgical testing program. The facility has no financial interest in 5E and was chosen for its expertise in crystallization and process development.

In addition to Kemetco's work, earlier test programs (July 2022) were conducted by Ardent. While Ardent's initial studies primarily used synthetic solutions, some of their later work incorporated actual process materials and contributed to the development of the current test program. Their findings, particularly in the areas of impurity removal and crystallization behavior, were valuable in shaping the scope and direction of the Kemetco testing.

## **10.4 Relevant Results**

### **10.4.1 Feedstock Assay Results**

5E shipped brine solution and crude boric acid, both produced at the SSF, to Kemetco's testing facility. These materials were directly generated from actual wellfield operations, making them highly representative of the expected feedstock for the LSBF. The use of authentic, wellfield-derived PLS is a critical component of the metallurgical test program, ensuring that the results are directly applicable to full-scale operations. This approach enhances confidence in the process design, performance assumptions, and downstream engineering decisions.

At Kemetco, the brine and crude boric acid were combined to reconstitute the PLS. Prior to blending, each component underwent comprehensive metallurgical analysis to characterize its composition. The results of this analysis are presented in Table 10.1.

Table 10.1: Kemetco metallurgical analysis for the five brine samples

			5E-PLS #1	PLS #2	PLS #3	PLS #4	PLS #5	Average
Ag	Silver	mg/L	<0.5	<0.5	<0.5	<0.5	<0.5	<DL
Al	Aluminum	mg/L	51	49	50	50	50	50
As	Arsenic	mg/L	<2.	<2.	<2.	<2.	<2.	<DL
B	Boron	mg/L	4,006	3,995	3,836	3,858	3,846	3,908
Ba	Barium	mg/L	1	1	1	1	1	1
Be	Beryllium	mg/L	<0.2	<0.2	<0.2	<0.2	<0.2	<DL
Bi	Bismuth	mg/L	<2.	<2.	<2.	<2.	<2.	<DL
Ca	Calcium	mg/L	21,284	20,693	21,312	21,121	21,151	21,112
Cd	Cadmium	mg/L	<0.2	<0.2	<0.2	<0.2	<0.2	<DL
Co	Cobalt	mg/L	<0.5	<0.5	<0.5	<0.5	<0.5	<DL
Cr	Chromium	mg/L	<0.5	<0.5	<0.5	<0.5	<0.5	<DL
Cu	Copper	mg/L	<1.	<1.	<1.	<1.	<1.	<DL
Fe	Iron	mg/L	183	172	174	183	178	178
K	Potassium	mg/L	185	179	187	186	183	184
Li	Lithium	mg/L	39	38	39	39	38	38
Mg	Magnesium	mg/L	1,341	1,305	1,369	1,331	1,358	1,341
Mn	Manganese	mg/L	44	42	44	44	43	43
Mo	Molybdenum	mg/L	<1.	<1.	<1.	<1.	<1.	<DL
Na	Sodium	mg/L	4,462	4,323	4,457	4,416	4,423	4,416
Ni	Nickel	mg/L	2	2	2	2	2	2
* P	Phosphorus	mg/L	<5.	<5.	<5.	<5.	<5.	<DL
Pb	Lead	mg/L	<2.	<2.	<2.	<2.	<2.	<DL
* S	Sulfur	mg/L	404	393	382	407	393	396
Sb	Antimony	mg/L	<2.	<2.	<2.	<2.	<2.	<DL
Se	Selenium	mg/L	3	3	3	<2.	3	3
Si	Silicon	mg/L	25	25	24	24	24	24
Sn	Tin		<2.	<2.	<2.	<2.	<2.	<DL
Sr	Strontium	mg/L	225	219	224	224	223	223
Ti	Titanium	mg/L	<1.	<1.	<1.	<1.	<1.	<DL
Tl	Thallium	mg/L	<2.	<2.	<2.	<2.	<2.	<DL
U	Uranium	mg/L	<5.	<5.	<5.	<5.	<5.	<DL
V	Vanadium	mg/L	<1.	<1.	<1.	<1.	<1.	<DL
Zn	Zinc	mg/L	3	3	3	3	3	3
Density (g/mL)		g/mL	1.08	1.09	1.09	1.09	1.08	1.08
Cl (colorimetric)		mg/L	48,377	48,472	49,576	51,116	49,233	49,355
F by ISE (ppm)		mg/L	101	96	99	101	97	99
pH			4.85	4.88	4.83	4.90	4.89	
H <sub>3</sub> BO <sub>3</sub>		g/kg	21	21	20	20	20	21

\* Not certified



Table 10.2: Kemetco metallurgical analysis for the five boric acid samples

			Boric Acid #1	Boric Acid #2	Boric Acid #3	Boric Acid #4	Boric Acid #5	Average
Ag	Silver	mg/kg	<5.	<5.	<5.	<5.	<5.	<DL
Al	Aluminum	mg/kg	<10.	<10.	<10.	<10.	<10.	<DL
As	Arsenic	mg/kg	<20.	<20.	<20.	<20.	<20.	<DL
B	Boron	mg/kg	158,991	163,909	155,827	160,997	157,943	159,533
Ba	Barium	mg/kg	<2.	<2.	<2.	<2.	<2.	<DL
Be	Beryllium	mg/kg	<2.	<2.	<2.	<2.	<2.	<DL
Bi	Bismuth	mg/kg	<20.	<20.	<20.	<20.	<20.	<DL
Ca	Calcium	mg/kg	19,181	16,696	18,409	18,283	18,282	18,170
Cd	Cadmium	mg/kg	<2.	<2.	<2.	<2.	<2.	<DL
Co	Cobalt	mg/kg	<5.	<5.	<5.	<5.	<5.	<DL
Cr	Chromium	mg/kg	<5.	<5.	<5.	<5.	<5.	<DL
Cu	Copper	mg/kg	<10.	<10.	<10.	<10.	<10.	<DL
Fe	Iron	mg/kg	18.3	14.1	14.6	14.1	14.5	15
K	Potassium	mg/kg	<50.	<50.	<50.	<50.	<50.	<DL
Li	Lithium	mg/kg	<10.	<10.	<10.	<10.	<10.	<DL
Mg	Magnesium	mg/kg	<10.	<10.	<10.	<10.	<10.	<DL
Mn	Manganese	mg/kg	<2.	<2.	<2.	5.6	<2.	6
Mo	Molybdenum	mg/kg	<10.	<10.	<10.	<10.	<10.	<DL
Na	Sodium	mg/kg	<50.	<50.	<50.	<50.	<50.	<DL
Ni	Nickel	mg/kg	<5.	<5.	<5.	<5.	<5.	<DL
* P	Phosphorus	mg/kg	<50.	<50.	<50.	<50.	<50.	<DL
Pb	Lead	mg/kg	<20.	<20.	<20.	<20.	<20.	<DL
* S	Sulfur	mg/kg	15,260	13,021	15,540	14,630	14,707	14,632
Sb	Antimony	mg/kg	<20.	<20.	<20.	<20.	<20.	<DL
Se	Selenium	mg/kg	<20.	<20.	<20.	<20.	<20.	<DL
Si	Silicon	mg/kg	87.2	80.6	87.2	84.1	86.7	85
Sn	Tin	mg/kg	<20.	<20.	<20.	<20.	<20.	<DL
Sr	Strontium	mg/kg	35.9	30.7	36.5	33.9	35.4	34
Ti	Titanium	mg/kg	<10.	<10.	<10.	<10.	<10.	<DL
Tl	Thallium	mg/kg	<20.	<20.	<20.	<20.	<20.	<DL
U	Uranium	mg/kg	<50.	<50.	<50.	<50.	<50.	<DL
V	Vanadium	mg/kg	<10.	<10.	<10.	<10.	<10.	<DL
Zn	Zinc	mg/kg	<5.	<5.	<5.	<5.	<5.	<DL
H <sub>3</sub> BO <sub>3</sub>		g/kg	909	937	891	921	903	912

#### 10.4.2 PLS Characterization

The PLS composition that is fed to the crystallizers was simulated using METSIM® modelling software and is shown below. Kemetco amended the reconstituted PLS with small amounts of magnesium chloride, calcium chloride, and sodium chloride to approach the simulated feed conditions. This was done to simulate the various recycle streams within the plant.

The target boric acid head grade expected from the mining operation is 10.2 wt.%. Actual testing by Kemetco was performed at a target of 10.4 wt.%. The slight variation in boric acid head grade is a result of some adjustments to the overall process simulation that were performed after the test work program had begun. Table 10.3 provides the simulated crystallizer feed conditions from the METSIM model.

Table 10.3: Simulated crystallizer feed conditions

Component	wt. %
H <sub>2</sub> O	76.6%
H <sub>3</sub> BO <sub>3</sub>	10.4%
CaCl <sub>2</sub>	5.3%
NaCl	3.8%
MgCl <sub>2</sub>	2.4%
KCl	1.0%
LiCl	0.5%
CaSO <sub>4</sub>	0.1%
pH	4.0

The amended PLS feed compositions for the crystallization tests are shown in Table 10.4 and Table 10.5 provides the feed solutions compositions for continuous crystallization tests (CRZ1-4 and CRZ1-5).

Table 10.4: Amended PLS feed compositions for batch crystallization tests (CRZ1-1 through CRZ1-3)

	Unit	CRZ1-1	CRZ1-2	CRZ1-3
<b>Ag Silver</b>	mg/kg	<1.	<2.5	<1.
<b>Al Aluminum</b>	mg/kg	63	65	58
<b>As Arsenic</b>	mg/kg	<4.0	<10.0	<4.0
<b>B Boron</b>	mg/kg	15,941	21,030	18,491
<b>Ba Barium</b>	mg/kg	1	1	1
<b>Be Beryllium</b>	mg/kg	<0.4	<1.0	<0.4
<b>Bi Bismuth</b>	mg/kg	<4.0	<10.0	<4.0
<b>Ca Calcium</b>	mg/kg	17,380	16,830	17,095
<b>Cd Cadmium</b>	mg/kg	<0.4	<1.0	<0.4
<b>Co Cobalt</b>	mg/kg	<1.0	<2.5	<1.0
<b>Cr Chromium</b>	mg/kg	<1.0	<2.5	2
<b>Cu Copper</b>	mg/kg	<2.0	<5.0	<2.0
<b>Fe Iron</b>	mg/kg	146	153	142
<b>K Potassium</b>	mg/kg	244	250	249
<b>Li Lithium</b>	mg/kg	69	70	68
<b>Mg Magnesium</b>	mg/kg	6,067	6,069	5,762
<b>Mn Manganese</b>	mg/kg	33	38	31
<b>Mo Molybdenum</b>	mg/kg	<2.	<5.0	<2.0
<b>Na Sodium</b>	mg/kg	14,504	14,467	15,575
<b>Ni Nickel</b>	mg/kg	<1.0	<2.5	3
<b>* P Phosphorus</b>	mg/kg	<10.0	<25.0	<10.
<b>Pb Lead</b>	mg/kg	<4.0	<10.0	<4.0
<b>* S Sulfur</b>	mg/kg	249	243	313
<b>Sb Antimony</b>	mg/kg	<4.0	<10.0	<4.0
<b>Se Selenium</b>	mg/kg	<4.0	<10.0	<4.0
<b>Si Silicon</b>	mg/kg	27	27	27
<b>Sn Tin</b>	mg/kg	<4.0	<10.0	<4.0
<b>Sr Strontium</b>	mg/kg	166	163	161
<b>Ti Titanium</b>	mg/kg	<2.0	<5.0	<2.0
<b>Tl Thallium</b>	mg/kg	<4.0	<10.0	<4.0
<b>U Uranium</b>	mg/kg	<10.0	<25.0	<10.0
<b>V Vanadium</b>	mg/kg	<2.0	<5.0	<2.0
<b>Zn Zinc</b>	mg/kg	3	<2.5	3

Table 10.5: Feed solutions for continuous crystallization

	Unit	CRZ1-4	CRZ1-5
Ag Silver	mg/kg	<1.0	<1.0
Al Aluminum	mg/kg	40	12
As Arsenic	mg/kg	<4.0	<4.0
B Boron	mg/kg	19,967	16,484
Ba Barium	mg/kg	1	1
Be Beryllium	mg/kg	<0.4	<0.4
Bi Bismuth	mg/kg	<4.0	<4.0
Ca Calcium	mg/kg	17,460	16,609
Cd Cadmium	mg/kg	<0.4	<0.4
Co Cobalt	mg/kg	<1.0	<1.0
Cr Chromium	mg/kg	2	<1.0
Cu Copper	mg/kg	<2.0	<2.0
Fe Iron	mg/kg	125	<2.0
K Potassium	mg/kg	248	244
Li Lithium	mg/kg	67	65
Mg Magnesium	mg/kg	5,915	5,350
Mn Manganese	mg/kg	33	31
Mo Molybdenum	mg/kg	<2.0	<2.0
Na Sodium	mg/kg	15,983	14,480
Ni Nickel	mg/kg	2	2
* P Phosphorus	mg/kg	<10.0	<10.0
Pb Lead	mg/kg	<4.0	<4.0
* S Sulfur	mg/kg	319	324
Sb Antimony	mg/kg	<4.0	<4.0
Se Selenium	mg/kg	<4.0	<4.0
Si Silicon	mg/kg	22	50
Sn Tin	mg/kg	<4.0	<4.0
Sr Strontium	mg/kg	167	34
Ti Titanium	mg/kg	<2.0	<2.0
Tl Thallium	mg/kg	<4.0	<4.0
U Uranium	mg/kg	<10.0	<10.0
V Vanadium	mg/kg	<2.0	<2.0
Zn Zinc	mg/kg	3	4
Cl	mg/kg	76,599	66,522

### 10.4.3 Crystallization Results

Five boric acid crystallization tests and a re-crystallization test were performed. These tests were performed using 1-stage crystallization, 2-stage crystallization, flash crystallization, and re-crystallization processes. In each test, representative samples were collected and analyzed. The crystal samples were analyzed using Inductively Coupled Plasma (ICP) techniques. Crystallization tests CRZ1-1 to CRZ1-3 were performed in batch mode and CRZ1-4 and CRZ1-5 were performed in a continuous process.

Boric acid solubility curves were generated by measuring boric acid concentrations at various temperatures ranging from 10°C to 80°C (50°F to 176°F). This is a critical step in designing full-scale crystallizers, as it defines the temperature range required for crystal growth and enables calculation of the amount of boric acid that can be crystallized from solution—directly impacting plant throughput. The solubility curve data collected, confirmed previously postulated data used in the process simulation. This information is essential for accurately sizing crystallizers and associated process equipment by informing the mass and energy balance requirements needed to meet design capacity. A well-characterized solubility curve also supports optimized process control, helping to prevent fouling and poor crystal quality, and is used to validate the overall process simulation model.

Figure 10.1: Boric acid solubility curve at various temperatures for CRZ1-1, CRZ1-2, and CRZ1-3

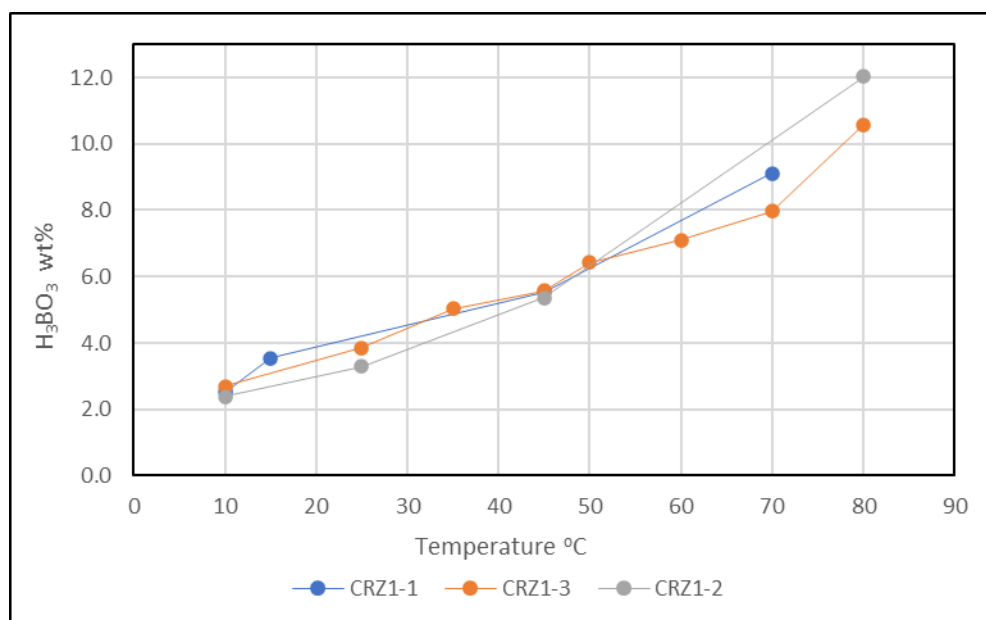


Figure 10.2: Boric acid continuous crystallization set-up including an agitated feed tank



*Figure 10.3: Boric acid crystals after continuous crystallization test (CRZ1-4)*

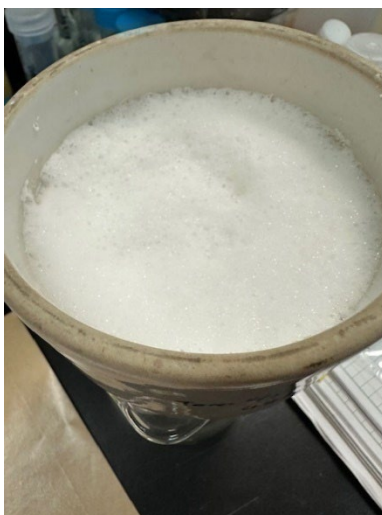


*Figure 10.4: Boric acid crystals after continuous crystallization test (CRZ1-4) and centrifugation*



The boric acid crystals in the continuous crystallization test, CRZ1-4, had a distinct brown-orange layer that is indicative of ferric iron precipitation. The boric acid crystals pictured are not the finished product. They are the result of the crude crystallization step. The full process includes a filtration step for the crude crystallizer slurry. The resulting filter cake is washed and redissolved. This solution is filtered again before being fed to the re-crystallization process as shown in Figure 10.5 and Figure 10.6 below.

*Figure 10.5: Boric acid crystals after re-crystallization*



*Figure 10.6: Boric acid crystals after re-crystallization and dewatering process*



The re-crystallization testing yielded a bright-white boric acid crystal product. This is a visual indicator of higher product purity and was confirmed in the lab testing through ICP and chloride analysis as shown below. The boric acid recrystallization test confirmed that the product can achieve the customer specifications listed in Section 16 through water dissolution and displacement washing. This method successfully met or exceeded target chemical specifications, particularly for iron and chloride, and is the design basis for the Large-scale Boron Facility.



Table 10.6: Boric acid re-crystallization results

		Solutions			Crystals - wet solids			Crystals - dry solids		
	Unit	Feed	Mother Liquor	Wet Discharge	Batch 1- Crystals- wet	Batch 2- Crystals -wet	Batch 3- Washed Crystals wet	Batch 1- Crystals -dry	Batch 2- Crystals -dry	Batch 3- Washed Crystals - dry
<b>BA assay</b>	wt%	-	-	-	-	-	-	<b>98.89</b>	<b>98.85</b>	<b>98.61</b>
<b>Calc H<sub>3</sub>BO<sub>3</sub></b>	wt%	12.50	5.14	4.50	<b>102.71</b>	<b>95.62</b>	<b>95.94</b>	<b>101.68</b>	<b>108.03</b>	<b>109.08</b>
<b>Ag</b>	mg/kg	<1.0	<1.0	<1.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
<b>Al</b>	mg/kg	<2.0	<2.0	<2.0	<10.0	<10.0	<10.0	<10.0	<10.0	<10.0
<b>As</b>	mg/kg	<4.0	<4.0	<4.0	<20.0	<20.0	<20.0	<20.0	<20.0	<20.0
<b>B</b>	mg/kg	21,862	8,983	7,869	170,117	146,588	152,546	177,782	175,656	177,375
<b>Ba</b>	mg/kg	<0.4	<0.4	<0.4	<2.0	<2.0	<2.0	<2.0	<2.0	<2.0
<b>Be</b>	mg/kg	<0.4	<0.4	<0.4	<2.0	<2.0	<2.0	<2.0	<2.0	<2.0
<b>Bi</b>	mg/kg	<4.0	<4.0	<4.0	<20.0	<20.0	<20.0	<20.0	<20.0	<20.0
<b>Ca</b>	mg/kg	187	200	33.0	17.8	38.3	<10.0	18	35	<10.0
<b>Cd</b>	mg/kg	<0.4	<0.4	<0.4	<2.0	<2.0	<2.0	<2.0	<2.0	<2.0
<b>Co</b>	mg/kg	<1.0	<1.0	<1.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
<b>Cr</b>	mg/kg	<1.0	<1.0	<1.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
<b>Cu</b>	mg/kg	<2.0	<2.0	<2.0	<10.0	<10.0	<10.0	<10.0	<10.0	<10.0
<b>Fe</b>	mg/kg	2.6	2.9	<2.0	<10.0	<10.0	<10.0	<10.0	<10.0	<10.0
<b>K</b>	mg/kg	<10.0	<10.0	<10.0	<50.0	<50.0	<50.0	<50.0	<50.0	<50.0
<b>Li</b>	mg/kg	<2.0	<2.0	<2.0	<10.0	<10.0	<10.0	<10.0	<10.0	<10.0
<b>Mg</b>	mg/kg	58.6	63.7	9.9	<10.0	10.2	<10.0	<10.0	11	<10.0
<b>Mn</b>	mg/kg	2.2	2.5	0.9	<2.0	<2.0	<2.0	<2.0	<2.0	<2.0
<b>Mo</b>	mg/kg	<2.0	<2.0	<2.0	<10.0	<10.0	<10.0	<10.0	<10.0	<10.0
<b>Na</b>	mg/kg	154	162	25.3	<50.0	<50.0	<50.0	<50.0	<50.0	<50.0
<b>Ni</b>	mg/kg	<1.0	<1.0	<1.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
<b>* P</b>	mg/kg	<10.0	<10.0	<10.0	<50.0	<50.0	<50.0	<50.0	<50.0	<50.0
<b>Pb</b>	mg/kg	<4.0	<4.0	<4.0	<20.0	<20.0	<20.0	<20.0	<20.0	<20.0
<b>* S</b>	mg/kg	20.7	21.2	6.0	<20.0	<20.0	<20.0	<20.0	<20.0	<20.0
<b>Sb</b>	mg/kg	<4.0	<4.0	<4.0	<20.0	<20.0	<20.0	<20.0	<20.0	<20.0
<b>Se</b>	mg/kg	<4.0	<4.0	<4.0	<20.0	<20.0	<20.0	<20.0	<20.0	<20.0
<b>Si</b>	mg/kg	<4.0	<4.0	<4.0	<20.0	<20.0	<20.0	<20.0	<20.0	<20.0
<b>Sn</b>	mg/kg	<4.0	<4.0	<4.0	<20.0	<20.0	<20.0	<20.0	<20.0	<20.0
<b>Sr</b>	mg/kg	1.9	2.0	<0.4	<2.0	<2.0	<2.0	<2.0	<2.0	<2.0
<b>Ti</b>	mg/kg	<2.0	<2.0	<2.0	<10.0	<10.0	<10.0	<10.0	<10.0	<10.0
<b>Tl</b>	mg/kg	<4.0	<4.0	<4.0	<20.0	<20.0	<20.0	<20.0	<20.0	<20.0
<b>U</b>	mg/kg	<10.0	<10.0	<10.0	<50.0	<50.0	<50.0	<50.0	<50.0	<50.0
<b>V</b>	mg/kg	<2.0	<2.0	<2.0	<10.0	<10.0	<10.0	<10.0	<10.0	<10.0
<b>Zn</b>	mg/kg	<1.0	<1.0	<1.0	<5.0	<5.0	<5.0	<5.0	<5.0	<5.0
<b>Cl</b>	mg/kg	687	775	123	40.1	105	10.0	28.8	104	12.6

Table 10.7: Particle size distribution for batch crystallization test CRZ1-1 through CRZ1-3

	Unit	CRZ1-1	CRZ1-2	CRZ1-3
D10	µm	101	73	58
D50	µm	283	215	189
D90	µm	492	419	404

Table 10.8: Particle size distribution for continuous crystallization test CRZ1-4

Batch #	D10	D50	D90
Unit	um	um	um
1	79.0	318.0	646.7
3	82.5	250.2	696.5
5	75.9	238.9	663.4
7	79.6	233.7	653.2
9	80.1	225.4	586.3
10	96.6	366.9	793.6

Table 10.9: Particle size distribution for continuous crystallization test CRZ1-5

Batch #	D10	D50	D90
Unit	um	um	um
1	78.0	289.5	573.8
3	43.6	233.8	651.1
5	54.8	175.2	648.1
7	61.9	177.6	635.8
9	47.9	175.9	591.1
10	73.5	184.9	526.9

Table 10.10: Boric acid crystal particle size distribution for re-crystallization

D10	D50	D90
µm	µm	µm
147.9	269.7	449.3

The particle size distribution for the re-crystallization test yielded boric acid crystals that are coarser than the final product specification.

Table 10.11: Boric acid crystal particle size specification

PARAMETER	UNIT	DESIGN VALUE
<b>Dry Sieve Analysis</b>	-	-
8 mesh (2360 micron)	%, Max	0.0
20 mesh (850 micron)	%, Max	2.0
30 mesh (600 micron)	%, Max	5.0
100 mesh (150 micron)	%, Min	60.0
200 mesh (75 micron)	%	Report

Crystal growth dynamics are influenced by several interdependent process parameters, including residence time, slurry density, degree of supersaturation, cooling method and rate, agitation intensity, and mixing efficiency. These variables can be strategically manipulated to control nucleation and growth rates, thereby influencing the final crystal size distribution—favoring either larger crystals or a greater yield of smaller crystals, depending on process objectives. While crystal growth optimization was not a primary focus of the current test work campaign, the data generated—including operating conditions and corresponding residence times—provides a valuable baseline. These results will inform future optimization efforts during final process design.

#### 10.4.4 Impurity Removal Test Results

Impurity removal testing was conducted on crystallizer mother liquor to evaluate two process flow options for removing magnesium while minimizing boron losses. The goal was to selectively precipitate impurities without compromising boron recovery. Two different flow sheet options were evaluated as part of the test work.

**Option 1:** Crystallizer mother liquor → Evaporation (50% mass) → Cooling Crystallization → Sequential pH Adjustments with Lime Slurry

- The mother liquor was first evaporated to 50% of its original mass, followed by cooling crystallization and two sequential pH adjustments using lime slurry.
- At a mid-range acidic pH, approximately 45% of boron and 2% of the magnesium were removed.
- A second pH adjustment to a higher and more basic pH removed an additional 38% of boron and 84% of the magnesium.
- The final solid phase contained 53% of the initial boron, primarily as a calcium–boron complex with measurable magnesium content (11% B, 15.2% Ca, 8.2% Mg).

**Option 2:** CRZ1 mother liquor → Sequential pH adjustments → Evaporation (EVP1) (60% mass reduction)

- The mother liquor underwent sequential pH adjustments to a mid-ranged acidic pH and then to a higher and more basic pH. This was followed by evaporation to 60% of its original mass.
- At the first pH adjustment (mid-ranged acidic), only 8% of boron was removed, with no measurable magnesium removal.
- At the second (basic) pH adjustment, 60% of boron and 12% of magnesium were removed.

Note that the actual pH values were determined through experimentation.

The difference in magnesium removal at a basic pH (Option 1) was 84% compared to a basic pH (Option 2) was 12% removal. Magnesium removal is strongly pH dependent. Boron precipitates out at lower pH and the resulting boron calcium complex can be recycled to increase overall boron recovery. Removing magnesium is important because it is a waste product, and the remaining filtrate is rich in calcium chloride which is to be further concentrated and sold as a byproduct. Both options that were tested were successful. The major difference between the two options was that the size of evaporation ponds was smaller in Option 2. Option 2 is included in the basis of design.

These data points are helpful for understanding the sensitivities of the selective precipitations in order to further recover valuable boron while removing impurities.

## 10.5 Adequacy of Data

The QP for Fluor, Kevin R. Martina, has conducted a thorough review of the metallurgical test methods and results of the metallurgical test involving the PLS sample collected from the SSF. He confirms that the reporting is consistent with industry standard practice and that the appropriate protocols were followed during sample preparation. Mr. Martina further verifies that the processing and testing of the PLS sample were conducted in accordance with the accepted methodologies. Based on this evaluation, he QP concludes that the extent of testing performed is suitable for the current engineering study level and provides relevant data to support ongoing process design development.

# 11 Mineral Resource Estimates

In March 2025, Mr. Steven Kerr of Escalante Geological Services, LLC completed an updated resource estimate for the Project. Since the previous resource estimate in 2021, 5E completed three more bore holes and acquired additional mineral tenure for the Project. The 2021 resource estimate identified a total resource of 171.3 million short tons of  $B_2O_3$  with 30.95 million short tons classified as measured resource and 43.35 million short tons classified as indicated resource using a cut-off grade of 2.0%  $B_2O_3$ .

## 11.1 Key Assumptions

Key assumptions used in the economic assessment include:

- Mineralized horizons exhibit lateral continuity that will support mining using in-situ leaching mining methods;
- Mineralized horizons are not disrupted by structural or stratigraphic features that could limit mining;
- There is reasonable continuity of colemanite mineralization throughout the deposit; and
- There is adequate exploration data to support estimation of resources

A detailed financial model using a discount rate of 7% delivered a positive net present value to support the cut-off grade and more broadly the resulting mineral resource estimation.

## 11.2 QP's Estimate of Resource

### 11.2.1 Resource Database

The database used for resource estimation includes 52 core holes and three rotary holes for a total of 55 bore holes. Thirty of the core holes were completed by Duval between 1979 and 1981. 5E completed 14 core holes in 2017 and another hole in 2022. In 2024, 5E completed three rotary holes as observation wells from which chip samples were collected through the mineral horizons for  $B_2O_3$  and Li analyses. The cumulative sampled length for the database is 5,440.19 m (17,848.39 ft). Table 11.1 summarizes the drilling database. The Project's exploration dataset is current as of February 12, 2025. Drilling coordinates in the database are in UTM NAD 83-11, and depths and elevations are reported in meters. Borate is listed as weight percent (%)  $B_2O_3$  and Li as ppm. The drilling database contains 5,767 analytical values for  $B_2O_3$  and 5,402 analytical values for Li.

Core recovery for the 5E drilling programs has ranged from 93% to 100% with an overall average of 97.60%. Core recovery records for earlier drilling conducted by Duval are not available, but based on missing intervals in the drilling database, core recovery likely exceeded 90% in the core drilling. The QP has completed a thorough review and verification of the drilling database and found the database to be sufficient for resource modeling.

Table 11.1: Summary of drilling database

Core Hole ID	Cumulative Core Length (m)	Cumulative Sample Length (m)	B <sub>2</sub> O <sub>3</sub> Analyses	Li Analyses
APBL-01	111.13	88.90	82	82
APBL-02	91.74	87.74	107	107
APBL-03	93.11	92.80	91	91
APBL-04	143.77	142.71	162	162
APBL-05	107.35	104.76	150	150
APBL-06	95.34	90.47	83	83
APBL-07	176.27	166.09	207	207
APBL-08	128.96	127.20	153	153
APBL-09	119.33	118.51	120	120
APBL-10	133.81	126.50	176	176
APBL-11	135.72	134.79	155	155
APBL-12	142.77	138.42	212	212
APBL-13	138.99	136.75	155	155
APBL-14	157.43	156.99	260	260
DHB-01	162.49	158.41	184	184
DHB-03	212.90	212.12	213	213
DHB-05	207.26	207.26	179	179
DHB-06	175.57	155.42	124	124
DHB-07	204.83	204.06	179	179
DHB-08	224.63	224.63	186	186
DHB-09	170.69	170.69	138	138
DHB-10	139.08	81.79	86	86
DHB-11	112.90	73.28	86	86
DHB-12	120.67	74.04	85	-
DHB-13	102.57	61.17	70	70
DHB-14	117.63	75.71	80	-
DHB-15	125.70	56.18	51	51
DHB-16	145.48	122.62	138	138
DHB-17	141.25	104.49	151	151
DHB-18	139.48	92.32	105	105
DHB-19	106.68	59.40	74	74
DHB-21	26.33	25.93	39	39
DHB-22	135.94	101.81	135	135
DHB-23	136.24	100.80	114	114
DHB-24	146.00	120.00	119	119
DHB-25	173.74	134.87	152	152
DHB-26	121.37	81.99	106	106
DHB-27	132.71	67.07	95	95
DHB-28	128.62	80.07	115	115
DHB-29	120.64	75.28	101	101
DHB-30	137.53	68.49	83	83
DHB-31	49.00	57.36	41	-
DHB-33	111.19	92.17	80	-
DHB-34	68.76	87.47	79	-
IR-2-01-01	137.59	119.57	135	135
SMT-1	24.40	24.40	57	59
SMT-2	24.60	24.60	55	-

<b>SMT-3</b>	33.10	33.10	69	-
<b>P1</b>	61.10	61.10	20	-
<b>P2</b>	64.20	64.20	21	-
<b>P3</b>	55.10	55.10	18	-
<b>P4</b>	54.20	54.20	34	-
<b>Total</b>	<b>6,327.89</b>	<b>5,375.80</b>	<b>5,910</b>	<b>5,330</b>

<b>Rotary Hole ID</b>	<b>Hole Depth</b>	<b>Cumulative Sample Length (m)</b>	<b>B<sub>2</sub>O<sub>3</sub> Analyses</b>	<b>Li Analyses</b>
<b>OW-09</b>	480.06	126.50	46	46
<b>OW-10</b>	466.00	132.88	44	44
<b>OW-11</b>	460.00	121.71	41	41
<b>Total</b>		<b>381.09</b>	<b>131</b>	<b>131</b>

### 11.2.2 Geologic Model

The QP developed a gridded geologic model of the Project using Carlson Mining™ software. The mineralization does not correlate to lithological markers as the entire sequence is predominantly lacustrine mudstone. However, detailed examination of the analytical results reveals distinct mineralized horizons. The deposit was delineated based on these patterns of mineralization into four mineralized horizons, two non-mineralized or weakly mineralized interbeds and two non-mineralized horizons bounding the deposit. These horizons are listed in Table 11.2.

The grid model was constructed across the deposit area, with a grid cell size of 50 m x 50 m. Grids represent the bounding elevation surfaces of key horizons, horizon thicknesses, and analytical grades. Grids representing the bounding surface elevations of the mineral horizon were interpolated through triangulation. Mineral horizon grids for thickness and analytical grades were interpolated using Ordinary Kriging (OK) and Inverse Distance Squared (ID2) algorithms. Mineralization is spatially defined by a resource boundary using a distance of 200 m from the last intersection of mineralization in a drill hole and by property boundaries. Grids are masked to the outside of the resource boundary.

Table 11.2: Modelled horizons

<b>Horizon</b>	<b>Abbreviation</b>	<b>Thickness Range (m)</b>	<b>Average Thickness (m)</b>	<b>Composite B<sub>2</sub>O<sub>3</sub> Range (wt.%)</b>	<b>Composited Li Range (ppm)</b>
<b>Overburden</b>	OBN	317.0 - 507.7	381.8	NA	NA
<b>Upper Mineralized Horizon</b>	UMH	0.1 - 12.5	4.3	0.87 - 14.45	99 - 588
<b>Upper Interbed</b>	UI	0.1 - 16.7	6.7	0.5 - 4.1	108 - 623
<b>Main Mineralized Horizon</b>	MMH	0.7 - 69.4	27.4	2.6 - 17.6	98 - 550
<b>Medial Interbed</b>	MI	0.2 - 5.2	9.7	0.3 - 1.9	386 - 492
<b>Intermediate Mineralized Horizon</b>	IMH	1.8 - 58.3	22.5	0.7 - 12.0	23 - 534
<b>Lower Mineralized Horizon</b>	LMH	0.0 - 53.9	19.7	0.2 - 5.7	91 - 534
<b>Lower Sandstone*</b>	LSS	0.1 - 58.6	15.6	NA	NA

\* Horizon not fully penetrated, NA: Not Applicable

### 11.2.3 Grade Estimation & Resource Classification

Using composites for each mineralized horizon, variography was successful for B<sub>2</sub>O<sub>3</sub> grades for the Major Mineralized Horizon (MMH), Intermediate Mineralized Horizon (IMH), and the Lower Mineralized Horizon (LMH) and are summarized in Table 3. Variogram modelling was unsuccessful for the Upper Mineralized Horizon and with Li in all horizons. Grids representing B<sub>2</sub>O<sub>3</sub> grades for the MMH, IMH, and LMH were constructed using OK based on the constructed variograms. ID2 interpolation was used with all remaining grade grids using the same spatial limits established with the horizon grids.



Table 11.3: Modelled variograms

Horizon	Type	Nugget	First Structure	Second Structure
MMH	Spherical, omnidirectional	—	200.0	400
IMH	Spherical, omnidirectional	0.2	180.0	450
LMH	Spherical, omnidirectional	0.2	530.0	—

Based on the variography above, the deposit was classified as follows:

- Measured Resource Category: based on a maximum spacing between mineralized drill holes for each horizon of 200 m.
- Indicated Resources Category: based on a maximum spacing between mineralized drill holes for each horizon of 400 m.
- Inferred Resources Category: based on a maximum spacing between mineralized drill holes for each horizon of 800 m.

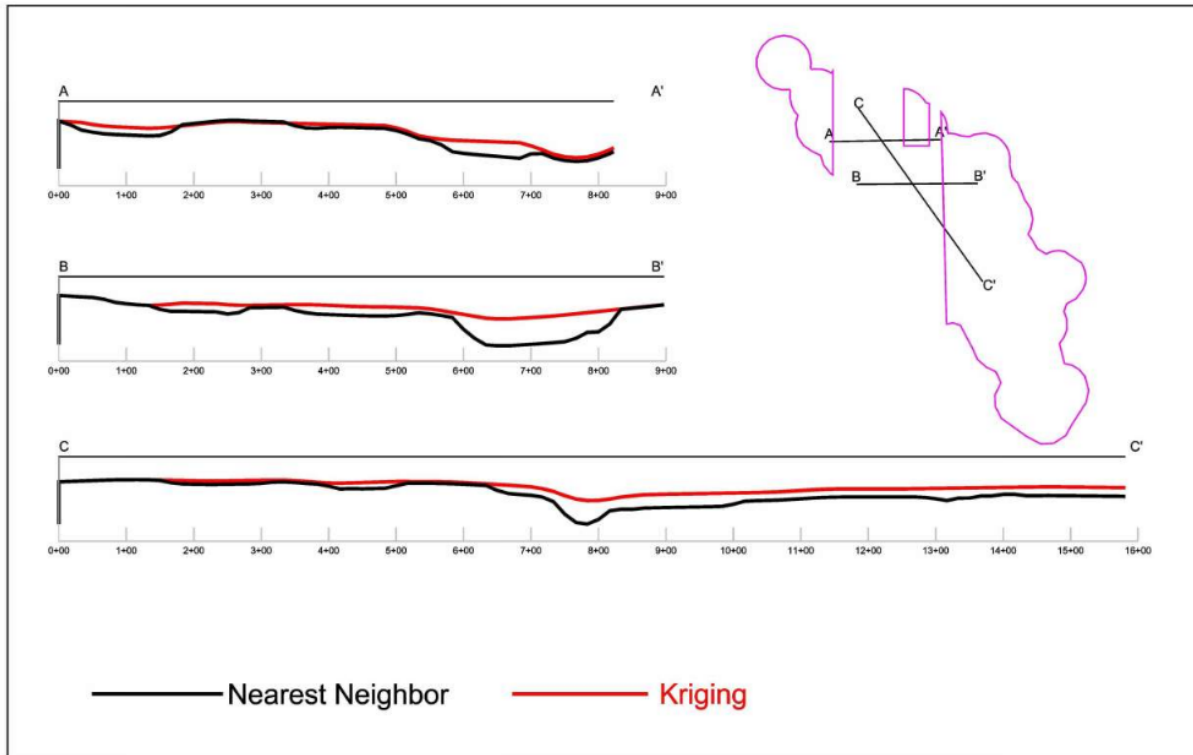
Drilling and sampling density is sufficient that no further limits on classification are required.

### 11.3 Model Validation

The QP has conducted an audit of the gridded model. The audit and validation of the gridded model consisted of the following steps:

1. Drilling data was loaded into Carlson Mining to compare drill hole postings with the provided grids representing the top and bottom surfaces for each mineralized horizon. This comparison was done using a grid inspector tool in Carlson Mining that enables simultaneous viewing of drill hole data along with grid values at each drilling location. The QP found the resulting comparisons to be satisfactory. This step was repeated comparing drill hole composite grades from drill hole data with grids representing the grades of B<sub>2</sub>O<sub>3</sub> and Li for each mineralized horizon. While there are some fluctuations with grid values generated by OK and ID2, these fluctuations are small and within expected ranges.
2. The gridded model was evaluated using a series of swath plots. A swath plot is a graphical display of the grade distribution derived from a series of bands, or swaths, generated as sections through the deposit. Grade variations from the OK model are compared to nearest neighbor (NN) searches on drill hole composites.
3. On a local scale, the NN search does not provide reliable estimations of grade but, on a much larger scale, it represents an unbiased estimation of the grade distribution based on the underlying data. If the model estimation completed by OK is unbiased, the grade trends may show local fluctuations on a swath plot, but the overall trend should be similar to the NN distribution of grade. Three swath plots are shown in Figure 11.1.

Figure 11.1: Grade variation swath



### 11.3.1 Density Measurements

The 2017 drilling program included the collection of 777 density measurements from core samples. Density determinations were made using the weight in air/weight in water method. The weighted average bulk density determined from the 381 samples collected through the mineralized horizons is 2.18 g/cm<sup>3</sup>, and has been used as the bulk density in resource estimation.

### 11.4 Cut-off Grade

A 5.0% B<sub>2</sub>O<sub>3</sub> cut-off grade was previously established by Duval and was carried forth by previous QP's in previous technical report summaries. An in-depth assessment of cut-off grade was undertaken in 2022 and 2023 as mass and energy balances were developed to fundamentally begin to assess economic viability. Data informing the mass and energy balances included incorporating the results of leaching tests, historical results, mining, and processing costs, as well as commodity pricing. This assessment derived a 2.0% cut-off calculation based on the most recent previous initial assessment.

Cut-off grade is an economic analysis to measure cash costs (i.e., the variable cost to produce boric acid compared to the price that can be achieved in the market for the sale of boric acid). SE commenced mining operations in January 2024 and began operating the SSF in April 2024. The SSF achieved a steady state of operation in the Summer of 2024 and optimized mining operations by September 2024. As such, mining data from September and October 2024 have been utilized as the basis of design and further leveraged for the cut-off grade analysis. Using this data set, an in-depth assessment was performed that included an analysis of the cash costs (i.e., the variable cost to produce boric acid) and excluded book costs (i.e., depreciation) as the capital is assumed to have already been invested to build the project such that it can operate. The definition of cut-off grade for the in-situ mining operation is the point at which the Company would cease operating a particular well or in the case of a combination of wells, the wellfield. As such, cash costs are established as the basis for the analysis.

The in-depth analysis incorporates mineralization and at what point economic extraction or boron in solution is no longer viable. The driver of this analysis focuses on three specific ratios derived from the basis of design using mining

data during the period of September and October 2024: calcium to boron, sodium to boron, and magnesium to boron. These three ratios are drivers of various costs, chemical utilizations, and byproduct production rates. For example, calcium to boron impacts sulfuric acid utilization and gypsum production compared to boric acid production. Additionally, magnesium to boron impacts lime utilization and metal salt waste production compared to boric acid production. Lastly, sodium to boron impacts HCl utilization and sodium chloride production compared to boric acid production. Table 11.4 below details the average, minimum and maximum ratios of elements utilized in the basis of design from September and October 2024:

*Table 11.4: Basis of design ratios*

	<b>Ca:B</b>	<b>Mg:B</b>	<b>Na:B</b>
Average	1.27	0.13	0.34
Minimum	0.77	0.03	0.02
Maximum	2.05	0.22	0.70

To calculate cut-off grade, the following assumptions were utilized which are in-line with the basis of design noted in Section 14:

- Overall boric acid yield of 95.1% and HCl utilization of 90%;
- Magnesium accounts for 50% of the metal impurities and all impurities are extracted at similar rates;
- Sodium chloride is 80% of the chloride losses;
- The LSBF is designed for 130,000 short tons per year with a maximum 50% recycling and 10% excess flow capacity in the plant and max solubility of 10% boric acid; and
- Orebody calcite is held constant at 7.03% (Note: This assumption is derived from XRD results (7.03% calcite) of core and historical pilot plant results from the 1980's (3.80%, 6.08%, and 6.08% calcite).

Table 11.5 provides the cost inputs used in the sensitivity analysis for cut-off grade:

*Table 11.5: Cut-off grade input costs*

<b>Raw Material</b>	<b>Unit</b>	<b>Price</b>
36% HCl	per short ton BA	\$158.61
H <sub>2</sub> SO <sub>4</sub>	per short ton BA	\$124.13
Lime	per short ton BA	\$197.47
Metal impurities waste	per short ton BA	\$45.00
Natural gas	per MMBTU	\$3.19

Finally, a sensitivity analysis was performed where cash costs were calculated at each discreet cutoff grade to determine where the cost curves relative to the price of boric acid intersect. For this analysis, the magnesium to boron ratio and the sodium to boron ratio were held constant using the averages obtained from actual mining data and noted in Table 11.4 above. Table 11.6 provides this analysis:

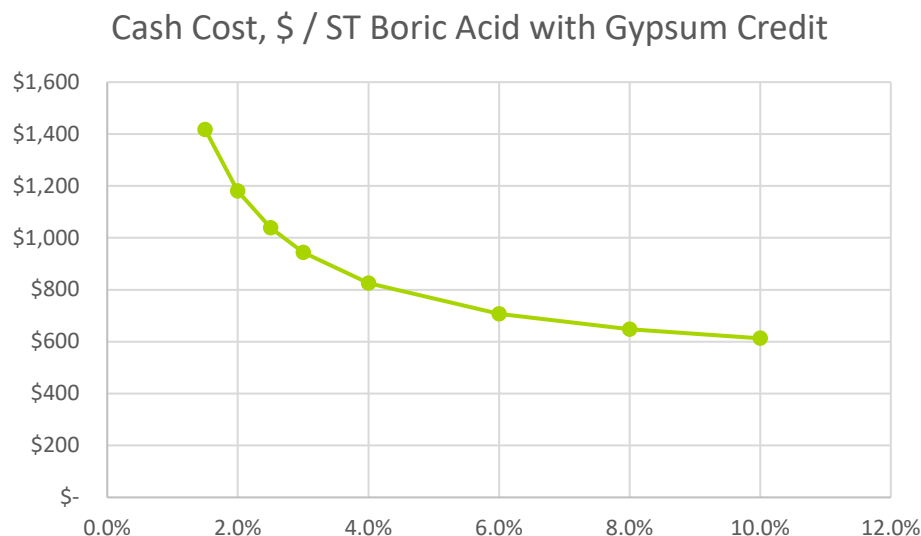
Table 11.6: Cut-off grade analysis

B <sub>2</sub> O <sub>3</sub>	1.5%	2.0%	3.0%	4.0%	6.0%	8.0%	10.0%
Ca:B	6.98	5.47	3.96	3.20	2.45	2.07	1.85
Mg:B	0.13	0.13	0.13	0.13	0.13	0.13	0.13
Na:B	0.34	0.34	0.34	0.34	0.34	0.34	0.34
Max head grade BA wt%	4.4%	4.9%	5.9%	6.7%	7.8%	8.7%	9.3%
Production rate (kst/yr)	40.9	51.3	68.6	82.5	103.6	118.7	130.0
Plant flow (gpm)	880	880	880	880	880	880	880
36% HCl (lb/st)	655	655	655	655	655	655	655
H <sub>2</sub> SO <sub>4</sub> (lb/st)	7,216	5,743	4,270	3,534	2,797	2,429	2,208
Lime (lb/st)	957	821	685	618	550	516	496
Gypsum production (kST/yr)	259	259	257	256	255	253	252
Metal waste (kST/yr)	6.3	7.9	10.6	12.7	16.0	18.3	20.1
NaCl Production (kST/yr)	6.2	7.7	10.4	12.5	15.7	17.9	19.6
Heating (MMBTU/ST)	7.7	7.7	7.7	7.7	7.7	7.7	7.7
Electricity (kwh/ST)	3,424	2,734	2,043	1,698	1,353	1,180	1,078
BTU/ST	21.7	19.2	16.6	15.3	14.1	13.4	13.0
BA Packaging (\$/ST)	\$18.00	\$18.00	\$18.00	\$18.00	\$18.00	\$18.00	\$18.00
BA freight (\$/ST)	\$113.50	\$113.50	\$113.50	\$113.50	\$113.50	\$113.50	\$113.50
Variable cost (\$/ST)	\$877.98	\$749.52	\$621.06	\$556.83	\$492.60	\$460.49	\$441.20
Fixed cost (\$/ST)	\$746.52	\$595.99	\$445.45	\$370.19	\$294.92	\$257.29	\$235.00
Cash cost (\$/ST)	\$1,624.50	\$1,345.51	\$1,066.52	\$927.02	\$787.53	\$717.78	\$676.20
Cash cost w/ credit (\$/ST)	\$1,417.49	\$1,180.75	\$944.01	\$825.64	\$707.27	\$648.09	\$612.85

Sales pricing has risen over the past several years and is currently tracking around \$1,100 to \$1,300 per short ton F.O.B. in the spot market as of July 2025. For this evaluation, current pricing was used along with price forecasting based on the preliminary market study performed by Kline.

Figure 11.2 plots the cutoff grade relative to cash costs. The result of this exercise is a 2.0% financially viable cutoff grade, where our cash costs are near the current and forecasted boric acid pricing at the commencement of production. The geological model used a 2.0% B<sub>2</sub>O<sub>3</sub> cutoff grade which has a boric acid equivalent cutoff of 3.55% boric acid.

Figure 11.2: Cash costs, \$/st of boric acid



## 11.5 Mineral Resource Estimation

Results of the mineral resource estimation are shown in Table 11.7. Below, Figure 11.3 shows resource classification of the Project. The resource estimate for lands under mineral control by 5E contains a combined 109.13 million short tons of measured plus indicated resources with an average grade of 7.89% B<sub>2</sub>O<sub>3</sub> and 303 ppm Li, using a 2.0% cut-off grade

for  $B_2O_3$ . The mineral resource estimate also identifies 3.35 million short tons of inferred resources under mineral control. Uncontrolled land (State of California Surface) contains approximately 22.36 million short tons of measured plus indicated resources and an inferred resource of 0.93 million short tons. The electrical transmission corridor contains 27.78 million short tons or 25% of the total mineral resources are contained within the electrical transmission corridor operated by SCE. While SCE maintains control of the surface and resources to a depth of 500 ft, it does not impinge on SE's mineral rights for  $B_2O_3$  and Li which occur at depths greater than 1,000 ft.

It is noted that these numbers are different to previous reports, which are ascribed to the change in cut-off grade as detailed in Section 11.4 and Section 3.6 as well as an increase in mineral tenure. Regulation S-K 1300 requires a current economic assessment to be completed which provides a reasonable basis for establishing the prospects of economic extraction of the mineral resource estimation.

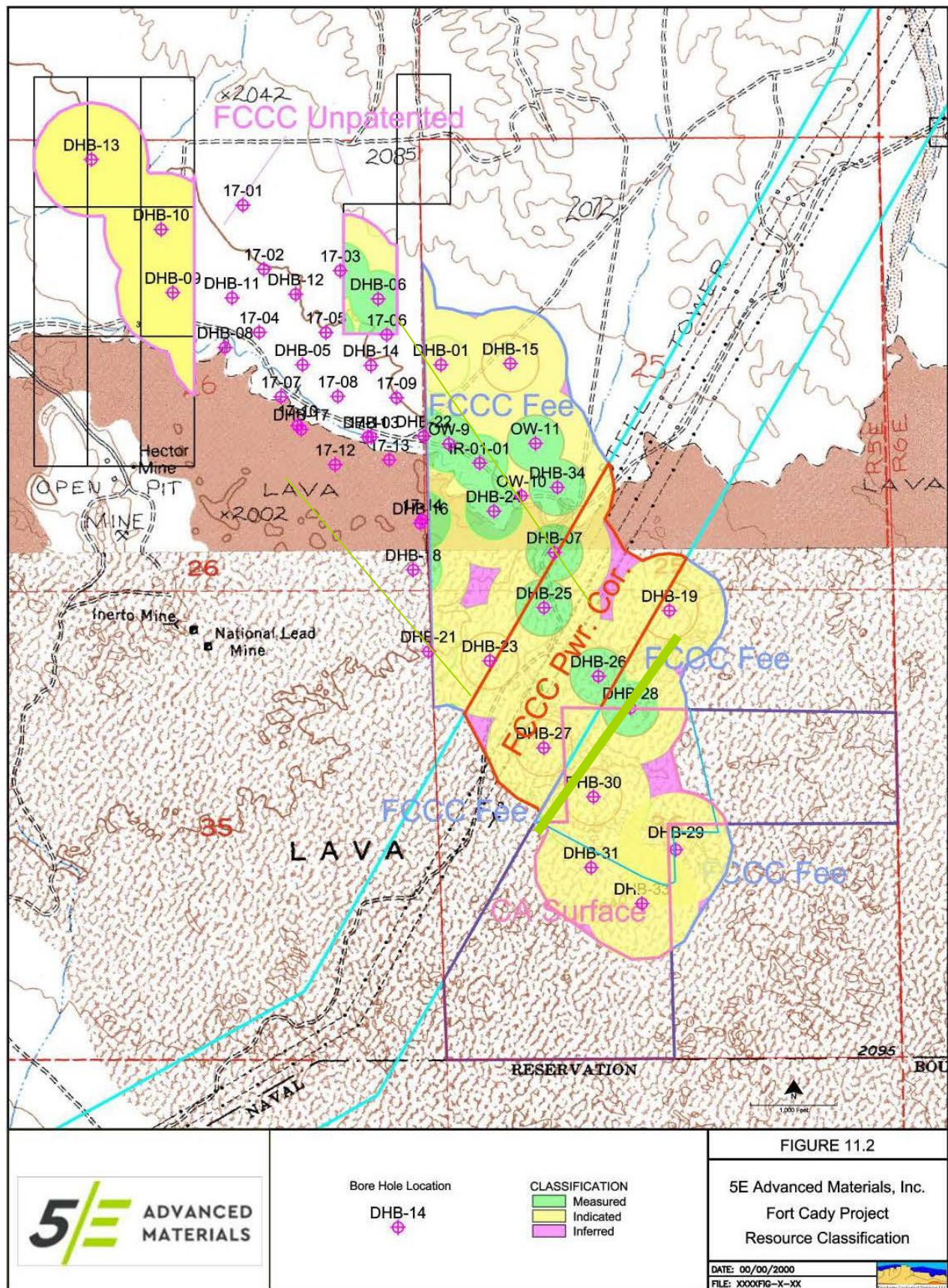
Table 11.7: Fort Cady Project mineral resource estimate\*, March 10, 2025

Property	Bed	Thick (m)	B <sub>2</sub> O <sub>3</sub> %	H <sub>3</sub> BO <sub>3</sub> %	LI ppm	LCE %	Tonnes	Tons	Resource Classification Tons			Product Tons - Measured			Product Tons - Indicated			Product Tons - Inferred		
									Measured	Indicated	Inferred	B <sub>2</sub> O <sub>3</sub>	H <sub>3</sub> BO <sub>3</sub>	LCE	B <sub>2</sub> O <sub>3</sub>	H <sub>3</sub> BO <sub>3</sub>	LCE	B <sub>2</sub> O <sub>3</sub>	H <sub>3</sub> BO <sub>3</sub>	LCE
Unpatented Lode Claims	UMH	1.29	6.95	12.34	305.2	0.16	1,019,259	1,123,540	134,825	988,715	-	9,370	16,642	219	68,716	122,039	1,606	-	-	-
	MMH	5.81	8.53	15.15	382.3	0.20	4,604,120	5,075,172	609,021	4,466,151	-	51,949	92,262	1,239	380,963	676,590	9,089	-	-	-
	IMH	10.02	6.66	11.82	334.1	0.18	7,930,744	8,742,146	1,049,058	7,693,089	-	69,824	124,008	1,866	512,046	909,393	13,681	-	-	-
	LMH	5.18	9.42	16.73	252.7	0.13	4,097,952	4,517,217	542,066	3,975,151	-	51,069	90,698	729	374,505	665,121	5,348	-	-	-
Sub-Total							17,652,074	19,458,075	2,334,969	17,123,106	-	182,213	323,610	4,053	1,336,229	2,373,143	29,724	-	-	-
Fee Land	UMH	2.96	6.60	11.72	250.6	0.13	5,239,482	5,775,538	1,443,885	4,216,143	115,511	95,296	169,246	1,926	278,265	494,199	5,624	7,624	13,540	154
	MMH	15.25	8.23	14.62	323.0	0.17	26,950,960	29,708,340	7,427,085	21,687,088	594,167	611,249	1,085,578	12,770	1,784,847	3,169,889	37,289	48,900	86,846	1,022
	IMH	6.09	7.24	12.85	349.4	0.19	10,770,455	11,872,391	2,968,098	8,666,845	237,448	214,781	381,451	5,520	627,160	1,113,837	16,119	17,182	30,516	442
	LMH	8.11	8.63	15.33	222.9	0.12	14,330,824	15,797,025	3,949,256	11,531,828	315,941	340,831	605,316	4,686	995,227	1,767,523	13,682	27,266	48,425	375
Sub-Total							57,291,720	63,153,293	15,788,323	46,101,904	1,263,066	1,262,157	2,241,592	24,902	3,685,500	6,545,448	72,714	100,973	179,327	1,992
Power Corridor	UMH	2.57	5.91	10.50	2.7	0.00	2,094,642	2,308,947	415,611	1,731,711	161,626	24,563	43,623	6	102,344	181,763	25	9,552	16,965	2
	MMH	22.06	7.83	13.91	277.0	0.15	17,965,945	19,804,059	3,564,731	14,853,044	1,386,284	279,118	495,714	5,256	1,162,993	2,065,476	21,900	108,546	192,778	2,044
	IMH	4.40	5.09	9.04	279.0	0.15	3,580,525	3,946,852	710,433	2,960,139	276,280	36,168	64,234	1,055	150,699	267,642	4,396	14,065	24,980	410
	LMH	4.25	7.83	13.90	250.0	0.13	3,461,337	3,815,470	686,785	2,861,603	267,083	53,754	95,466	914	223,973	397,776	3,808	20,904	37,126	355
Sub-Total							27,102,450	29,875,328	5,377,559	22,406,496	2,091,273	393,602	699,038	7,231	1,640,010	2,912,658	30,129	153,068	271,848	2,812
Total							102,046,244	112,486,697	23,500,851	85,631,507	3,354,339	1,837,973	3,264,240	36,186	6,661,739	11,831,248	132,567	254,040	451,175	4,804
CA Surface Section 36 (Uncontrolled)	UMH	4.78	6.99	12.41	313.2	0.17	3,788,533	4,176,141	167,046	3,842,050	167,046	11,676	20,737	279	268,559	476,961	6,406	11,676	20,737	279
	MMH	14.02	6.76	12.01	376.0	0.20	11,109,308	12,245,912	489,836	11,266,239	489,836	33,113	58,809	980	761,598	1,352,598	22,549	33,113	58,809	980
	IMH	4.88	3.66	6.50	340.3	0.18	3,869,439	4,265,325	170,613	3,924,099	170,613	6,243	11,088	309	143,590	255,016	7,109	6,243	11,088	309
	LMH	2.98	6.18	10.98	465.9	0.25	2,358,930	2,600,274	104,011	2,392,252	104,011	6,431	11,422	258	147,921	262,708	5,933	6,431	11,422	258
Uncontrolled Total							21,126,210	23,287,653	931,506	21,424,641	931,506	57,464	102,056	1,826	1,321,669	2,347,283	41,996	57,464	102,056	1,826

\* Denotes 2.0% cut-off



Figure 11.3: Resource classification



## 11.6 Uncertainties

The QP is not aware of any known environmental, permitting, legal, title, taxation, socio-economic, marketing, or other relevant factors or uncertainties that could affect the mineral resource estimate.

The accuracy of resources and reserve estimates is, in part, a function of the quality and quantity of available data and of engineering and geological interpretation and judgment. Given the data available at the time this report was prepared, the estimates presented herein are considered reasonable. However, they should be accepted with the understanding that additional data and analysis available after the date of the estimates may necessitate revision. These revisions may be material. There is no guarantee that all or any part of the estimated resources or reserves will be recoverable.

## 11.7 Individual Grade for Each Commodity

Included with Section 11.5.

## 11.8 Disclose Required Future Work

Approximately 96% of the deposit is measured plus indicated resources. Though there is potential to expand the resource with step-out drilling, there are more than sufficient resources defined to focus efforts on development and production.

# 12 Mineral Reserve Estimates

A detailed mine plan was prepared in Section 13 in support of mineral reserves. The EPA UIC permit subdivides the mineralized deposit into three blocks for development. Block 1 comprises the northwestern third of the orebody, Block 2 occupies the central portion of the orebody, and Block 3 comprises the southeastern third of the orebody. The SSF currently operates in Block 2 and Block 2 is permitted for mining with sufficient resources on fee-based lands and within the power corridor to convert resources to reserves on an economic basis, which provides for 39.5 years of mining life. To convert additional resources to reserves, Block 1 and Block 3 would need to be authorized by the EPA and a mine plan devised that includes this mineral tenure.

For economic modeling, a mine plan (Section 10) was designed where recovery and flow rates are sufficient to feed the chemical plant (Section 14) where PLS is converted to a finished refined borate product available for sale. Production output is within permitted parameters with forecasted revenue from borate sales based on a pricing forecast based on a preliminary market study commissioned by 5E, as discussed in Section 16 of this report.

The mine plan and wellfield optimization were based on third-party engineering work that incorporated 18 months of actual wellfield data from the SSF into the design and includes a bottoms-up capital estimate. A capital estimate was derived by Fluor for the inside and outside battery limits above ground and a total capital estimate was derived and incorporated into the economic analysis. The operating costs were derived from material and energy balances provided by Fluor as well as a bottoms-up labor build for human capital requirements. The revenue and cost inputs for the economic model were on a real basis and the economic model yields an NPV of \$725million.

## 12.1 Conversion Assumptions, Parameters, and Methods

All conversion assumptions such as plant efficiency, leaching efficiency, and mining efficiency were taken into consideration to calculate the reserve estimate.

The following steps and assumptions were used to calculate reserves:

- Measured and indicated resource of fee-based land and the power corridor were included as the base resource.
- The mine plan includes 80% of 5E's fee-based lands and 5% of the power corridor.
- Trade off analysis performed based on actual vertical well performance relative to expected horizontal well performance.



- Fluor designed the above ground chemical plant with a 95.1% boric acid yield.
- The leaching efficiency is 81.9% based on leach testing performed by 5E, Hazen, and MSME.
- Mining efficiency is 95% based on the July 2025 horizontal well drill program.
- Discounted cash flow based on capital and operating cost inputs.

Reserves are stated in-situ with a 2.0% cutoff grade established based on the analysis performed with mineral resources in Section 11. Cut-off was established using a long-term forecasted sales price of \$1,350 per ton F.O.B. and a cash cost as detailed in Table 11.6 of \$1,181 per short ton. The long-term price was obtained from a preliminary market study with the price of boric acid having increased, which has been driven by supply-demand fundamentals. B<sub>2</sub>O<sub>3</sub> grade was captured from the measured and indicated grades of the fee-based land and power corridor.

## 12.2 Mineral Reserve Estimate

The mine plan considered measured and indicated resources with measured resources converted to proven reserves and indicated resources converted to probable reserves. The plan design results in 1.4 million tons of boric acid proven reserve and 4.0 million tons of boric acid probable reserve with an average grade of 8.03% boric oxide. The mineral reserve statement, as of August 4, 2025, for the Fort Cady Project is presented in Table 12.3. Table 12.1 provides the proven mineral reserves and Table 12.2 provides the probable mineral reserves. The reference point for the mineral reserves is in-situ.

Table 12.1: Proven mineral reserves

Proven Mineral Reserves							
Bed	Mean Mineralized Bed Thickness (ft)	Avg. B <sub>2</sub> O <sub>3</sub> Grade (wt. %)	Insoluble Material Grade (wt. %)	Mineralized Bed Volume (ft <sup>3</sup> )	Recoverable Mineralized Bed Volume (ft <sup>3</sup> )	B <sub>2</sub> O <sub>3</sub> Reserve Tons	H <sub>3</sub> BO <sub>3</sub> Reserve Tons
UMH	9.08	6.59	52.5	1,924,171	1,497,102	57,319	101,798
MMH	61.18	8.22	56.9	12,492,985	9,720,167	372,149	660,937
IMH	17.20	7.21	55.9	4,312,901	3,355,652	128,476	228,173
LMH	20.27	8.62	54.2	6,839,526	5,321,493	203,740	361,843

Table 12.2: Probable mineral reserves

Probable Mineral Reserves							
Bed	Mean Mineralized Bed Thickness (ft)	Avg. B <sub>2</sub> O <sub>3</sub> Grade (wt. %)	Insoluble Material Grade (wt. %)	Mineralized Bed Volume (ft <sup>3</sup> )	Recoverable Mineralized Bed Volume (ft <sup>3</sup> )	B <sub>2</sub> O <sub>3</sub> Reserve Tons	H <sub>3</sub> BO <sub>3</sub> Reserve Tons
UMH	9.08	6.58	52.5	5,656,611	4,401,126	168,503	299,261
MMH	61.18	8.21	56.9	36,911,677	28,719,130	1,099,550	1,952,800
IMH	17.20	7.20	55.9	12,649,669	9,842,075	376,817	669,227
LMH	20.27	8.62	54.2	20,054,643	15,603,515	597,401	1,060,984

Table 12.3: Mineral reserve statement

Proven and Probable Mineral Reserves						
Reserve	Avg. B <sub>2</sub> O <sub>3</sub> Grade (wt. %)	Insoluble Material Grade (wt. %)	Mineralized Bed Volume (ft <sup>3</sup> )	Recoverable Mineralized Bed Volume (ft <sup>3</sup> )	B <sub>2</sub> O <sub>3</sub> Reserve Tons	H <sub>3</sub> BO <sub>3</sub> Reserve Tons
Proven	8.03	55.7	25,569,583	19,894,414	761,684	1,352,751
Probable	8.03	55.7	75,272,600	58,565,846	2,242,271	3,982,272

## 12.3 Relevant Factors

The reserve statement herein is subject to potential change based on changes to the forward-looking cost and revenue assumptions utilized in this TRS. It is assumed that 5E will produce and sell borates to customers once the LSBF is constructed, commissioned, and in operation. Full extraction of this reserve is dependent upon the modification of the UIC permit to include the finalized mine plan based on the learnings obtained from the Company's horizontal wells. 5E

obtained a minor modification and authorization to drill the horizontal and sidetrack program in July 2025 and it is 5E's expectation that it will be successful in modifying the UIC permit. In the QP's opinion, 5E's expectation is reasonable. The evaporation ponds incorporated into the design of the LSBF and placed on 5E's fee-based land require a waste discharge permit (WDR) with the Lahontan Regional Water Quality Control Board. 5E had a WDR for evaporation ponds and 5E expects to obtain the WDR for the evaporation ponds to remove calcium and sodium. In the QP's opinion, 5E's expectation is reasonable.

The QP is not aware of other existing environmental, permitting, legal, socio-economic, marketing, political, or other factors that might materially affect the in-situ mineral reserve estimate. An increase to mineral reserves is possible as the current mine plan only captures approximately 41% of the resource. Additionally, an exploration target is available which, with further exploration work, could increase the resource and provide potential to increase the mineral reserves.

## 13 Mining Methods

Given the geological and stratigraphic suitability, the Project will be employing ISL as its mining method to recover borates from the mineralized horizons. Depth and grade of the deposit precludes conventional mining techniques such as open pit and underground mining as effective methods for economical extraction of ore. With ISL mining, there is no stripping of waste rock or underground development required for the Project. Mine development steps include drilling and constructing of injection/recovery wells (IR Wells), installing pumping or airlifting extraction equipment on wells, and piping to transport leach solutions to the wellfield and PLS to the chemical plant for processing. Mining fleet and machinery are not required for the Project.

The process designed by 5E and Fluor assumed an initial production rate of 130,000 stpa boric acid. This production rate should correspond to 880 – 900 gallons/min of PLS to the processing plant, assuming a head grade of 10.2% weight boric acid in the PLS (160°F), and 95.1% yield of boric acid in the processing plant. This translates to a minimum of 100 gpm production from at least nine wells during recovery phase of injection cycles when operating under the proven cyclic injection-residence-recovery well operation. Required well production capacity will be minimized when recovering from dedicated production wells outside of the cyclic cycle and/or during continuous mining operation of horizontal wells.

Based on the results of operating the SSF injection – recovery wells and preliminary work completed by 5E, the LSBF calls for the installation of 27 directional wells targeting the upper mineralized horizon (UMH), major mineralized horizon (MMH), and lower mineralized horizon (LMH) spaced at 200-ft horizontal offset and 120 – 180-ft vertical spacing. Operating strategy of the wells will focus on high-grade mineralization zone cavern development through continuous injection and cyclic push-pull mechanics. These wells are to operate as injection and recovery wells whereby injection and recovery of lixiviant through separate horizontal wellbores and full reservoir contact is accomplished by geo-steered laterals in a “fishbone” pattern and positively intercepting each well. The leach solution (lixiviant) is pumped into the well and, after a prescribed residence time, is retrieved from the same well, or offset wells as caverns develop, for processing. This method will be used until the dissolution of the colemanite in the deposit progresses to where complete reservoir flow is established between regional groups of wells.

### 13.1 Geotechnical and Hydrological Model Contribution to Mine Design

The mineralized body exists in four major evaporite sequences totaling approximately 108-ft thickness and comprised of interbedded layers of claystone, anhydrite, heulandite, biotite, quartz, and muscovite, inhibiting permeability. The Major Mineralized Horizon contains 40 – 60% colemanite in nearly continuous 50 – 60-ft thick intervals providing the basis for targeting for primary wells. Upper Mineralized Horizon (UMH) contains 30 – 50% colemanite in semi-continuous 15 – 20-ft thick intervals interbedded with associated insoluble material providing the targeting basis secondary wells. Lower Mineralized Horizon (LMH) contains 40 – 60% colemanite in nearly-continuous 15 – 18-ft thick intervals. The Intermediate Mineralized Horizon (IMH) is in the target range with the MMH for wellfield development and mine planning.

Static geotechnical model and drilling programs indicate orebody deposition exists in stratigraphically continuous beds at an 8 – 10° NE – SW inclination. Regional water monitoring wells have indicated solution migration and pore pressure transmission along this inclination of the orebody from IR Wells via transducer response from monitoring wells. Micro-deformation instrumentation has provided fluid migration via plume tracking of injected fluids to confirm orebody dip migration of lixiviant. Incorporating an operating strategy to utilize injection wells with the end of the well placed up-dip provides the opportunity to leverage the downward dip of the 8 – 10° inclination to ensure solvent flows downward through the orebody dissolving colemanite. Since production wells down-dip and the plan equips the bottom of wells with jet pumps to efficiently lift the PLS to surface, this operating strategy utilizes the natural 8 – 10° inclination and gravity to assist with recovery. This knowledge supports a mine plan for a 27-well network to manage cavity formation and maintain artificial lift when operating wells within each horizon.

Well planning of mineralized horizons and the sequence of the drilling program utilize directional drilling to target MMH/IMH in a primary set of IR Wells in 90 – 92° trajectory drilled along the strike of orebody, perpendicular to the 8 – 10° structural dip/inclination. The horizontal well's extended reach along the strike enables multiple injection/production points via perforated intervals and slotted liners promoting uniform dissolution of colemanite and ensures effective leaching across a wider area than vertical well patterns. Gravity driven flow of the solvent from up-dip wells to dedicated production wells at lower elevations de-risks fluid injection leak off concerns and higher probability of fluid capture, which is necessary for maintaining hydraulic gradient per the EPA UIC permit.

Vertical production wells have indicated that wellbore collapse due to collapsing clay will not occur if the operating strategy is followed. Reservoir re-charge to wellbore is greater than geo-mechanical collapse stress and is evident during recovery phase of production cycles. Pilot horizontal wells will run geophysical logging tools to quantify degree of geo-mechanical collapse stresses and jet pump deployment will confirm quantification. Given the estimated degree of geo-mechanical stability within the mineralized zones, directional and horizontal wellbores become feasible as tools of scaling to increase contact area by a factor of 20X with a 3,450-ft lateral well and permeability driven sustainable injection rates of +100 gpm.

### 13.2 Artificial Lift

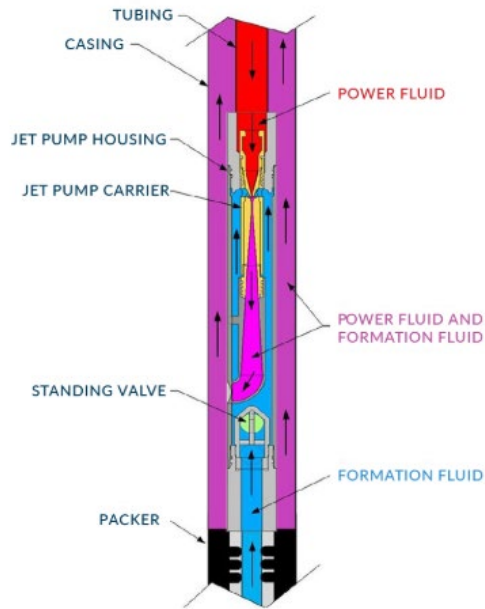
Current recovery method at the SSF wellfield is airlifting solution using compressed air injected into production tubing to force fluids up the backside annulus of the well between 7-in casing and production tubing. Average recovery rates are approximately 15 – 20 gpm and heavily rely on reservoir pressure to maintain higher recovery rates. The LSBF design includes installation of jet pump systems due to proven designs with artificial lift in oil and gas fields and ability to recover higher rates of PLS needed for commercial plant design.

Hydraulic jet pumps are planned as the primary means of PLS recovery from the orebody when reservoir pressure has not been maintained for adequate recovery rates between a network of communicating wells within a target horizon. Each dual use IR Well and dedicated production well will contain a jet pump BHA (bottom-hole assembly) constructed of corrosion resistant alloy (CRA) and the possible addition of corrosion inhibitor to ensure adequate production rates of PLS. Jet pumps have no moving parts and operate using a high-pressure fluid to create a Venturi effect, drawing reservoir fluids into the pump and lifting to the surface.

Each jet pump will consist of a nozzle, throat, and diffuser. High-pressure power fluid is pumped from the surface through the nozzle, creating a high velocity, low-pressure jet which draws in corrosive reservoir PLS from the wellbore and mining region in the absence of reservoir pressure. The mixed fluids (power fluid + PLS) pass through the diffuser where kinetic energy is converted back to pressure, enabling the fluid to be lifted to surface. The absence of moving parts reduces the need for maintenance and the ability of the jet pumps to tolerate solids without significant wear. The diagram in Figure 13.1 below provides the assembly structure of the jet pump.

Typical jet pump systems in oil and gas applications are frequently used to produce residual acid with minimal erosion and corrosion to conventional steel designs. 5E anticipates near-term deployment of a conventional jet pump to prove out required recovery rates of leachate. Deployment of exotic alloy jet pump expected in Q4 2025 to acquire data on possible further optimization of wellfield strategy.

Figure 13.1: jet pump assembly



### 13.3 Wellfield Operating Strategy

The wellfield will be operating under an artificially induced reservoir pressure environment with the main objective of maintaining a high enough productivity index while remaining below the established fracture gradient. Maintenance of reservoir pressure will be key to achieving adequate recovery rates of PLS from each targeted horizon, particularly for offset wells within direct communication where displacement of reacted HCl will need to be recovered at surface. The network of 27 jet pumps will be key to maintaining the ability of the orebody to deliver fluids to the wellbore by recovering fluid during production phase and circulation of unspent or reacted HCl during injection phase.

In addition to recovery rate of fluids, the installation of a jet pump network provides the ability to maintain a high temperature power fluid to the reservoir fluid and maintain a critical temperature needed for boric acid to remain in solution. Installation of the centralized surface facility (CSF) will supply high-pressure power fluid to multiple jet pumps across the 27 well network, recovering and circulating fluid as needed. After lifting at-grade PLS to surface, the power fluid and produced fluid are separated at surface with PLS directed towards plant and lower concentration PLS recycled and directed towards the next group of wells undergoing recovery operations.

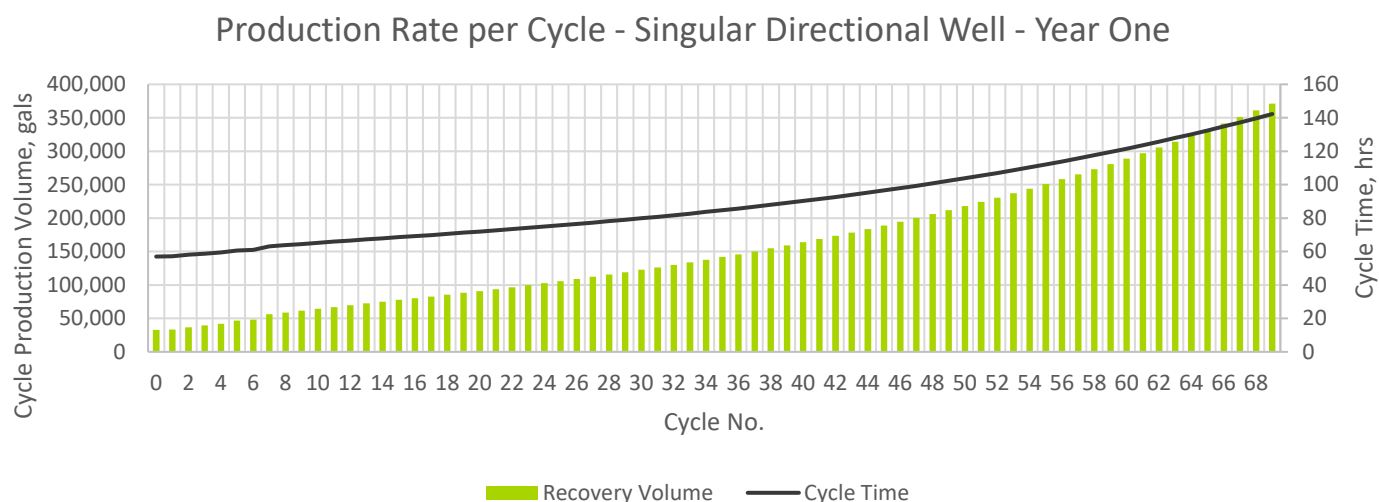
Dissolution kinetics of the rate at which colemanite dissolves and boron is extracted assumes that the solid colemanite particle reacts with HCl, and the reaction front moves inward as mineralized particles dissolve. Geo-steered wells adjust the wellbore path using measurement while drilling (MWD) and logging while drilling (LWD) technology to ensure the well stays within target horizon. The rate of dissolution is mainly controlled by film diffusion of HCl through the liquid boundary layer, underground surface reaction between HCl and colemanite, and diffusion of reaction products through a porous layer of undissolved precipitates. To progressively leach the orebody in required amounts, greater volumes of fluid will need to be injected to replace previously leached volume and contact new colemanite. The underground surface chemical reaction is the rate-controlling step because the reaction at the colemanite surface is slower than the diffusion of HCl to the mineralized particle or removal of products, thus resource temperature needs to be maintained at dissolution levels to produce required head grades. Table 13.1 below provides the parameters for which the wellfield operating strategy will be deployed, and Figure 13.2 provides the first-year production rates per cycle.

Table 13.1: Wellfield operating strategy mining parameters

Well Group	Unit	MMH	UMH	LMH	IMH
Geologic Unit	horizon	Major	Upper	Lower	Intermediate
Colemanite Reserve	tons	3,270,047	501,765	1,780,099	1,122,736
MMH Reserve, H <sub>3</sub> BO <sub>3</sub>	tons	2,613,737.67	401,058.83	1,422,827.36	897,399.29
No. of Wells	each	9.00	9.00	9.00	* accounted in MMH
Well Completion	type	Open-Hole, limited entry perforated tubing, liner hanger	Open-Hole, limited entry perforated tubing, liner hanger	Open-Hole, limited entry perforated tubing, liner hanger	Open-Hole, limited entry perforated tubing, liner hanger
Avg Length	ft	3,450	3,450	3,450	3,450
Avg Thickness	ft	61.18	9.08	20.27	17.20
Group Injection Rate	gpm	1,125	1,170	1,350	1,125
Group Production Rate	gpm	1,125	1,170	1,350	1,125
H <sub>3</sub> BO <sub>3</sub> tons per year (TPY)	tons	43,333	43,333	43,333	*
Colemanite Mass Leached, TPY	tons	74,377	77,352	89,252	*
Horizon Life	years	43.97	6.49	19.94	*
Mining Efficiency	%	95.0	95.0	95.0	*
Leaching Efficiency	%	81.9	81.9	81.9	*
Plant Efficiency	%	95.1	95.1	95.1	*
Dedicated Injection Wells	each	1.0	-	-	*
Dedicated Production Wells	each	1.0	-	-	*
Dual Injection/Recovery Wells	each	7.00	9.00	9.00	*

\*Accounted for in MMH

Figure 13.2: Year 1 production rates per cycle



The mine plan utilizes in-situ leaching operations via lixiviant solutions to mine the colemanite resource in place without physically removing large volumes of ore or overburden. The process relies on the natural and enhanced permeability of the deposit to allow leaching solution to flow through and dissolve targeted mineralization. Solution mining accesses the colemanite deposit through wells drilled into the orebody, where leaching solution is then injected directly into the mineralized zone. The colemanite mineral's moderate solubility combined with its geological and stratigraphic suitability allows leaching solutions to extract boron without stripping the surface or backfilling voids from underground development.

Mine recovery rate (leaching efficiency) of 81.9% is applied to account for losses for leaching solution not reaching and reacting with the ore body, as well as for non-recoverable saturated solution underground. This is based on studies conducted by 5E, Hazen, and MSME. Leaching efficiency requires lixiviant to contact colemanite, therefore an additional "mining efficiency" factor for fluid to contact colemanite probability has been introduced to account for reduction



anomalies due to wellbore traversing in lower grade zones or discontinuous colemanite beds along horizontal well paths. The mining efficiency factor is based on drilling experience during a 3000-ft horizontal well and sidetrack program deployed in July 2025 which tested drill cuttings using ICP-OES and confirmed approximately 95% of the wellbore was in the planned zone. Table 13.2 below provides the ICP-OES results from the horizontal well program.

Table 13.2: Horizontal well program ICP-OES results (July 7, 2025)

Test Sample ID	Depth (md ft)	Date	Test Date	Al (ppm)	As (ppm)	B (ppm)	B (wt. %)	Ca (ppm)	Fe (ppm)	K (ppm)	Li (ppm)	Mg (ppm)	Mn (ppm)	Na (ppm)	S (ppm)	Si (ppm)	Sr (ppm)	Ti (ppm)	Zn (ppm)
7092563	1090-1100	7/7/2025	7/17/2025	1,429	49	261	0.1%	125,607	2,233	6,279	-	1,896	590	4,802	>38,702	2,485	6,210	21	-
7092562	1190-1200	7/7/2025	7/17/2025	954	133	370	0.2%	101,618	2,752	6,026	-	1,795	347	9,440	>43,670	1,462	6,224	-	-
7092561	1220-1230	7/7/2025	7/17/2025	1,073	96	451	0.3%	100,893	1,852	7,782	-	2,058	272	6,911	>42,540	1,478	8,714	-	-
7092560	1230-1240	7/7/2025	7/17/2025	1,179	192	567	0.3%	113,484	3,433	7,240	-	2,002	332	8,914	>42,951	1,515	3,806	-	-
7092559	1240-1250	7/7/2025	7/17/2025	2,308	67	602	0.3%	45,406	2,611	10,940	-	2,146	186	13,398	>27,689	1,554	7,538	-	-
7092558	1250-1260	7/7/2025	7/17/2025	1,206	111	603	0.3%	99,541	3,605	9,300	-	2,056	474	6,951	>41,829	1,191	2,783	-	-
7092557	1260-1270	7/7/2025	7/17/2025	1,419	123	774	0.4%	135,328	3,629	9,211	-	1,710	446	7,660	>43,335	1,271	4,382	-	-
7092556	1270-1280	7/7/2025	7/17/2025	1,572	123	1,040	0.6%	116,244	3,276	8,530	-	1,683	425	8,870	>43,810	1,147	2,761	-	-
7092555	1280-1290	7/7/2025	7/17/2025	1,646	88	390	0.2%	82,825	2,059	11,775	-	1,868	277	7,276	>44,076	1,514	3,686	-	-
7092554	1290-1300	7/7/2025	7/17/2025	1,325	84	600	0.3%	103,330	2,181	4,191	-	1,713	303	4,821	>43,003	1,679	4,099	-	-
7092553	1370-1380	7/7/2025	7/17/2025	1,380	125	810	0.5%	113,453	2,612	9,955	-	2,714	300	9,277	>42,004	-	12,491	-	-
7092552	1380-1390	7/7/2025	7/17/2025	913	202	822	0.5%	156,475	2,809	8,358	-	2,303	334	6,742	>42,702	1,288	13,441	-	-
7092551	1390-1400	7/7/2025	7/17/2025	1,565	323	1,205	0.7%	128,577	4,084	8,446	-	2,608	296	9,043	>42,849	1,397	11,787	-	-
7092550	1400-1410	7/7/2025	7/17/2025	838	206	10,478	6.0%	175,003	2,289	8,333	-	1,996	306	5,845	>44,070	1,292	13,966	-	-
7092549	1410-1420	7/7/2025	7/17/2025	1,041	162	9,456	5.4%	147,142	2,307	7,282	-	2,652	280	7,079	>43,938	1,572	4,219	-	-
7092548	1420-1430	7/7/2025	7/17/2025	1,289	169	7,031	4.0%	123,375	3,127	8,459	-	2,642	277	7,845	>44,396	1,564	7,765	-	-
7092547	1430-1440	7/7/2025	7/17/2025	1,198	116	5,288	3.0%	173,385	1,858	7,458	-	2,691	287	7,329	>43,984	1,410	10,056	-	-
7092546	1440-1450	7/7/2025	7/17/2025	781	115	11,449	6.5%	157,714	1,256	6,834	-	1,983	263	6,230	>42,023	1,080	8,933	-	-
7092545	1530-1540	7/7/2025	7/15/2025	649	141	16,792	9.6%	192,185	1,343	5,246	-	1,398	183	405	>52,789	1,079	17,493	-	-
7092544	1550-1560	7/7/2025	7/15/2025	1,378	163	7,387	4.2%	176,049	2,547	7,565	-	1,725	194	1,957	>52,386	1,599	10,261	-	220
7092543	1580-1590	7/7/2025	7/15/2025	813	74	17,522	10.0%	>206,819	1,248	2,417	-	947	193	377	>51,705	1,331	10,044	-	163
7092542	1690-1700	7/7/2025	7/15/2025	493	133	7,901	4.5%	>197,773	2,106	3,969	-	1,332	160	2,966	>49,443	1,617	14,302	-	167
7092541	1780-1800	7/7/2025	7/15/2025	-	87	4,274	2.4%	201,932	1,936	4,191	-	1,054	212	866	>54,254	1,379	13,362	-	230
7092540	1800-1820	7/7/2025	7/15/2025	401	166	10,417	6.0%	>206,458	2,923	4,377	-	1,486	455	1,700	>51,615	1,727	18,578	-	156
7092539	1820-1840	7/7/2025	7/14/2025	292	197	35,684	20.4%	>167,183	2,618	6,990	-	1,501	273	4,580	>41,796	1,529	17,113	-	-
7092538	1840-1860	7/7/2025	7/14/2025	310	189	35,610	20.4%	>153,839	2,720	6,670	-	1,476	265	4,458	>38,460	1,416	17,058	-	-
7092537	1860-1880	7/7/2025	7/14/2025	718	141	42,442	24.3%	>159,921	3,284	6,309	-	1,427	210	2,841	>39,980	1,219	14,588	-	-
7092536	1880-1900	7/7/2025	7/14/2025	605	126	23,761	13.6%	>167,104	2,202	6,204	-	1,328	221	2,285	>41,776	1,035	15,672	-	-
7092535	1900-1920	7/7/2025	7/14/2025	582	132	29,091	16.6%	>17,895	2,140	6,331	-	1,355	266	2,968	>44,724	1,401	18,983	-	-
7092534	1920-1940	7/7/2025	7/14/2025	997	171	19,077	10.9%	133,397	2,811	11,536	-	1,737	196	2,653	>43,156	1,209	15,413	-	-
7092533	1940-1960	7/7/2025	7/9/2025	-	192	33,517	19.2%	>155,231	1,875	6,611	90	1,074	145	1,347	>38,808	1,075	15,226	82	-
7092532	1960-1980	7/7/2025	7/9/2025	63	222	49,058	28.0%	>155,569	2,222	6,539	91	1,013	105	1,056	>38,892	656	13,455	80	-
7092531	1980-2000	7/7/2025	7/9/2025	304	379	10,202	5.8%	>138,112	1,909	8,576	91	1,429	128	1,505	>34,528	4,611	8,094	75	-
7092530	2000-2020	7/7/2025	7/9/2025	157	155	19,179	11.0%	>137,156	1,691	8,113	87	1,409	94	1,937	>34,289	811	7,930	69	-
7092529	2020-2040	7/7/2025	7/9/2025	277	176	17,087	9.8%	>141,037	2,278	11,755	104	1,667	61	3,343	>39,921	1,158	10,534	86	-
7092528	2040-2060	7/7/2025	7/9/2025	-	163	43,631	24.9%	>161,324	1,237	6,670	89	988	85	1,989	>40,331	912	15,596	79	-
7092527	2060-2080	7/7/2025	7/9/2025	75	191	16,692	9.5%	>156,423	2,009	9,584	88	1,246	139	2,552	>39,106	1,028	11,085	81	-
7092526	2100-2120	7/7/2025	7/9/2025	-	158	16,692	9.5%	>155,883	1,353	6,995	93	1,215	97	2,268	>38,971	1,010	12,078	77	-
7092525	2180-2200	7/7/2025	7/9/2025	-	122	16,918	9.7%	>157,460	830	2,519	75	762	48	-	>39,365	727	8,635	76	-
7092524	2220-2240	7/7/2025	7/9/2025	-	141	27,287	15.6%	>158,720	1,072	2,392	82	752	37	248	>39,680	1,074	10,737	83	-
7092523	2280-2300	7/7/2025	7/9/2025	-	148	12,674	7.2%	>146,014	1,202	3,586	74	984	77	490	>36,503	1,169	9,618	74	-
7092522	2380-2400	7/7/2025	7/9/2025	-	146	9,210	5.3%	>165,228	1,104	2,160	86	918	101	1,445	>41,307	1,150	10,993	84	-
7092521	2548	7/7/2025	7/9/2025	-	165	7,976	4.6%	>159,690	1,228	2,233	86	882	122	382	>39,922	961	11,579	81	-
7092520	2580-2600	7/7/2025	7/9/2025	37	238	2,696	1.5%	>171,634	2,321	5,803	108	1,431	144	1,445	>42,908	900	8,782	88	-
7092519	2600-2620	7/7/2025	7/9/2025	-	206	7,440	4.3%	>161,274	2,003	4,912	105	1,346	101	1,616	>40,319	1,176	11,114	87	-
7092518	2640-2660	7/7/2025	7/9/2025	212	172	12,033	6.9%	>144,798	1,945	8,102	108	1,484	87	2,426	>36,199	1,408	13,307	82	-
7092517	2680-2700	7/7/2025	7/9/2025	47	160	14,388	8.2%	>149,230	1,391	5,160	98	1,162	52	1,518	>37,308	1,386	13,046	80	-
7092516	2780-2800	7/7/2025	7/9/2025	108	157	6,899	3.9%	>159,966	1,523	4,711	100	1,259	103	924	>39,991	1,257	10,514	90	-
7092515	2880-2900	7/7/2025	7/9/2025	77	201	6,021	3.4%	>156,296	2,067	4,207	89	1,117	130	1,020	>39,074	1,288	12,675	80	-
7092514	2980-3000	7/7/2025	7/9/2025	131	162	4,054	2.3%	>162,181	1,688	5,649	94	941	80	1,374	>40,543	1,276	10,815	82	-
7092513	3022	7/7/2025	7/9/2025	122	146	35,828	20.5%	>140,990	1,222	3,236	82	810	65	1,043	>35,247	1,431	10,926	70	-

The EPA UIC permit subdivides the mineralized deposit into three blocks for development. Block 1 comprises the northwestern third of the orebody, Block 2 occupies the central portion of the orebody, and Block 3 comprises the southeastern third of the orebody. The SSF currently operates in Block 2 and Figure 13.3 presents the commercial mine plan of the 27 wells in Block 2. Figure 13.4 provides an example of the cross section in Block 2 and the MMH wells with vertical spacing while Figure 13.5 provides an example of the cross section in Block 2 and the MMH wells with lateral spacing. To permit mining of Block 1 and Block 3, the EPA UIC permits will require additional monitoring wells to be installed and baseline parameters to be established via sampling and laboratory testing. Block 2 has established enough resources and reserves for the first phase of mining.

Figure 13.3: LSBF block 2 mine plan



Figure 13.4: Block 2 mining cross section – MMH wells vertical spacing

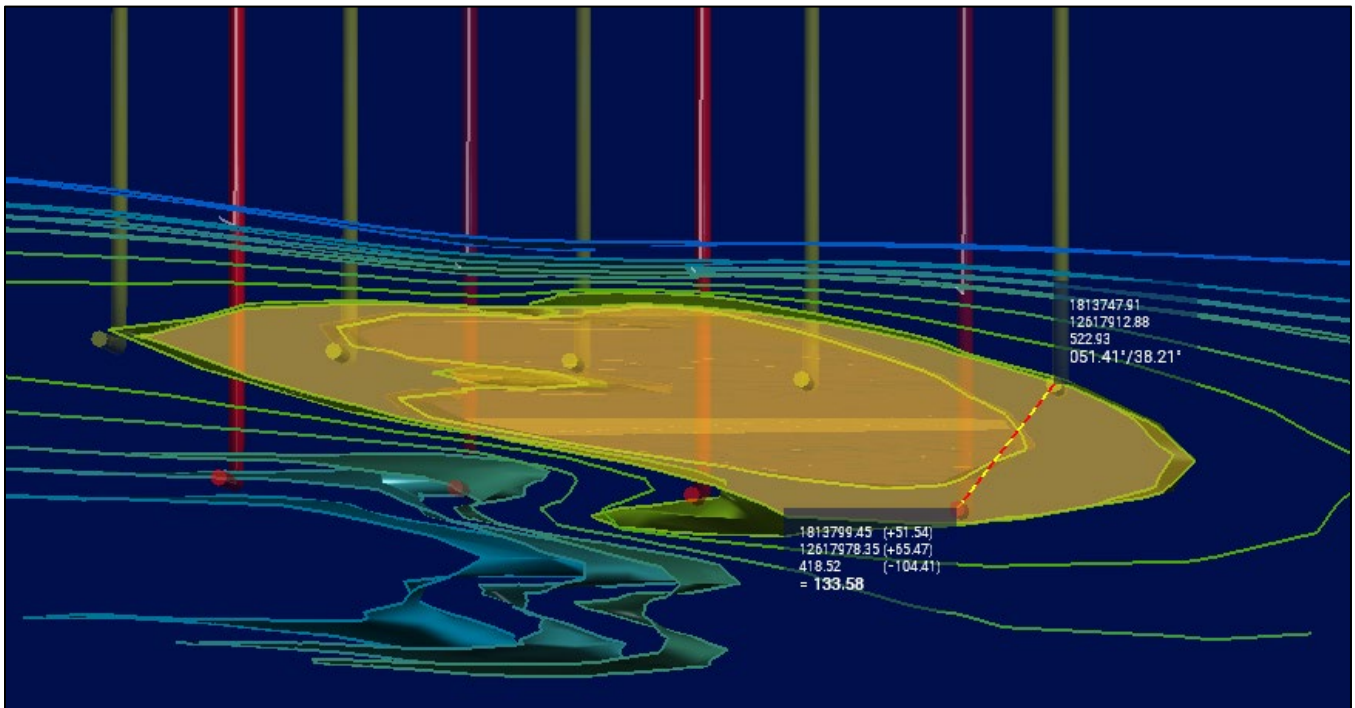
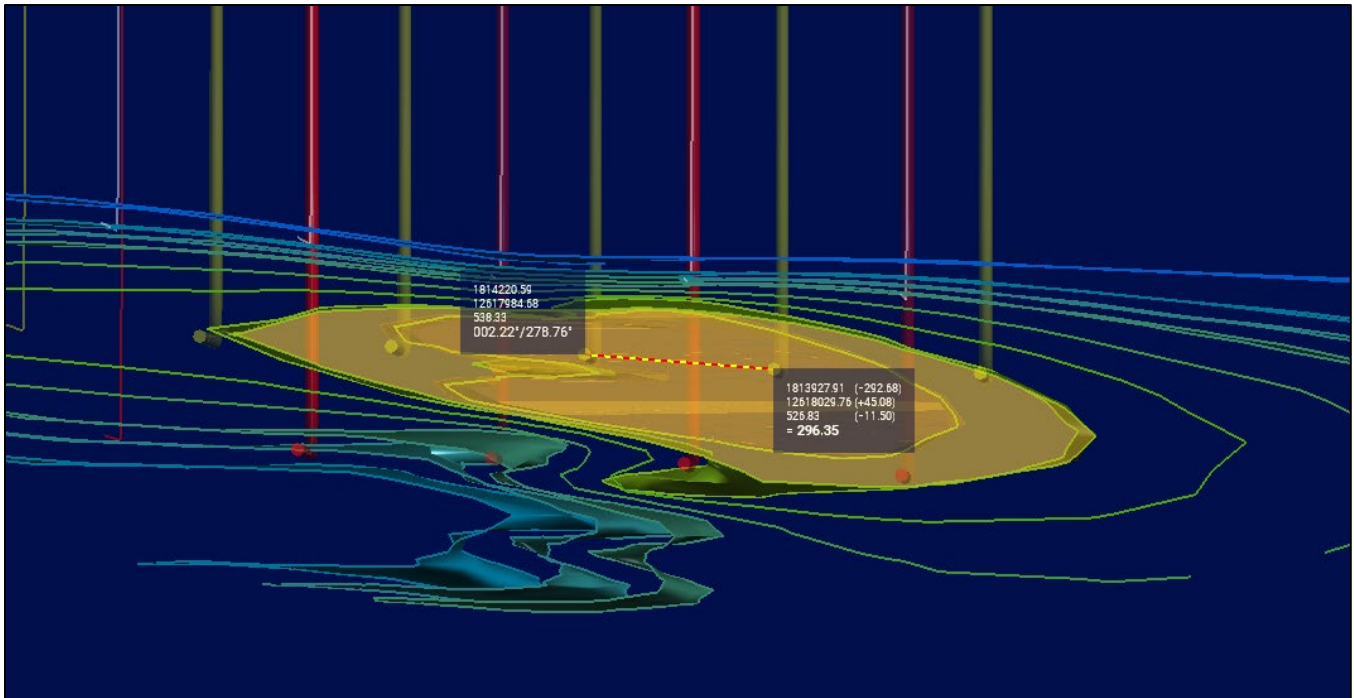


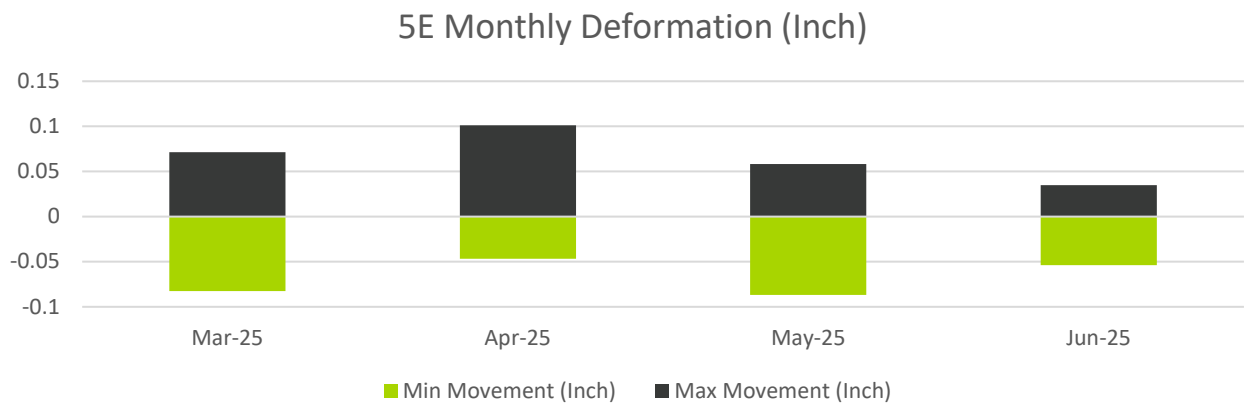
Figure 13.5: Block 2 mining cross section – MMH wells lateral spacing



Drilling and construction of the 27 wells for the LSBF wellfield requires a precision super single automated drilling rig operating by a 5-man crew with 24 hour per day and seven days a week (24/7) operations. Additional personnel require a dedicated tool-pusher and drill site manager on-site 24/7 while the rig deploys a rotary steerable directional drilling method. During the program, the commercial production wells will actively be adjusted or geo-steered based on logging during drilling operations.

Given the progressive nature of cavern development and injection fluid recharge and re-injection, cavern voids are expected to remain fluid-filled thus limiting subsidence risks at surface. Existing Micro-deformation instrumentation monitors the surface for subsidence and indicates cyclical net balance of subsidence and heave, and results are displayed in Figure 13.6 below. The injection interval is isolated to colemanite bearing orebody with overburden geological layers providing a bridge to reduce subsidence effects. Micro-deformation instrumentation will continue to monitor orebody throughout life of mine.

Figure 13.6: Micro-deformation results





## 14 Processing and Recovery Methods

This section outlines the processing facilities established in the final stage of the 2025 Prefeasibility Study for the Large-Scale Borate Facility Project (LSBF). It encompasses all processing operations, from the delivery of PLS from the mine wells to the production of boric acid and associated byproducts.

### 14.1 Processing Summary

During the Front-End Loading Phase 2 (FEL-2), 5E successfully executed an extensive program of mineral processing and metallurgical testing, as detailed in Section 10. Building on these results, the company has selected a proven, crystallization-based process for boric acid extraction. This method has been validated through both laboratory-scale experiments and the operational success of the SSF, illustrated in Figure 14.1.

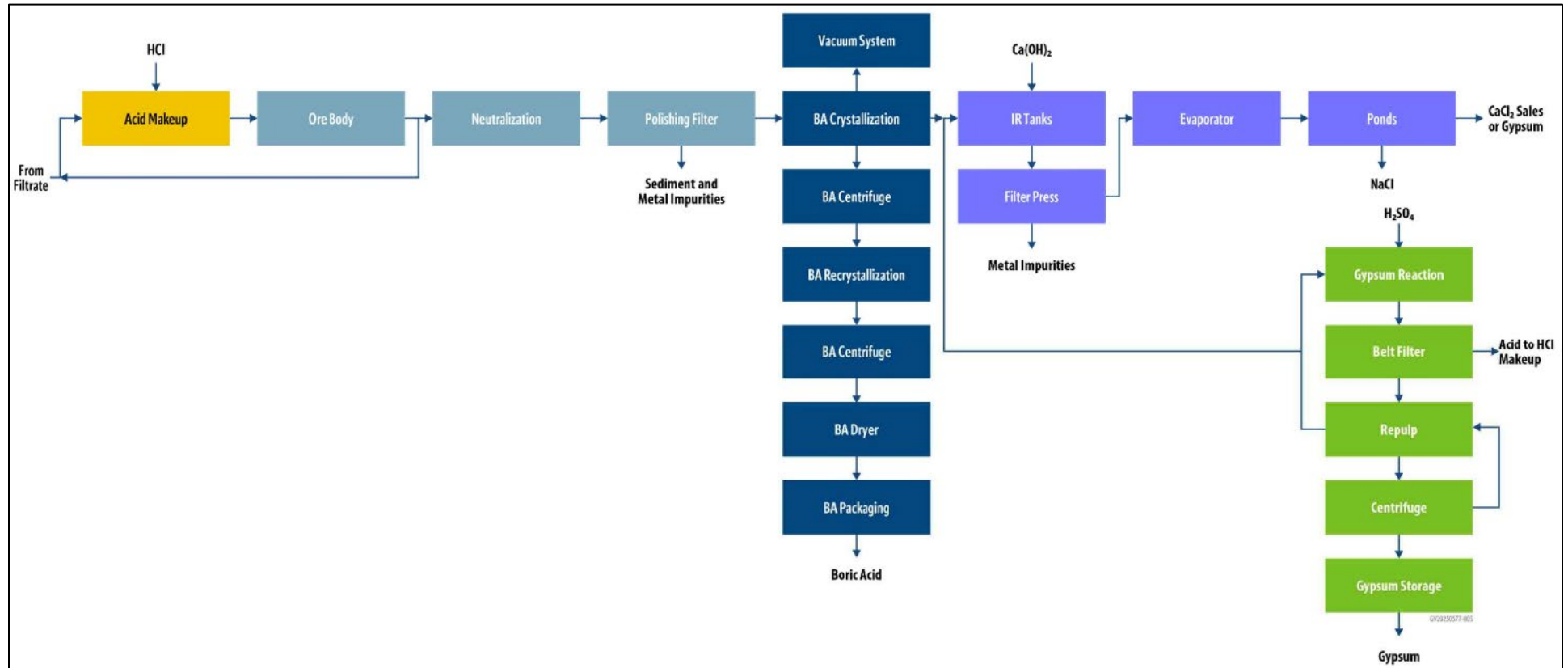
*Figure 14.1: Small-Scale Facility*



The SSF has consistently produced boric acid that meets or exceeds customer quality specifications. Operational insights, performance data, and key learnings from the SSBF have been integrated into the design of the forthcoming Large-Scale Borate Facility.

A high-level overview of the selected process, along with a simplified block flow diagram (Figure 14.2), is presented below. Additional technical details are available in Section 14.3 and the Process & Utility Description document (5EAM-G1-RPT-225-00003).

Figure 14.2: Block flow diagram of the Large-Scale Facility



- **Solution Mining and Injection:** Target minerals are dissolved in situ using solution mining techniques utilizing heat and steam. The resulting PLS is transported via pipeline infrastructure to the surface processing facilities.
- **PLS Recovery and Clarification:** The PLS undergoes pH adjustment through lime addition, which reduces acidity and enables the use of more cost-effective materials of construction. A multi-stage solid-liquid separation process, including filtration, removes precipitated solids, yielding a clarified solution ready for downstream processing.
- **Boric Acid Circuit:** This core section of the process is dedicated to the concentration, extraction, and purification of boric acid. A two-stage vacuum chilled crystallization system initiates the precipitation of boric acid, followed by filtration, washing, and redissolution. A second two-stage recrystallization step ensures high-purity product formation. Final dewatering is achieved via centrifugation, and the wet crystals are dried in a rotary dryer, cooled, and packaged. A portion of the centrate is directed to the Impurity Removal Circuit and the remainder is sent to the Gypsum circuit.
- **Impurity Removal Circuit and Evaporation:** In the Impurity Removal stage, magnesium hydroxide [Mg(OH)<sub>2</sub>] and other impurities are removed from the process stream through a reaction with hydrated lime. This reaction causes the impurities to precipitate, allowing them to be separated via filtration. The resulting filtrate slurry then enters the Evaporation Circuit, where mechanical evaporation and evaporation ponds concentrate solution. During this process, sodium chloride is precipitated and removed as waste. The concentrated brine, now enriched with calcium chloride, is either directed to truck loading for sale as a byproduct or sent to the Gypsum Circuit for further processing.
- **Gypsum Circuit:** Here, the Calcium Chloride rich brine reacts with sulfuric acid to precipitate gypsum, which is then filtered and refined to be sold as a byproduct. This circuit also facilitates the regeneration of hydrochloric acid, which is recycled back to the wellfield for reuse in the mining process.

## 14.2 Process Design Criteria / Usages

The LSBF's engineering and design framework is guided by the specifications detailed in the Process Design Criteria document (5EAM-G1-DBD-225-00001), with summary of the most critical process parameters, assumptions, and usages reflected in Table 14.1 below:

Table 14.1 LSBF design criteria

Parameter	Units	Design Criteria / Usages – Process Summary		
		Value (Gypsum only)	Value (CaCl <sub>2</sub> and Gypsum)	Comments
Feed Rate	st/hr	25.6	25.6	
Operating Days per Year	days/yr	365	365	
Operating Factor	%	91	91	
Plant Operating Hours	hr/yr	8,000	8,000	
Boron Recovery	%	95.1	95.1	
Boric Acid Production Rate	st/hr	16.25	16.25	
Boric Acid Design Production	stpy	130,000	130,000	
Gypsum Production	stpy	162,000	129,000	Dry Basis
Calcium Chloride Production	stpy	0	57,000	~57,000 @ 40% weight CaCl <sub>2</sub> solution, equivalent to 60,000 @38%
Water Consumption	gpm	237	237	Make up from wells
Hydrochloric Acid	lbs/st Boric Acid	291	510	100% basis
Sulfuric Acid	lbs/st Boric Acid	1,451	1,157	100% basis
Lime	lbs/st Boric Acid	423	423	100% basis
Natural Gas	MMBTU/st	7	7	
Electricity	kW/st	1,000	1,000	
Employees	people	110	110	80 operators and 30 overhead

### 14.2.1 Basis for Boric Acid (BA) Head Grade

As stated in Section 11.1 Key Assumptions, it is the opinion of the QP for Section 13 that 5E may achieve a boric acid head grade of 10.2% weight in the PLS at 160°F, with 12% head grade being the maximum potentially achieved at 212°F for PLS recovery. The drivers assume to achieve this rate are two-fold: (1) injectate solution can be heated above ground at a temperature above 200°F with PLS solution leaving the formation at 160°F, or (2) the formation can be heated via dedicated steam injection such that PLS solution exits the formation at 160°F. Other drivers that have been proven include: (1) recycled boron remains in solution during mining, (2) boron solubility curves follow calcium curves as demonstrated by work performed by MSME in the 1980's, and (3) 5E's extracted PLS aligns with the solubility curves versus temperature. See Kemetco solubility curve in Section 10.

### 14.3 Work Breakdown Structure and Plant Layout

To support the execution and management of the LSBF project, the processing facilities have been organized using a structure Work Breakdown Structure (WBS). This framework provides a clear, hierarchical representation of the project scope, enabling effective planning, coordination, and control throughout the project lifecycle. Table 14.2 presents the processing facilities by WBS, while the plant layout is illustrated in Figure 14.3 and Figure 14.4. This WBS divides the LSBF into five primary geographic areas, each representing a distinct portion of the processing infrastructure. Two additional areas are included for cost accounting purposes. During FEL-2, the project scope was defined to the Level 2 WBS, providing sufficient detail for pre-feasibility level planning and reporting. Further refinement to Levels 3 and 4 will be completed during FEL-3 and the detailed design phase.

This structured approach ensures that each component of the processing facilities is clearly defined and traceable, supporting efficient execution and alignment with overall project objectives.

Table 14.2 LSBF WBS processing facilities

FEL-2 (DEFINITION LVL)		FEL-3/EXECUTION	DESCRIPTION
AREA LEVEL 1	AREA LEVEL 2	AREA LEVEL 3	
PLANT AREA	UNIT TYPE	CWA – DRAFT	
"N"	"N#"	"N###"	
G	G100000		General
			GENERAL
S	S100000		Site and Infrastructure
			Site Preparation
		S101000	Site Preparation
		S102000	Mass Earthworks
		S103000	Site Drainage
		S104000	Sediment Handling
		S105000	Site Finish Grading
		S106000	Topsoil/Overburden Storage
	S200000		Plant Roads
		S201000	Plant Site Roads
		S202000	Parking
		S203000	Access Roads
B	B100000		Buildings/Ancillary Facilities
			Buildings
		B101000	Administration Buildings (by 5E)
		B102000	Guard House/Security Buildings/Gate House
		B103000	Truck Weigh Scale
		B104000	Central Control Room
		B105000	Warehouses
		B106000	Process Controls Lab
		B107000	Maintenance Building
P	P100000		Hydrometallurgical Processing Facility
			Solution Mining and Injection
		P101000	Mining Acid Make-up
	P200000	P102000	Reserved for Owner
			PLS Recovery and Clarification
		P201000	Mine FEED Storage and Return



FEL-2 (DEFINITION LVL)	FEL-3/EXECUTION	DESCRIPTION
	P202000	PLS Solid/Liquid Separation
	P203000	PLS Tailings Filtration
	P204000	Tailings Handling and Storage
<b>P300000</b>		<b>Boric Acid Circuit</b>
	P301000	Boric Acid Crystallization
	P302000	Boric Acid Filtration and Washing
	P303000	Boric Acid Recrystallization and Dissolution
	P304000	Boric Acid Drying
	P305000	Boric Acid Product Packing and Loadout System
	P306000	Boric Acid Building
	P307000	Brine Storage and Distribution
<b>P400000</b>		<b>Impurity Removal Circuit</b>
	P401000	Impurity Precipitation/Concentration
	P402000	Impurity Filtration
	P403000	Impurity Handling and Storage
<b>P500000</b>		<b>Evaporation Circuit</b>
	P501000	Brine Concentration
<b>P600000</b>		<b>Gypsum Circuit</b>
	P601000	Gypsum Precipitation/Concentration
	P602000	Gypsum Filtration
	P603000	Gypsum Refining
	P604000	Gypsum Drying
	P605000	Gypsum Product Packing and Truck Loadout System(s)
	P606000	Gypsum Plant Building
<b>P700000</b>		<b>Reagents</b>
	P701000	Lime System
	P702000	Hydrochloric Acid System
	P703000	Sulfuric Acid System
	P704000	Sodium Hydroxide System
	P705000	Miscellaneous Reagent Systems
<b>P800000</b>		<b>Evaporation Ponds</b>
<b>U</b>		<b>Utilities and Offsite (U&amp;O)</b>
<b>U100000</b>		<b>Plant Utilities (Above/Underground)</b>
	U100000	Utilities General
	U101000	Natural Gas
	U102000	Process Water Storage and Supply
	U103000	Gland Water Storage and Supply
	U104000	Potable Water Storage and Supply
	U105000	Reverse Osmosis Water Storage and Supply
	U106000	Firewater/Raw Water Storage and Supply
	U107000	Fire Protection System
	U108000	Cooling Water
	U109000	Chilled Water
	U110000	Demin Water
	U111000	Steam and Condensate Systems
	U112000	Storm Water System
	U113000	Compressed Air
	U114000	Instrument Air
	U115000	Lube Oil/Hydraulic
	U116000	Oily Water Treatment
	U117000	Environmental Monitoring
	U118000	Utility Shelters
	U119000	Sanitary Sewer
<b>U200000</b>		<b>Interconnecting Systems</b>
	U201000	Piperack
	U202000	Piperack (Placeholder)
	U203000	Piperack (Placeholder)
	U203000	Piperack Utilities
<b>U300000</b>		<b>Power Supply and Distribution</b>
	U301000	Plant Site Power Distribution
	U302000	Plant Site Grounding
	U303000	Main Sub-Station E-House
	U304000	E-House 1
	U305000	E-House 2
<b>U400000</b>		<b>Communications</b>

FEL-2 (DEFINITION LVL)	FEL-3/EXECUTION	DESCRIPTION
	U401000	Plant Control Systems
	U402000	Fire Detection System
	U403000	Security System
	U404000	Process Monitoring System (CCTV)
	U405000	Telephone System
	U406000	Fiber Optics/Networks
	U407000	Satellite Connection
	U408000	Radio Communication
U500000		Offsites
U600000		Cogen Facility

Figure 14.3: LSBF plant layout

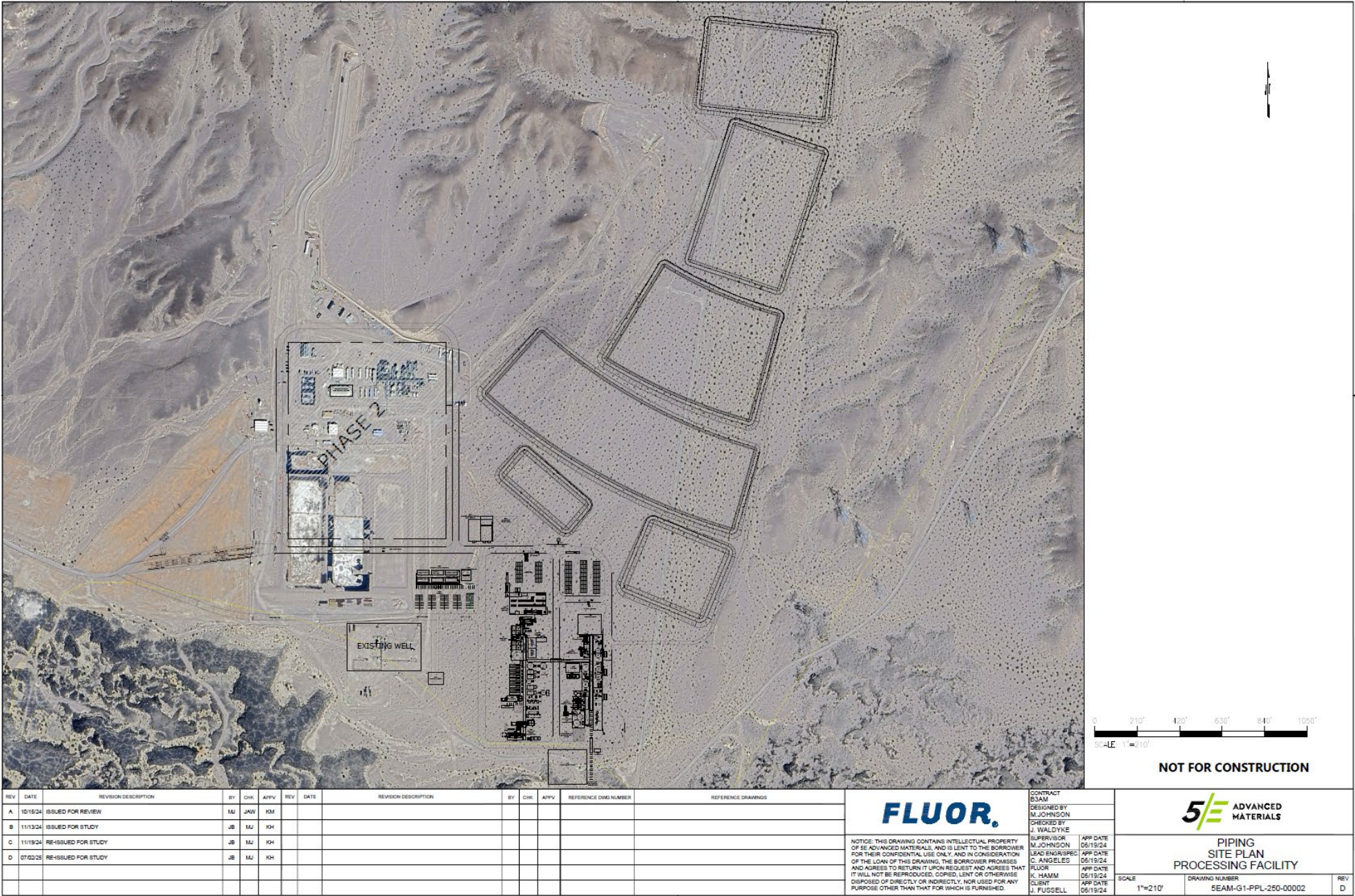
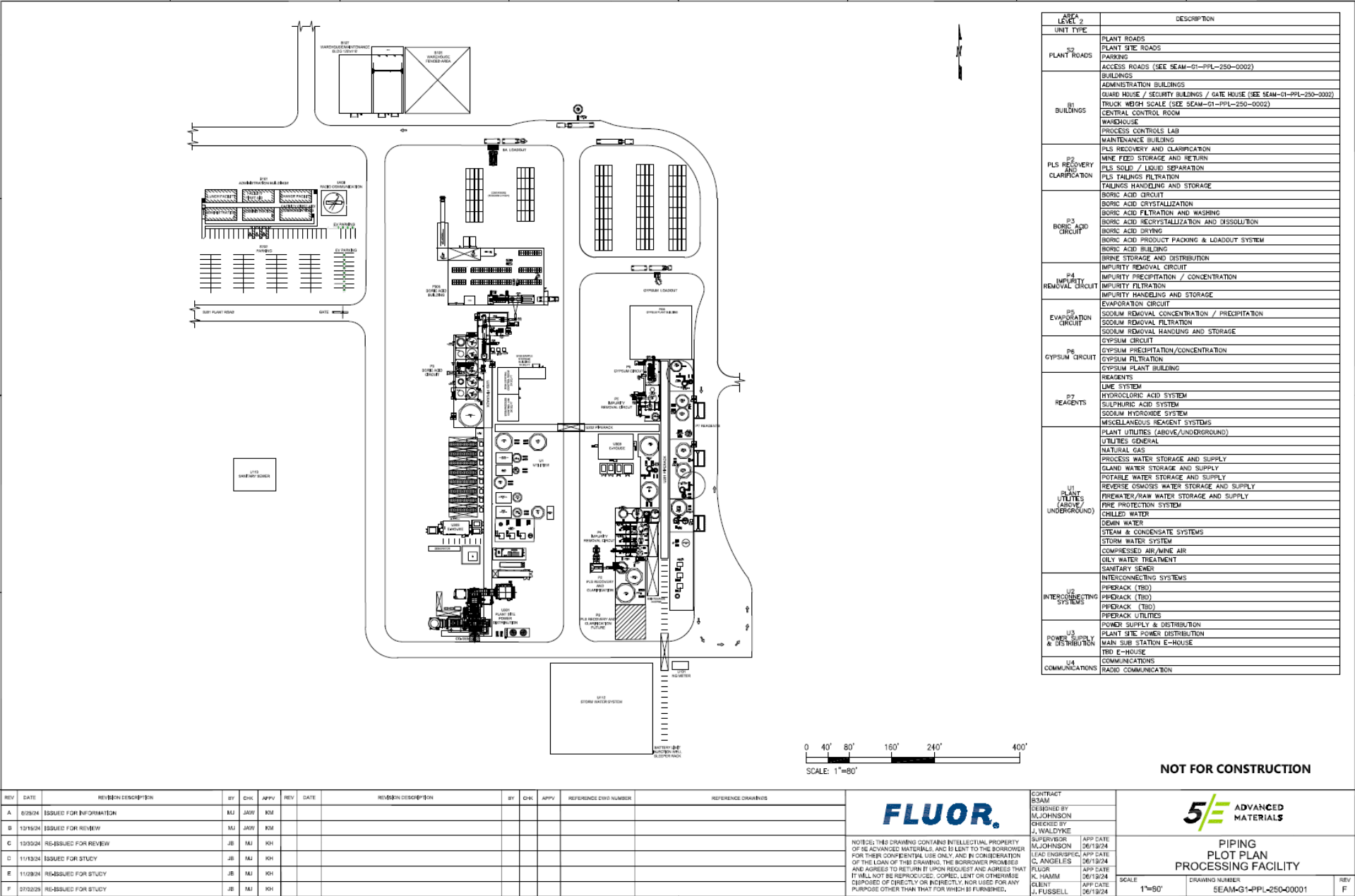




Figure 14.4: LSBF detailed layout



## 14.4 Description of Processing Facilities

The processing facility at the LSBF is engineered to support high-efficiency, high-throughput extraction and refinement of boric acid and associated byproducts from the PLS. This section provides a more detailed overview of each major processing area, highlighting the unit operations, equipment, and supporting systems that collectively enable the transformation of raw leached solution into finished, market-ready products. The design integrates industry best practices and leverages proven technologies validated through extensive test work and the successful operation of the SSF.

At the core of the LSBF is the Hydrometallurgical Processing Area, which encompasses all major processing functions. The following subsections describe this area. For a comprehensive breakdown of the facility scope, refer to the Scope of Facilities document 5EAM-G1-RPT-201-00003.

- **Solution Mining and Injection:** This unit area utilizes in-situ mining techniques to dissolve target minerals underground. The resulting PLS is then transferred for further processing via pipelines to the Hydrometallurgical Processing area.
- **PLS Recovery and Clarification:** In this unit, PLS undergoes a pH adjustment and a multi-stage solid-liquid separation process. Lime is added to increase the pH, reducing the solution's acidity before it enters the Crystallization Circuit. This adjustment allows for better material of construction selection for downstream equipment. Filtration units then remove the precipitated solids, resulting in clarified PLS for the next stages and dewatered tailings. Dedicated storage tanks (PLS Storage) ensure a constant flow of clarified PLS to subsequent stages.
- In addition to the above, this area contains the mine feed and regenerated acid return scope (i.e., storage and pipe headers).
- **Boric Acid Circuit:** This critical sub-area focuses on boric acid concentration, extraction, and purification and employs the following unit operations:
  - **Crystallization:** A two-stage vacuum cooled crystallization system is employed to precipitate the primary boric acid. This is followed by a filtration and washing operation using a belt filter. The boric acid crystals are then redissolved and recrystallized through another two-stage vacuum cooled crystallization system to achieve high-purity boric acid. The product is dewatered via centrifugation to a moisture content suitable for drying.
  - **Boric Acid Drying/Cooling:** Wet boric acid crystals from the filtering/washing centrifuge stage will undergo a rotary drying process to remove residual moisture. After the drying operation, the crystals will be cooled prior to being sent to the packaging and loadout system.
  - **Boric Acid Product Packing & Loadout System:** This system facilitates the packaging of dried boric acid crystals into appropriate containers for shipment and sale.
  - **Boric Acid Building:** This building encompasses the equipment and machinery required for the boric acid packaging and loadout area to remove risks of product contamination from external moisture, dust etc.
  - **Brine Storage and Distribution:** Concentrated brine from the boric acid extraction process is stored and distributed from this area.
- **Impurity Removal Circuit:** This circuit aims to precipitate and remove bulk impurities from the boric acid filtrate/centrate, which is disposed of as a waste material.
  - The circuit includes equipment to precipitate impurities through reagent addition. This process is carried out in two separate steps, each involving filtration equipment to separate the precipitated material from the solution. Impurities will be disposed of as waste via a manual handling process performed by 5E.

- **Evaporation Circuit:** This circuit focuses on further concentrating the received brine solution to reduce the evaporation pond area necessary to promote precipitation of sodium in the form of sodium chloride as a waste material.
  - **Brine concentration:** Includes an Evaporation system (i.e., Evaporator and Heat Exchangers) to concentrate the brine solution, thus minimizing the downstream evaporation pond area needed to precipitate and remove solid sodium chloride before proceeding to the Gypsum Circuit.
- **Evaporation Ponds:** Following the Evaporation Circuit, the brine stream undergoes further concentration through a dedicated evaporation pond system. This system comprises six sequential ponds designed to extract sodium chloride (NaCl) from a calcium chloride (CaCl<sub>2</sub>) rich brine. The process begins in Buffer-1, which manages seasonal fluctuations by storing brine during cooler months and releasing it during warmer periods. The brine then passes through four main evaporation ponds (P-2 to P-5), where water evaporates and NaCl precipitates. The final stage occurs in the reservoir pond, which holds the remaining brine and ensures a consistent, year-round feed to the downstream processing plant.

In total, the pond system spans approximately 37 acres, with around 33.5 acres actively engaged in brine processing. Once the brine is sufficiently concentrated, the resulting calcium chloride stream is directed either to the Gypsum Circuit for further treatment or to a truck load-out facility for sale as a byproduct.

- **Gypsum Circuit:** This section addresses two key objectives:
  - **Gypsum precipitation and removal:** Includes reaction equipment (CSTR) to precipitate gypsum by the addition of sulfuric acid, followed by filtration to produce gypsum cake. This crude gypsum cake will be further refined to a product via a repulp step and a centrifugation step. The final gypsum product is transported to storage for truck load out and shipping. Additionally, this process serves to regenerate HCl acid that will then be recycled back to the IR Wells.
- **Reagents:** This area contains the various reagent systems for storing, preparing, and supplying various chemicals required throughout the processing plant. Examples include:
  - Lime
  - Hydrochloric Acid
  - Sulfuric Acid
  - Sodium Hydroxide
  - Soda Ash
  - Miscellaneous Reagents as defined on the PFDs
- **Plant Utilities (Above/Underground):** This covers the design, installation, and operation of all utility systems within the plant boundaries, including both above ground and underground piping and infrastructure.
  - **Utilities General:** Overall planning and coordination of the various utility systems within the plant.
  - **Natural Gas:** Delivery, pressure regulation, and distribution of natural gas for use as fuel in boilers, dryers, or other process equipment.
  - **Process Water Storage and Supply:** Storage and distribution of treated water used in various process applications.
  - **Potable Water Storage and Supply:** Storage and distribution of treated potable water.
  - **Reverse Osmosis Water Storage and Supply:** Production, storage, and distribution of high-purity water through reverse osmosis for specific process needs.
  - **Firewater/Raw Water Storage and Supply:** Storage and distribution of water for fire protection systems and potentially raw water for treatment and use in other applications.
  - **Fire Protection System:** Installation of a fire protection system including fire hydrants, sprinklers, and alarms.
  - **Cooling Water:** Delivery, treatment, and distribution of cooling water used to regulate process temperatures in various equipment.

- Chilled Water: Production, storage, and distribution of chilled water for specific cooling requirements within the process.
- Demin Water: Production, storage, and distribution of demineralized water, which is high-purity water with minimal ionic content, for critical process applications.
- Steam & Condensate Systems: Generation, distribution, and recovery of steam for use in various process equipment including the wellfield, along with management of condensate (returned condensed steam).
- Compressed Air: Production, storage, and distribution of compressed air for use in various instruments, etc. (excludes air for mine wells).
- Sanitary Sewer: This section covers the collection and treatment of sanitary wastewater generated within the plant before discharge to a leach field.
- Interconnecting Systems:
  - This area is meant to capture major pipe rack systems which provide utilities to multiple process areas.
- Power Supply and Distribution:
  - Electrical Distribution: Installation of the main ring grounding system, electrical distribution system within the plant, including transformers, switchgear, and cabling to deliver power to various equipment.
- Communications: This includes the installation of communication and auxiliary systems supporting multiple areas of the facility. Systems include the following:
  - Plant Control Systems
  - Fire Detection System
  - Security System
  - Process Monitoring System (CCTV)
  - Telephone System
  - Fiber Optics and Networks
  - Satellite Connection
  - Radio Communication
- Offsites:
  - Offsite Utilities: By Others; Natural Gas header and tie-in to offsite gas supplier metering stations is included.
- Combined Heat and Power Plant (CHP) Facility
  - A modular system featuring a gas engine or turbine generator set, capable of generating approximately 20 MW of electricity. This system will support the processing facility's operations independently, without requiring integration with the electrical grid.
  - An integrated waste heat recovery system designed to efficiently capture and economically utilize the generated heat/energy in other areas of the process design.

## 14.5 Equipment Selection – Processing Facilities

The selection of equipment for the LSBF is directly informed by the process design and operational requirements established during the FEL-2 phase. Each piece of equipment has been chosen to ensure reliable performance, alignment with throughput targets, and compatibility with the crystallization-based boric acid recovery process.

In addition to process suitability, the selection criteria emphasized:

- Safety
- Low capital cost
- Reliability



- Proven history of operation in similar applications
- Readily available spare parts
- Standardization of components to minimize inventory

Table 14.3 below summarizes the major plant equipment selections for the processing facilities that form the basis of the capital cost estimate. An all-inclusive list of equipment can be viewed in the plant mechanical equipment list (Mechanical Equipment List 5EAM-G1-EQL-255-00001). Details on equipment purchasing are provided in Project Execution Strategy 5EAM-G1-PEP-100-00001.

Table 14.3 Major Plant Equipment Selections

MAJOR EQUIPMENT SUMMARY – PROCESSING FACILITIES		
EQUIPMENT TAG	EQUIPMENT TYPE	EQUIPMENT DESCRIPTION
P2-TNK-201	TANK	PREGNANT LEACH SOLUTION HOLDING TANK
P2-SBR-202	SCRUBBER	HCL MAKE-UP TANK SCRUBBER
P2-TNK-202	TANK	HCL MAKE-UP TANK
P2-VPK-202	PACKAGE	HCL MAKE-UP TANK SCRUBBER PACKAGE
P2-TNK-205	TANK	PLS PH ADJUSTMENT TANK
P2-TNK-206	TANK	PLS FILTER PRESS FEED TANK
P2-FIP-201	FILTER PRESS	PLS FILTER PRESS
P2-FIL-201	FILTER	PLS POLISHING FILTER
P2-TNK-208	TANK	PLS FILTER PRESS WASH WATER TANK
P2-TNK-207	TANK	PLS FILTRATE TANK
P2-CRN-001	CRANE	FILTER PRESS CRANE
P3-TNK-301	TANK	BA CRYSTALLIZER FEED TANK
P3-VPK-301	PACKAGE	BORIC ACID CRYSTALLIZER PACKAGE
P3-CRZ-301	CRYSTALLIZER	1ST STAGE BA CRYSTALLIZER
P3-CRZ-302	CRYSTALLIZER	2ND STAGE BA CRYSTALLIZER
P3-HEX-301-A	CONDENSER	BA CRYSTALLIZER VENT CONDENSER 1
P3-HEX-302-A	HEAT EXCHANGER	INTER CONDENSER 1
P3-HEX-303-A	HEAT EXCHANGER	AFTER CONDENSER 1
P3-EJR-301-A	EJECTOR	FIRST VACUUM EJECTOR 1
P3-EJR-302-A	EJECTOR	SECOND VACUUM EJECTOR 1
P3-HEX-304	CONDENSER	BA CRYSTALLIZER VENT CONDENSER 2
P3-HEX-305	HEAT EXCHANGER	INTER CONDENSER 2
P3-HEX-306	HEAT EXCHANGER	AFTER CONDENSER 2
P3-EJR-303	EJECTOR	FIRST VACUUM EJECTOR 2
P3-EJR-304	EJECTOR	SECOND VACUUM EJECTOR 2
P3-TNK-302	TANK	BA CRYSTALLIZER HOTWELL
P3-VPK-302	PACKAGE	BA BELT FILTER VENDOR PACKAGE
P3-FIB-301	BELT FILTER	BA BELT FILTER
P3-TNK-303	TANK	BA DISSOLUTION TANK
P3-HEX-307	HEAT EXCHANGER	BA DISSOLUTION TANK HEAT EXCHANGER
P3-FIL-301	FILTER PRESS	CALCIUM SULFATE FILTER
P3-CRZ-303	CRYSTALLIZER	1ST STAGE BA RECRYSTALLIZER
P3-CRZ-304	CRYSTALLIZER	2ND STAGE BA RECRYSTALLIZER
P3-HEX-308	CONDENSER	BA RECRYSTALLIZER VENT CONDENSER STAGE 1
P3-HEX-309	CONDENSER	RECRYSTALLIZER INTER CONDENSER STAGE 1
P3-HEX-310	CONDENSER	RECRYSTALLIZER AFTER CONDENSER STAGE 1
P3-EJR-305	EJECTOR	RECRYSTALLIZER FIRST VACUUM EJECTOR STAGE 1
P3-EJR-306	EJECTOR	RECRYSTALLIZER SECOND VACUUM EJECTOR STAGE 1
P3-HEX-311	CONDENSER	BA RECRYSTALLIZER VENT CONDENSER STAGE 1
P3-HEX-312	CONDENSER	RECRYSTALLIZER INTER CONDENSER STAGE 1

MAJOR EQUIPMENT SUMMARY – PROCESSING FACILITIES		
EQUIPMENT TAG	EQUIPMENT TYPE	EQUIPMENT DESCRIPTION
P3-HEX-313	CONDENSER	RECRYSTALLIZER AFTER CONDENSER STAGE 1
P3-EJR-307	EJECTOR	RECRYSTALLIZER FIRST VACUUM EJECTOR STAGE 1
P3-EJR-308	EJECTOR	RECRYSTALLIZER SECOND VACUUM EJECTOR STAGE 1
P3-TNK-304	TANK	BA RECRYSTALLIZER HOTWELL
P3-CTF-301	CENTRIFUGE	BA CENTRIFUGE
P3-TNK-305	TANK	BA CENTRIFUGE FEED TANK
P3-TNK-306	TANK	BA CENTRATE TANK
P3-BLO-301	BLOWER	BA DRYER COMBUSTION AIR BLOWER
P3-BLO-302	BLOWER	BA DRYER AIR BLOWER
P3-BLO-303	BLOWER	BA COOLER AIR BLOWER
P3-BRN-301	BURNER	BA DRYER BURNER
P3-CLR-301	COOLER	BA COOLER
P3-HET-301	HEATER	BA AIR HEATER
P3-DRY-301	DRYER	BA DRYER
P3-HEX-314	COOLER	BA COOLER AIR COOLER
P3-CYC-301	CYCLONE	BA CYCLONE 1
P3-CYC-302	CYCLONE	BA CYCLONE 2
P3-VPK-303	PACKAGE	BA DRYER SCRUBBER PACKAGE
P3-SBR-301	SCRUBBER	BA SCRUBBER
P3-BUE-301	BUCKET ELEVATOR	BA PRODUCT BUCKET ELEVATOR
P3-DCO-301	DUST COLLECTOR	BA SILO DUST COLLECTOR
P3-SLO-301	SILO	BA PRODUCT STORAGE SILO
P3-VPK-304	BAGGING SYSTEM	BA PRODUCT BAGGING SYSTEM
P3-TNK-308	TANK	BRINE HOLDING TANK
P4-TNK-402	TANK	NEUTRALIZATION TANK
P4-THK-401	THICKENER	IMPURITY REMOVAL THICKENER
P4-TNK-403	TANK	IMPURITY REMOVAL THICKENER OVERFLOW TANK
P4-TNK-404	TANK	IMPURITY REMOVAL FILTER FEED TANK
P4-FIP-401	FILTER PRESS	IMPURITY REMOVAL FILTER PRESS
P4-TNK-405	TANK	IMPURITY REMOVAL FILTER CLOTH WASH TANK
P4-TNK-406	TANK	MAGNESIUM REMOVAL TANK
P4-FIP-402	FILTER PRESS	MAGNESIUM REMOVAL FILTER PRESS
P4-TNK-407	TANK	MAGNESIUM REMOVAL FILTER CLOTH WASH TANK
P4-TNK-408	TANK	MAGNESIUM REMOVAL FILTRATE TANK
P5-TNK-501	TANK	EVAPORATOR FEED TANK
P5-EVP-501	EVAPORATOR	EVAPORATOR
P5-EJR-501	EJECTOR	EVAPORATOR STEAM EJECTOR 1
P5-EJR-502	EJECTOR	EVAPORATOR STEAM EJECTOR 2
P5-HEX-501	HEAT EXCHANGER	EVAPORATOR PRE-HEATER
P5-HEX-502	HEAT EXCHANGER	EVAPORATOR HEATER
P5-FIL-501	FILTER	EVAPORATOR POLISHING FILTER
P6-TNK-601	TANK	GYPSUM PRECIPITATION TANK
P6-VPK-601	PACKAGE	GYPSUM VENT SCRUBBER PACKAGE
P6-SBR-601	SCRUBBER	GYPSUM VENT SCRUBBER
P6-CTF-601	CENTRIFUGE	GYPSUM CENTRIFUGE
P6-FIB-601	BELT FILTER	GYPSUM BELT FILTER
P6-VPK-602	PACKAGE	GYPSUM BELT FILTER PACKAGE
P6-TNK-603	TANK	GYPSUM CENTRIFUGE FEED TANK
P6-TNK-604	TANK	GYPSUM CENTRATE TANK
P6-TNK-606-A/B	TANK	CALCIUM CHLORIDE TANK A/B

MAJOR EQUIPMENT SUMMARY – PROCESSING FACILITIES		
EQUIPMENT TAG	EQUIPMENT TYPE	EQUIPMENT DESCRIPTION
P7-BLO-701	BLOWER	LIME BULK UNLOADING BLOWER
P7-SLO-701	SILO	LIME SILO
P7-TNK-701	TANK	LIME MIXING TANK
P7-TNK-702	TANK	LIME STORAGE TANK
P7-TNK-703-A/B	TANK	HYDROCHLORIC ACID STORAGE TANK A/B
P7-TNK-704-A	TANK	SULFURIC ACID STORAGE TANK A
P7-TNK-704-B	TANK	SULFURIC ACID STORAGE TANK B
P7-TNK-705	TANK	SODIUM HYDROXIDE STORAGE TANK
U1-MSC-101	SKID	NATURAL GAS METERING SKID
U1-FIL-101	FILTER	RO 1 POLISHING FILTER
U1-ROS-101	REVERSE OSMOSIS	REVERSE OSMOSIS NO. 1
U1-TNK-103	TANK	RAW WATER TANK
U1-TNK-104	TANK	TREATED WATER TANK
U1-TNK-105	TANK	RO 1 FEED TANK
U1-VPK-101	PACKAGE	RAW WATER TREATMENT PACKAGE
U1-VPK-102	PACKAGE	REVERSE OSMOSIS NO. 1 PACKAGE
U1-TNK-106	TANK	RO WATER TANK
U1-FIL-106	FILTER	GLAND SEAL WATER FILTER
U1-TNK-109	TANK	PROCESS WATER TANK
U1-TNK-111	TANK	POTABLE WATER TANK
U1-VPK-104	PACKAGE	POTABLE WATER TREATMENT PACKAGE
U1-TNK-112	TANK	FIRE WATER TANK
U1-VPK-105	PACKAGE	BOILER SYSTEM PACKAGE
U1-TNK-113	TANK	CHILLED WATER EXPANSION TANK
U1-VPK-106	PACKAGE	CHILLED WATER PACKAGE
U1-FIL-103	FILTER	WATER RECOVERY RO POLISHING FILTER
U1-ROS-103	REVERSE OSMOSIS	WATER RECOVERY REVERSE OSMOSIS
U1-TNK-114	TANK	WATER RECOVERY TANK
U1-VPK-107	PACKAGE	WATER RECOVERY RO PACKAGE
U1-ACO-101-A/B/C	COMPRESSOR	PLANT AIR COMPRESSOR
U1-DRY-101	DRYER	PLANT AIR DRYER
U1-FIL-104-A/B	FILTER	PLANT AIR PRE-DRYER FILTERS
U1-FIL-105-A/B	FILTER	PLANT AIR POST-DRYER FILTER
U1-VPK-108	PACKAGE	AIR COMPRESSOR PACKAGE
U1-VSL-101	RECEIVER	PLANT AIR RECEIVER
U1-VSL-102	RECEIVER	INSTRUMENT AIR RECEIVER
B1-CRN-101	CRANE	MAINTENANCE SHOP CRANE

## 15 Infrastructure

### 15.1 Access and Local Communities

The Project is located near Interstate-40 along with nearby access to rail and a natural gas transmission line. Currently, the Project receives electrical power from a 12kV powerline and the SSF operates off this power. Figure 15.1 shows general infrastructure needs for the Project.

**APPROVED FACILITIES AND  
PLANNED OPERATIONS**

Los Angeles Public Works Department  
City of Los Angeles, California

## 15.2 Site Facilities and Infrastructure

The infrastructure required for the Project is expected to consist of the following:

- Natural gas – 5E will require a natural gas pipeline that will need to be tied into a nearby transmission pipeline to serve the processing plant. Discussions are ongoing with a proposal received from Kinder Morgan and the cost of piping from the Mojave Pipeline to a cogeneration facility (COGEN) included in the CAPEX estimate.
- Electrical power upgrade– an economic trade-off study is currently being conducted to evaluate co-generation versus an upgraded and dedicated powerline to the Project.
- Rail – connection to a rail spur adjacent to our EIS boundary is being considered for rail loading and the BLM Plan of Operations includes a permitted rail spur. In conjunction, a truck-to-rail transloading operation is being evaluated at another, existing rail spur location located 15 miles from the Project, which may be implemented as part of Phase II expansion.
- Roads – Plant access roads will require upgrades, and some roads may require paving. New access roads are also being considered. 5E has a pending application with the Bureau of Land Management’s Barstow office for two right-of-way applications for the east and west side of the property. Both right-of-way applications are expected to be granted and have National Environmental Policy Act exclusions.
- Water – 5E currently has adequate water resources for Phase 1 of the project with two existing water wells. Wells and pipelines will need to be expanded to accommodate later phases and expansion. The well southwest of the property is included in the permitted Plan of Operations. The well northeast of the property is not yet included in the Plan of Operations. 5E has secured millsite claims for each well.
- Material storage – storage for materials products and consumables will need to be built near the plant site including a stacking system for gypsum. Off-site storage and distribution are being explored with potential partners.

## 15.3 Security

The Project currently has 24-hour security service and camera surveillance for critical areas and areas with high-traffic, with gates at entrances to the Project area. 5E is considering constructing a fence around the property.

## 15.4 Communications

The Project currently utilizes a satellite-based internet service, which is fully functional. For larger operations, 5E has considered a dedicated fiber line to site or a dedicated cell tower amongst other potential options. Additionally, a strong cell phone signal is available.

## 15.5 Logistics Requirements and Off-site Infrastructure

### 15.5.1 Rail

Rail is not currently used by the Project; however, the BNSF rail is situated next to the Project and is being assessed for logistical requirements. Several transloading and rail service providers have also been contacted for potential off-site loading to rail transport.

### 15.5.2 Port and Logistics

The Port of Los Angeles, Long Beach, and San Diego are all within a half-day drive from the Project on major highways. 5E has a truck scale on-site that can weigh deliveries to and from ports or rail.

### 15.5.3 Off-site storage and distribution

Storage and distribution locations off-site are being explored, and discussions have been initiated with several potential providers.

## 16 Market Studies and Contracts

This section was completed with reference to a preliminary market study performed by Kline and Company, Inc. titled Boric Acid, Calcium Chloride, Gypsum Market Studies and Pricing Models dated June 19, 2025. 5E incorporated information obtained through consultation with industry experts, discussions with current end-use customers, and other publicly available sources to complete this section.

### 16.1 General Market Overview

Initially, 5E recognizes two primary minerals mined through ISL at the Project : borate and calcium. 5E will produce boric acid from its borate mineral and either calcium chloride or gypsum from the calcium mineral. Additional byproducts can be produced from other minerals and elements included with metals salts (i.e., lithium and magnesium); however, additional testing, analysis and research will need to occur to finalize a process before these minerals can be included in economic analysis.

### 16.2 Borates

#### 16.2.1 Market Overview

Based on the preliminary market study, global boric acid demand was estimated at approximately 1,137k metric tonnes per year in 2024 and is projected to grow at a compounded annual growth rate (CAGR) of 5.5%, reaching 1,834k metric tonnes per year by 2033.

The growth is driven by both traditional and emerging sectors, with applications spanning E-glass, textile fiberglass, specialty borosilicate glass, fertilizers, ceramics, and detergents, as well as high-value uses such as permanent magnets, semiconductors, nuclear energy, and advanced defense materials. Currently, glass applications account for 21% of total demand, non-glass applications for 40%, and the remaining 39% is attributed to specialty borates. The boron market is a global oligopoly where two companies dominate approximately 85% of global supply. Specific to boric acid, there are approximately 13 global suppliers; however, the market remains dominated by the two largest suppliers.

#### 16.2.2 Historical Pricing

The global boric acid market has historically demonstrated stable prices with periods of relatively low volatility. Between 2010 and 2024, prices averaged \$789 per short ton F.O.B. with the material driver to prices being supply and demand. Figure 16.1 provides the historical and forecasted supply and demand. and Figure 16.2 provides the historical pricing and forecasted pricing.

There are two historical periods where pricing significantly increased relative to historical averages, and both are driven by tightness in supply and demand. In 2010 and 2011, a labor dispute caused a plant shutdown at one of the larger producers which caused a supply constraint such that demand exceeded supply. This led to a period where pricing increased to \$1,229 per short ton in Q4 2011. In 2020, the world experienced the COVID-19 pandemic. During the COVID-19 pandemic, demand dissipated causing pricing to drop to as low as \$470 per short ton in Q2 2020. Once the pandemic ended, demand surged such that supply capacity could not keep pace with demand. This led to the second period where pricing significantly increased to \$1,213 per short ton in Q2 2022. Although there has been a small decline since the COVID-19 pandemic, increases in demand have led to prices remaining elevated relative to long term historical averages. At the end of 2024, boric acid prices stabilized around \$1,000 per short ton.



Figure 16.1: Project market capacity versus demand

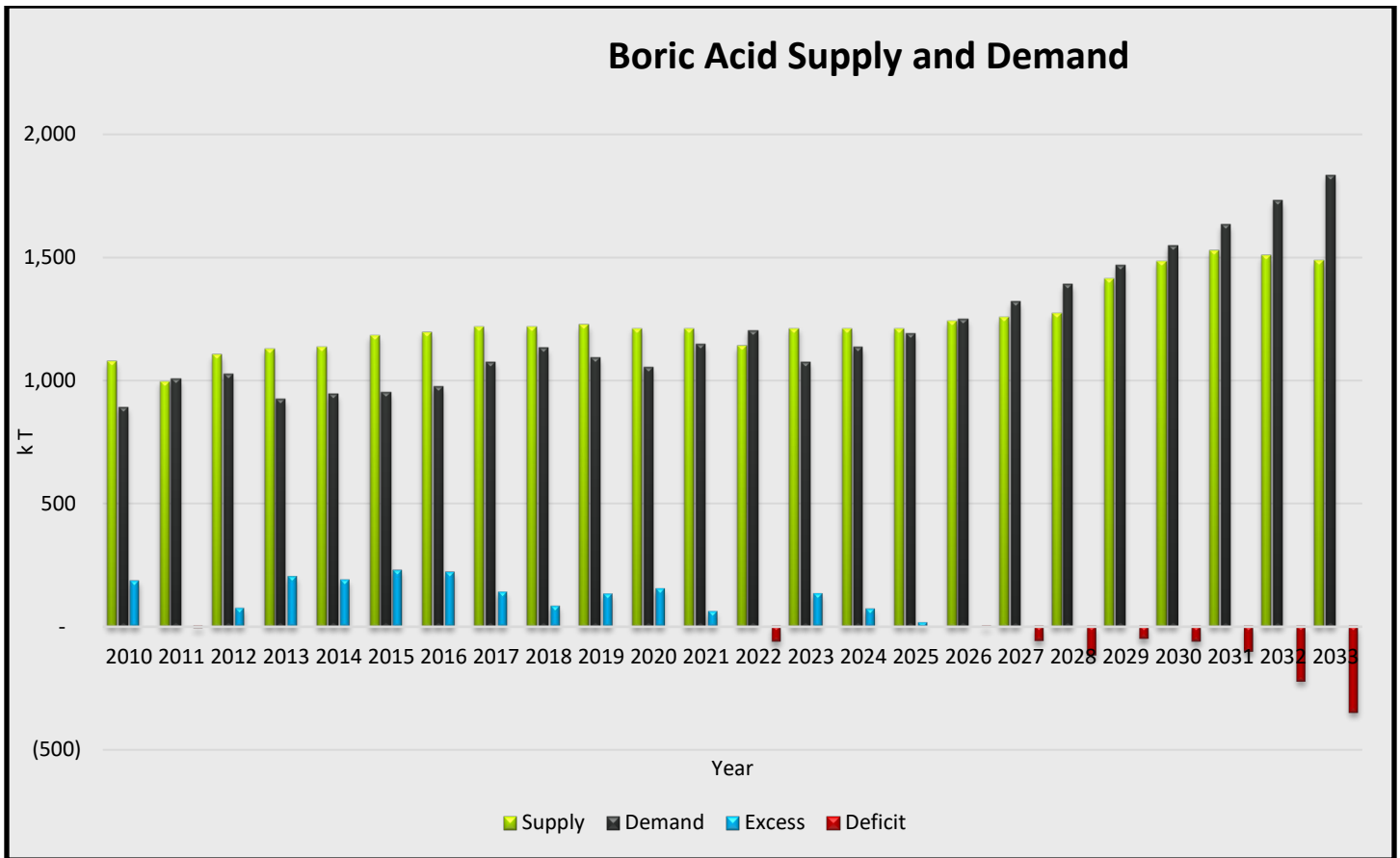
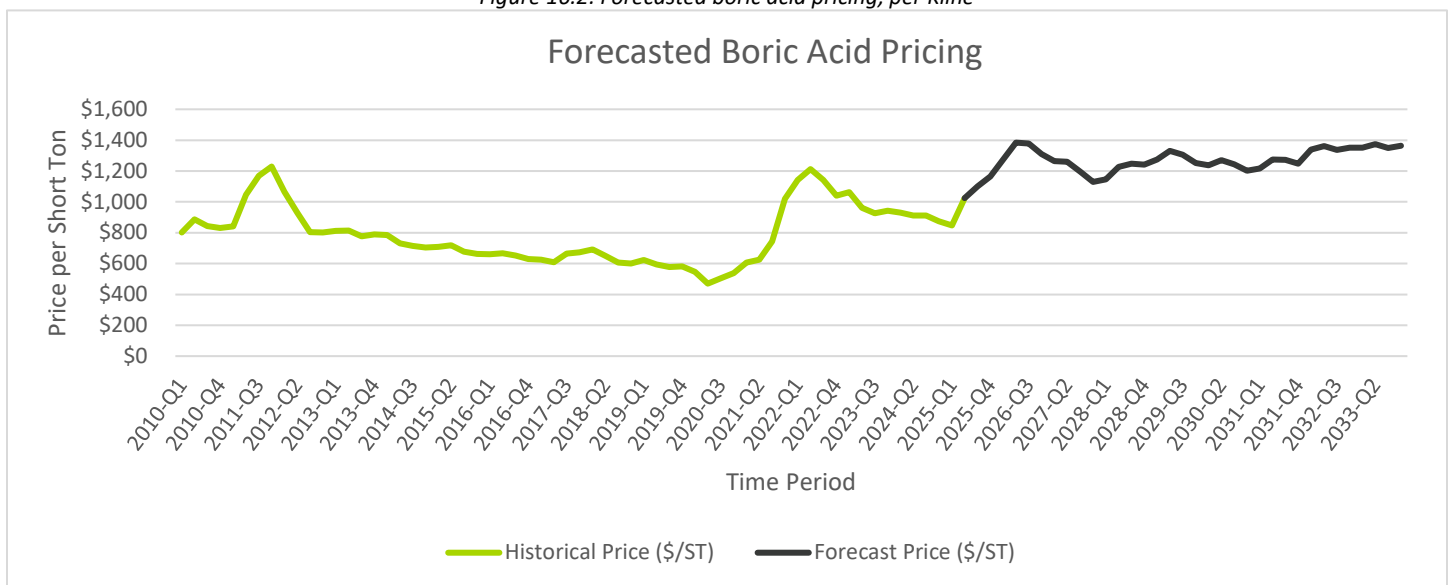


Figure 16.2: Forecasted boric acid pricing, per Kline



Boric acid is commercially available in two primary grades: granular and powder. Granular technical grade is the most traded form and serves as the standard product for large industrial customers. Powder grade, typically a byproduct of the screening process, is more variable in quality and availability and is required for high-specification applications such as pharmaceuticals or electronics.

Pricing is also influenced by packaging format. While bulk shipments offer the lowest-cost logistics solution, producers typically charge a \$25 – 50 per short ton premium for smaller pack sizes, such as 50 lb. bags, to account for handling and



purchasing in smaller quantities. Despite these differences, the underlying production costs for both grades and pack sizes are similar, indicating that pricing differentials are driven more by market dynamics and buyer preferences than by cost structure.

### 16.2.3 Market Balance

Over the period of 2010 through 2021, supply was sufficient to meet demand. Since 2021, global boric acid demand has steadily outpaced, with the imbalance expected to widen further through the end of the decade. Estimates project boric acid demand to grow from 1,137k metric tonnes in 2024 to 1,834k metric tonnes per year by 2033, driven by strong momentum in specialty glass, agriculture, EVs, and specialty applications. In contrast, supply is forecast to grow at a slower pace relative to demand, increasing from 1,242k metric tonnes in 2024 to 1,488k metric tonnes per year by 2033, resulting in a cumulative market shortfall that begins in 2025 and reaches approximately 346k metric tonnes by 2033.

On the supply side, growth remains limited due to the industry's high consolidation, with most of the production concentrated among Rio Tinto in the U.S. and Eti Maden in Turkey. Most other global producers operate at smaller scales or focus on lower-grade borates. While Eti Maden has confirmed a capacity expansion of 60k metric tonnes per year by 2027, no other major new supply is expected in the next 3 – 4 years. Several announced projects face delays or uncertainty. Additionally, China's opportunistic capacity has shifted toward domestic consumption and is often constrained by quality limitations.

Given the limited pipeline of new capacity and rising demand from sectors such as EVs, permanent magnets, and high-end agriculture, the boric acid market is expected to remain imbalanced. This tight supply outlook is likely to support continued pricing strength and enhance the commercial case for new entrants capable of delivering high-purity, reliable supply to strategic regions such as the U.S. and Asia.

The supply-side analysis in Figure 16.1 presumes moderate expansion at existing suppliers, 5E's anticipated supply per schedule in late 2028, and one additional major boric acid supplier entering the market per their publicly stated timeline. Demand-side analysis was built based on bottom-up analysis of expected and/or published end market expansion, moderated with the end market value in use as price pressures build on lower value applications. With existing market tightness, tailwinds for pricing exist as customers seek new supply sources outside of the existing oligopolistic market.

The analysis of the substitutability of boric acid in end uses concluded that most large volume applications have low or no risk of substitutability. Specifically, boric acid provides unique functionality in applications such as specialty glass, boron steel, and permanent magnets that have limited, and in many cases, higher cost alternatives such as rare earth elements, or would require significant investment to reformulate. Additionally, concerns for moderately substitutable applications have been identified as primarily other borate containing molecules (i.e., colemanite mineral), however, most market participants who can producer end products with a concentrate such as colemanite have already switched versus the boric acid alternative.

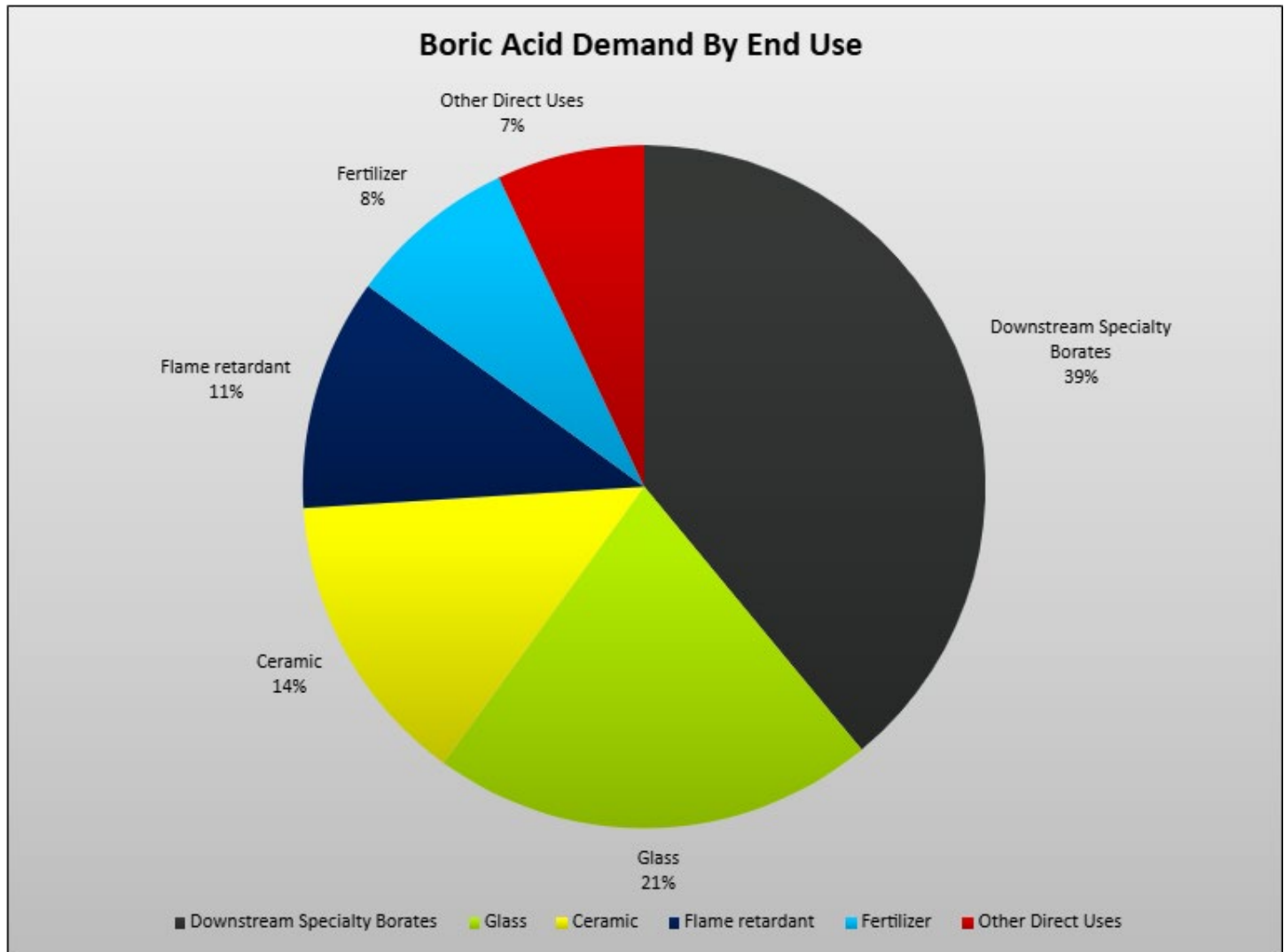
### 16.2.4 Market Costs

Estimating the operating unit cost of boric acid production is challenging due to limited public disclosures. One major supplier, being state-owned, does not report production costs separately, while another producer groups all borate-related products under a broader minerals category in its annual filings, complicating the isolation of boric acid costs. Recent company reports indicate that overall borate production costs are increasing due to input cost inflation, higher third-party expenses, and operational pressures. Although some inflationary effects have begun to stabilize, one of the larger producers faces margin pressure, incurred a reserve downgrade in 2018, and have implemented active cost-control measures with its board reportedly pushing for stronger operational discipline. 5E expected costs are given in Section 18.2.

### 16.2.5 Boric Acid Market

Boric acid is essential in diverse industries, catering to both commodity and specialty markets. Customers include large-scale users in glass and agriculture as well as smaller buyers purchasing through distributors. In high-value applications like specialty glass, flame retardants, and boron derivatives, performance outweighs price. Substitution is uncommon due to boric acid's reliable boron content and superior downstream performance compared to boron ores like colemanite or ulexite. Figure 16.3 provides an overview of boric acid demand by end use.

Figure 16.3: Boric Acid Demand by End Use, per Kline



Logistics and customer proximity dictate packaging and shipment formats for boric acid, usually provided in 25-kg bags, one-ton bags, or bulk containers which are transported by truck, rail, or ocean freight. Asia remains the leading sales region due to proximity and demand, but interest is rising in North America and Europe. This along with supply chain security efforts drives demand for high-purity boric acid from nations of reliable jurisdictions. In some areas, reliance on a single supplier prompts buyers to seek diverse and dependable sources.

Geopolitical concerns and consistent quality needs are likely to lead some buyers to pay a scarcity premium for reliable boric acid supply. Governments, especially in the U.S. and European Union, are encouraging domestic production of critical and strategic materials, boosting interest in new market entrants.

The market's opacity, reliance on negotiated contracts, and duopolistic nature mean there is no standard index price for boric acid. Pricing is highly influenced by demand, purity requirements, and capacity utilization. Kline's latest model

predicts Chinese boric acid prices will increase to about \$1,364 per short ton by 2030, driven by ongoing supply constraints and rising demand from high-specification sectors. Figure 16.2 provides forecasted boric acid pricing.

### 16.2.6 Boric Acid Specifications

Boric acid expected technical grade specifications are as follows:

- Chemical Specification:
  - o Analyte Guarantee
  - o  $B_2O_3\%$ : 56.25 – 56.5
  - o Equivalent  $H_3BO_3\%$ : 99.9 – 100.9
  - o  $SO_4$  ppm:  $\leq 250$
  - o Cl ppm:  $\leq 10$
  - o Fe ppm:  $\leq 5$
- Sieve Specification
  - o U.S. Sieve Mesh Size mm % Retained Guarantee
  - o No. 20, 0.850 mm  $\leq 2.0\%$

## 16.3 Calcium Chloride

### 16.3.1 Market Overview

Calcium chloride ( $CaCl_2$ ) is a versatile chemical compound widely used in various industries due to its hygroscopic properties and ability to lower the freezing point of water. It is commonly employed in de-icing and dust control applications, where it effectively melts ice and suppresses dust on roads and construction sites. In the oil and gas industry, it is used to increase fluid densities and control swelling. The compound is produced through several methods, both naturally from brine purification and synthetically via the Solvay process, where it is a byproduct of soda ash manufacturing, and by reacting hydrochloric acid with limestone.

The global calcium chloride market was estimated to be 3,825k metric tonnes in 2024, having seen higher-than-normal growth from the previous year of 1.5%. North America represents approximately 40% of global demand, followed by Asia, Europe, the Middle East and Africa, and South America. U.S. demand in 2024 was 1,050k metric tonnes, with growth expectations of 0.6% CAGR until 2034.

### 16.3.2 Historical Pricing

Calcium chloride pricing has nearly doubled since 2007, when average prices in the U.S. were \$267 per metric tonne, reaching \$500 in early 2025. The two biggest year-over-year increases during that time were between 2008 and 2009 and 2021 and 2022. The U.S. market has some of the highest average prices seen globally, driven by recent demand for winter road treatment and a supply deficit due to plant closures during the twenty-first century. The U.S. is thus a net importer of calcium chloride, with Mexico, China, Canada, Europe, and the Middle East as the main sources in recent years.

### 16.3.3 Market Balance

The U.S. calcium chloride market is dominated by two large public companies. The larger company operates a former Dow plant in Ludington, Michigan, with a calcium chloride capacity of 700k metric tonnes per year. The plant processes brine supplied by a Canadian operation. The second largest U.S. producer currently operates four plants throughout the U.S., two brine-based facilities in the Mojave Desert (California), and two facilities that use HCl and limestone feedstock in West Virginia, and Louisiana.

Outside of these two market leaders, the U.S. has limited calcium chloride producers. The U.S. market is also supplied by both Canada and Mexico. Leading Canadian producers include two brine-based producers. One Mexican-based producer is the only plant in North America running the Solvay Process.

16.3.4 Market Cost

Calcium chloride is sold in liquid and solid form, but the market always sells on a dry weight basis (dry metric tonnes – DMT) with pricing and margins determined by application. De-icing and dust control are the lowest price applications, selling for around \$240 per metric tonne, followed by construction (\$300-350) and oil and gas (\$450-550). While not consumed in large quantities, calcium chloride can sell for over \$600 per metric tonne and approach \$1,000 in food, agriculture, electronics, and chemical industry applications.

Production costs can be as low as \$80-100 per metric tonne for liquid calcium chloride produced from brine. Producing flake and pellet grades requires additional capital and operational costs for drying, typically adding around \$100 per metric tonne for flake and an additional \$50-100 per metric tonne for pellet capabilities.

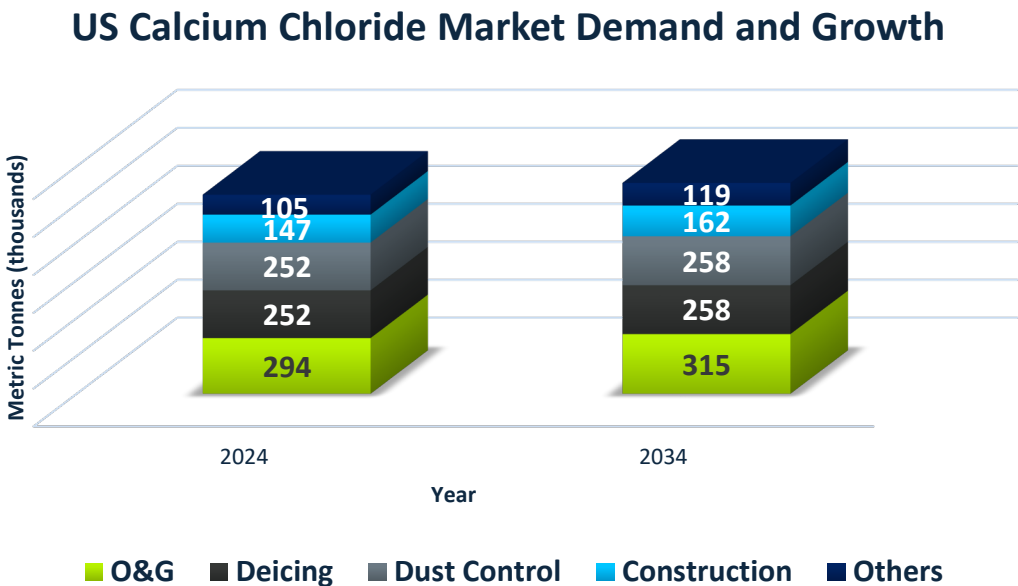
16.3.5 Calcium Chloride Market

When combined, the use of calcium chloride for road de-icing and dust control represents the largest application, with 2024 demand in the U.S. reaching 252k metric tonnes for each. De-icing is tied to winter weather patterns, where demand in the northern U.S. and Canada was strong in 2024 and early 2025. Historically and looking ahead, both segments are expected to grow at around 0.5% CAGR.

Usage in the oil and gas sector as a drilling fluid is the largest individual use in the U.S. at 294k metric tonnes. Key markets include Permian (West Texas), Marcellus (Appalachia), and offshore (Gulf of Mexico). U.S. oilfield growth projections are roughly 0.75% in 2025 and 2026, with similar growth expected through 2030, followed by a gradual decline.

The remainder of the market comprises construction (147k metric tonnes) and other uses (105k metric tonnes), spread across numerous end-use applications such as food and beverage, agriculture, desiccants, refrigeration and cooling, water treatment, concrete and masonry surface treatment, metallurgy, tire weighting, humidification, and chemical synthesis. Growth for these categories is slightly higher, at 1.0% and 1.25% CAGR for construction and other uses, respectively. Figure 16.4 provides a breakdown of U.S. calcium chloride market demand and growth from 2024 to 2034.

Figure 16.4: U.S. calcium chloride market demand and growth, 2024 – 2034



### 16.3.6 Calcium Chloride Specifications

Calcium chloride is sold in the market in various forms: liquid (with concentrations ranging from 28-42%), flake (72-87%), pellets or prill (92-97%), and powder (83-99%). These ranges represent observed concentrations from U.S. producers. Powder is collected from pellet or prill processing. Most applications utilize calcium chloride in liquid form, so solids are dissolved in water for most final uses. Given its exothermic properties, which make solid calcium chloride effective at melting snow, heat management must be considered during dissolution.

Product purity is separate from the above-mentioned criteria. Common contaminants include alkali chlorides (such as NaCl), magnesium (such as  $MgCl_2$ ), and calcium hydroxide and specifications typically call for impurities to be less than 5%. For certain food and beverage applications, producers can obtain various certifications, such as Halal, Kosher, etc.

## 16.4 Gypsum

### 16.4.1 Market Overview

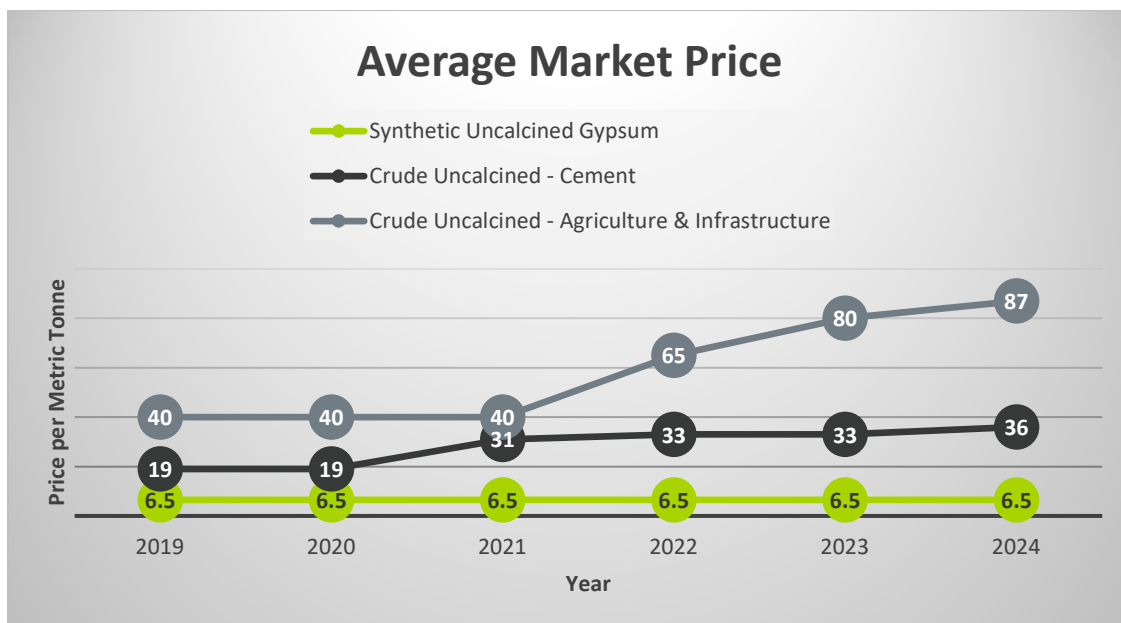
Gypsum, a versatile mineral, finds extensive use in construction, agriculture, and industry. Primarily utilized for drywall, plaster, and cement, it provides fire resistance and acoustic insulation in construction. In agriculture, gypsum enhances soil structure by supplying calcium and sulfur. It is obtained through natural mining and as a synthetic byproduct from flue-gas desulfurization (FGD). Between 2019 and 2024, U.S. gypsum demand held steady at approximately 44 million metric tonnes, with prefabricated products leading the market. During this period, the U.S. market experienced a modest growth rate of 0.1% CAGR.

### 16.4.2 Historical Pricing

Between 2019 and 2024, gypsum prices rose steadily due to supply constraints and cost pressures. In 2024, the average price for calcined gypsum reached \$63 per metric tonne, while uncalcined gypsum averaged \$13 per metric tonne. The sharper increase in calcined gypsum prices was driven by value-added processing and strong demand from the construction sector.

In 2024, the price of crude uncalcined gypsum used in cement and agriculture were estimated to vary from \$36 to \$87 per metric tonne, depending on the grade and application. Meanwhile, synthetic gypsum prices remained stable at approximately \$6.5 per metric tonne from 2019 to 2024. Figure 16.5 below provides historical pricing for various types of gypsum.

Figure 16.5 Average market price for uncalcined gypsum by grade and application, per Kline

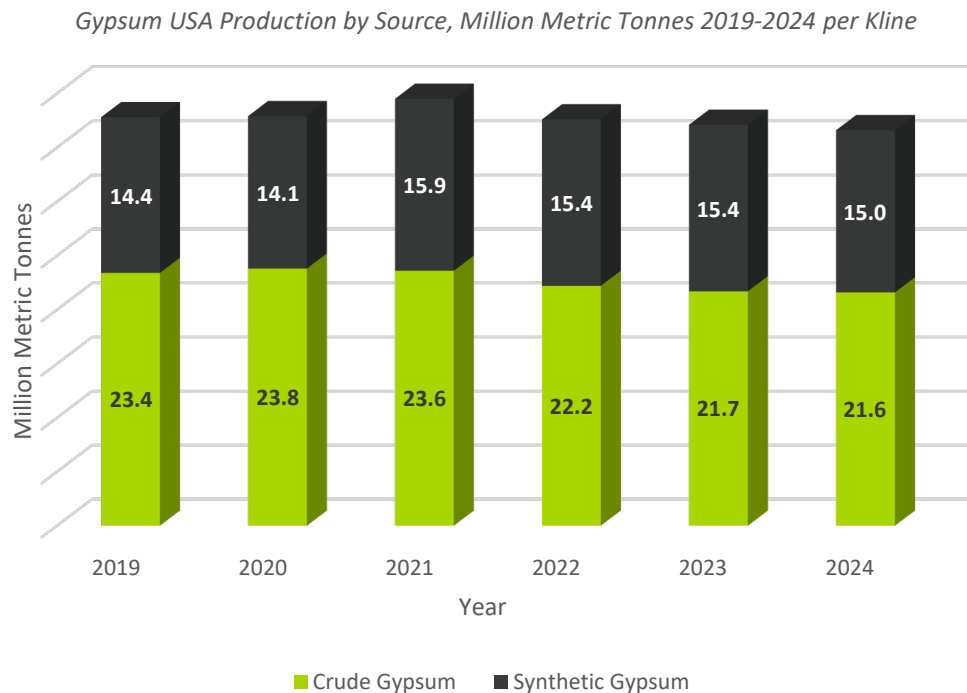


### 16.4.3 Market Imbalance

The U.S. gypsum market is supported by both domestic production and imports. Imports have risen due to limited local supply near demand centers and the decline in synthetic gypsum output caused by the phase-out of coal-fired power plants. As coal-fired power plants reduce production, the drop in synthetic gypsum supply is anticipated to open market opportunities for 5E's gypsum output. The Project is strategically located near major agricultural demand centers and wallboard manufacturers, which are expected to be primary outlets for the byproduct.

Gypsum is imported from countries such as Mexico, Spain, and Canada. Despite these imports, the U.S. retains substantial domestic production capacity, with major producers including USG, National Gypsum, and Georgia-Pacific. Figure 16.6 provides a breakdown of the U.S. production between crude and synthetic gypsum.

Figure 16.6 Gypsum USA production



### 16.4.4 Market Costs

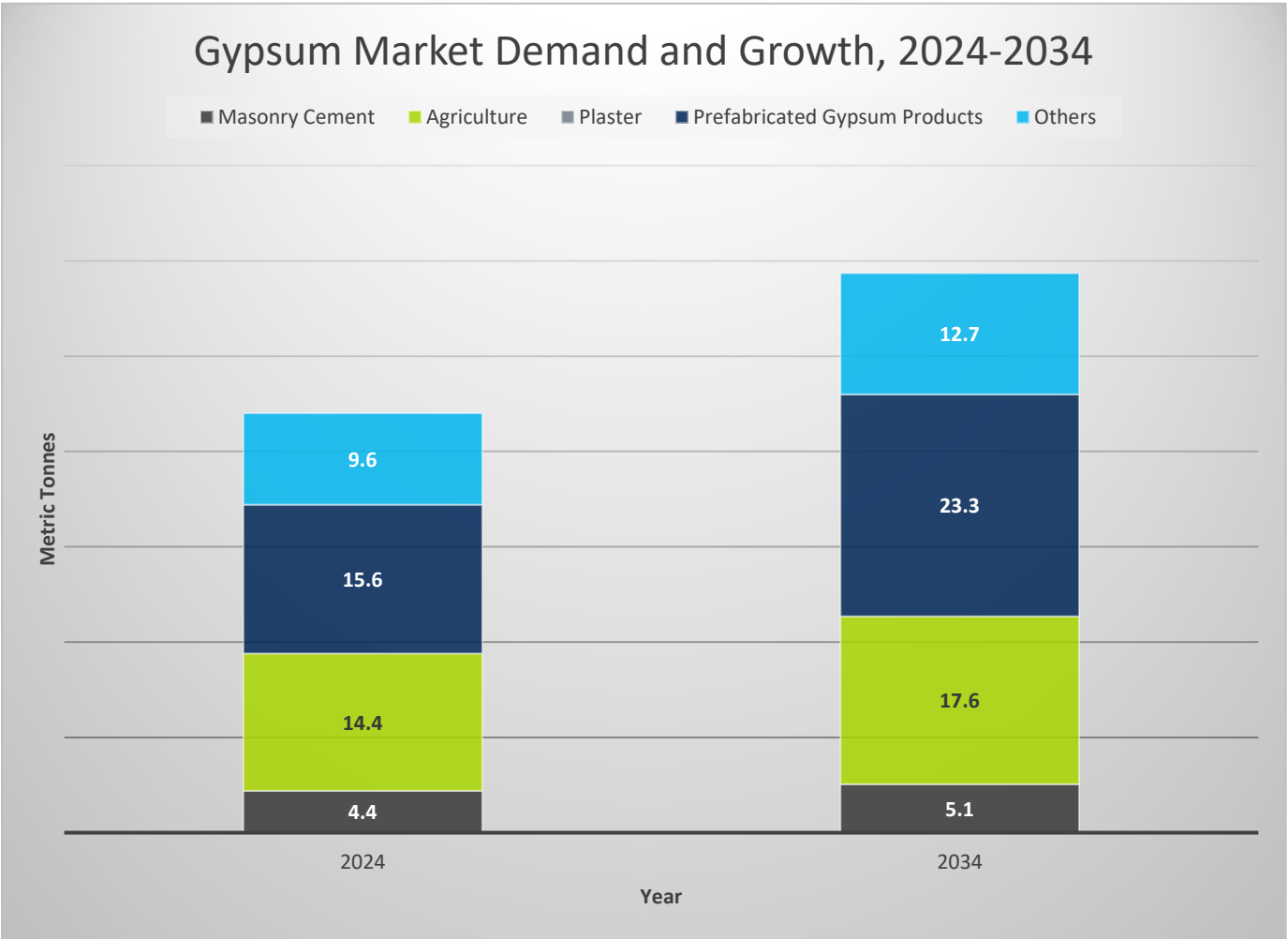
The operating costs for gypsum production can vary significantly due to several factors. Major producers typically do not disclose detailed operating costs publicly, making it difficult to determine the exact figures. However, overall production costs are influenced by factors such as increased manufacturing efficiency, recycling practices, and import dynamics. For example, synthetic gypsum, a byproduct of coal-fired power plants, is favored for its high purity levels (95–99%) and consistent quality. The cost of crude gypsum has increased due to rising energy and transportation expenses, while synthetic gypsum prices fluctuate based on transport distance and contractual agreements. Additionally, regional factors, such as proximity to mines and local demand, are crucial in determining market costs.

### 16.4.5 Gypsum Market

The U.S. gypsum market is projected to grow steadily at a 2.8% CAGR through 2034, driven by rising use of prefabricated gypsum products like lightweight wallboards, strong construction activity, and consistent cement demand. Agricultural applications are also gaining traction, especially in regions with saline soil and poor water quality, such as California. Specialty uses in plaster, joint compounds, and fillers add niche demand. Limited domestic supply near key consumption hubs has heightened reliance on imports, driving up delivered costs and creating an opportunity for regionally available

synthetic gypsum to meet growing demand. Figure 16.7 provides the U.S. gypsum market and demand growth forecasted from 2024 to 2034.

Figure 16.7: U.S. gypsum market demand and growth, 2024 – 2034



16.4.6 Gypsum Specifications

Final gypsum specifications are not confirmed at this time but it is expected that 5E will meet specification requirements for cement manufacturing.

16.5 Conclusions

Boric acid is a versatile product with hundreds of end-use applications that are critical to food security, national defense, decarbonization, electrification, and consumer consumption, among others. Due to increased demand for existing applications and new projected demand from future-facing technologies, combined with two major suppliers operating at, or near capacity, the supply of boric acid, and many downstream derivatives that require boric acid as feedstock, has been in tight supply, resulting in higher prices over the past 18 months. With existing suppliers unlikely, or unable, to add meaningful capacity, and only six new boric acid projects identified, of which only 5E is substantially permitted, the supply-demand deficit is expected to continue or worsen over the remainder of the decade. As a result, pricing will likely remain elevated and continue to rise. As a US-based producer, 5E is positioned to secure both domestic and strategic global supply chains for boric acid and other key boron derivatives that require boric acid.



## 16.6 Contracts

5E is engaged in discussions with several direct end-users as well as distributors for supply of boric acid, calcium chloride, and gypsum. 5E also has multiple signed non-binding letters-of-intent and/or proposal letters with terms agreed in principle which could result in definitive offtake agreements for multi-year supply. For boric acid specifically, these customers and distributors represent multiple end-use applications including specialty glass, insulation, defense, agriculture, and others, as well multiple geographic regions. Since 5E has produced products from its SSF, 5E has supplied and qualified finished products with future customers, with the intent of securing contracts for most of the available phased capacity, while reserving a portion for spot market sales and increased tonnage for contracted customers. 5E is in discussions with a large, local cement manufacturer for offtake of gypsum and the customer has sampled the product. Additionally, 5E is discussing a calcium chloride offtake agreement with two different counterparties who have visited the site. One is a large regional distributor, and the other is a large global manufacturer with operations in the southeastern United States. Delivery and saleable gypsum and calcium chloride will likely focus on customers within a certain geographical radius to minimize overall delivered costs.

## 17 Environmental Studies, Permitting, and Closure

### 17.1 Environmental Requirements for Solution Mining

Due to the depth and characteristics of both the ore body and overburden, in the 1980's the decision was made to recover the ore via solution mining. The Project mineralized deposit is an ideal candidate for solution mining as it is bound by faults. The Project is permitted to produce 90,000 short tons per year of borate, defined as boron oxide or boron oxide equivalent, thus permitting up to approximately 160,000 short tons of boric acid.

### 17.2 Environmental Study Results

The Project is located on both public and private lands. The public lands are managed by the BLM in accordance with its 43 CFR §§ 3809 Surface Management Regulations, the Federal Land Policy and Management Act, and federal environmental laws. The private lands are administered by San Bernardino County Land Use Planning (SBC – LUS) in accordance with the California Surface Mining and Reclamation Act, the County Development Code, and state environmental laws.

In 1990, a Plan of Operations (PoO) was submitted to the BLM and a Mining Conditional Use Permit and Reclamation Plan was submitted to San Bernardino County, which triggered environmental review under the National Environmental Policy Act (NEPA) and the California Environmental Quality Act (CEQA). BLM and the County prepared a joint Environmental Impact Statement (EIS)/Environmental Impact Report (EIR) to satisfy their environmental review requirements under NEPA and CEQA, respectively.

The EIS/EIR process follows clearly defined requirements for public participation and studies, such as threatened and endangered species, cultural resources, light, noise, and impacts to local communities. The studies were completed, as was the public participation process. Additional studies are currently not required at this time.

In 1994, the EIS/EIR process resulted in the issuance of a ROD from the BLM that approved the PoO and approval of the Mining Condition Use Permit and Reclamation Plan from the SBC – LUS, as discussed below.

### 17.3 Required Permits and Status

5E currently has the following permits in place:

1. The Mojave Desert Air Quality Management District (MDAQMD) has issued Operating Permits for the SSF and the permits are renewed annually. After FEED engineering and during detail design of the LSBF, once 5E has determined each original equipment manufacturer (OEM) for major pieces of equipment and based on the specification sheets for each piece of equipment, Authorization to Construct (ATC) permits for the LSBF will

be provided to MDAQMD for approval. It is expected that the issuance of the LSBF ATCs will require that the Operating Permit for the SSF be closed. The ATC permits for the LSBF must meet National Ambient Air Quality Standards (NAAQS) and MDAQMD requirements (ARB, MDAQMD, and EPA).

There is no reclamation or closure requirement under MDAQMD.

2. The Lahontan Regional Water Quality Control Board (LRWQCB) issued the current Waste Discharge Requirements (WDRs) in 1988. The WDRs regulate activities in the existing surface impoundments, which were used in the 1990's to produce CadyCal and are no longer being used. 5E remains compliant with the permit by complying with the monitoring requirements and submitting quarterly reports. A Final Permanent Closure Plan has been approved by the LRWQCB for closure of the existing impoundments. Closure of the ponds and 1988 WDRs is expected to be finalized later in 2025 or 2026. The current LSBF design includes approximately 37 acres of evaporation ponds for the purpose of removing sodium and calcium from the back end of the processing plant. 5E will apply for a new or amended WDRs order from LRWQCB for the LSBF.

There is an existing reclamation and closure requirement approved by LRWQCB. The bond amount to close the ponds is included in the SBC – LUS Financial Assurance Cost Estimate (FACE), discussed below. This is currently a cash bond.

3. The LRWQCB previously issued a Notice of Non-applicability (NONA), verifying that the Project does not require a stormwater permit for approved construction and operations activities.

There is no reclamation or bonding requirement associated with the NONA.

4. SBC- LUS issued the Mining Conditional Use Permit and Reclamation Plan in 1994, based upon the 1990 application and ensuing EIR. The Reclamation Plan was amended, and the permit was modified in 2019 to address changes such as relocation of the processing plant and additional water related infrastructure. Ground use is regulated in accordance with applicable state law. The Mining Conditional Use Permit and Reclamation Plan includes Conditions of Approval for engineering and planning related activities, as well as requirements to avoid impacts to desert tortoises. The permitted production throughput under the Mining Conditional Use Permit is 90,000 short tons of boron oxide or boron oxide equivalent.

5E maintains a cash bond with the California State Mining and Reclamation Agency, as administered by SBC – LUS. The FACE is updated annually. The FACE includes demolition of all existing structures, regrading, and revegetation of all disturbance on private lands. This bond also includes plugging and abandonment of all wells located outside the U.S Environmental Protection Agency (EPA) UIC purview (discussed below).

5. The BLM issued a ROD in 1994, establishing the EIS boundary (Figure 6.2). The ROD authorizes the mining of borates. The ROD also has requirements for company activities to avoid adverse impacts to desert tortoises and cultural resources.

Reclamation and land disturbance for BLM is currently included with the FACE on file with the County and bonded in cash with the California Division of Mine Reclamation.

6. The EPA retains primacy for Class 3 solution mining Underground Injection Control UIC permits in the State of California. EPA issued the UIC permit for the Project in August 2020. The permit defines the Area of Review (AOR) boundary. All subsurface solution mining activities, including monitoring wells, are located within the AOR boundary. The EPA approved mining operations in November 2023.

Per the permit conditions, 5E has installed five upgradient and four downgradient monitor wells for the initial mining block. As a condition to receive final approval in November 2023, the EPA required modification to the permit and the installation of three additional water monitoring wells. The permit was modified in June 2024, and the three additional wells were installed in Fall 2024.

5E installed four IR Wells and subsequently modified the permit to include horizontal wells. In July 2025, two of the IR Wells were converted from vertical wells to horizontal-side tracks where each well extends approximately 1,500 ft. 5E expects to submit a final mine plan to the EPA for review based on the performance of the horizontal-side track IR wells.

5E has submitted and maintains a surety bond with the EPA for plugging and abandonment of all wells within the EPA AOR boundary.

7. Additional environmental permitting that will likely be required for the LSBF includes:
  - a) The California Unified Control Act/Agency (CUPA) has primacy over EPA's Tier II reporting requirements. The Hazardous Material Business Plan (HMBP) has been submitted for construction related activities and will be updated with processing related chemicals that are expected to be utilized to operate the LSBF.

## 18 Capital and Operating Costs

Capital and operating costs are incurred and reported in US dollars and are estimated at an initial assessment level with an accuracy of approximately +/-25%.

### 18.1 Capital Cost Estimate

The capital cost estimate includes the first phase of commercial production for the LSBF and a summary by scope or area is provided below in Table 18.1. Capital expended for the SSF is excluded as that is in operation and for purposes of this TRS has been sunk.

*Table 18.1: Capital summary*

Scope / Area	Capital Cost (USD millions)
Process Facility & Infrastructure	\$280.7
COGEN	\$50.2
Evaporation Ponds	\$5.6
Wellfield	\$30.8
<b>Sub-total Capital Costs</b>	<b>\$367.3</b>
Contingency	\$55.1
Owner's Cost	\$12.5
<b>Total Capital</b>	<b>\$434.9</b>

#### 18.1.1 Capital Cost Estimate – Processing Facility and Infrastructure

The capital cost estimate for the LSBF Project has been developed with a high level of confidence and rigor, in alignment with Association for Advancement of Cost Engineering (AACE) Class 4 standards. This estimate supports the development of a new greenfield processing facility, strategically located adjacent to 5E's existing SSF. Designed for a production capacity of 130,000 short tons per year of boric acid and associated byproducts, the LSBF Project marks a significant milestone in the company's long-term growth strategy.

Led by Fluor, an industry leading engineering and construction firm, in close collaboration with 5E and Tier 1 equipment vendors, the estimate reflects the project's scope as defined in February 2025. Between February and June 2025, the project team successfully completed a targeted value engineering program and additional technical test work. These efforts resulted in meaningful refinements to both the process design and execution strategy, which have been integrated into the project's critical engineering deliverables, including updated process narratives, flow diagrams, material balances, and equipment list/pricing.

These refinements have contributed to a more efficient and cost-effective project configuration. Key improvements included optimizing the boric acid head grade, removing the need for upfront solid/liquid separation equipment such as clarifiers, and incorporating evaporation ponds for sodium chloride handling. Additional efficiencies were achieved through the optimization of utilities and tankage, the removal of the boiler system (now supported by the Cogen WHRS), reuse of existing site infrastructure, and a more compressed facility layout.

Collectively, these enhancements have led to a reduction in the capital expenditure estimate while simultaneously increasing the facility’s design capacity. The improvements have also strengthened the project’s financial model, resulting in a more favorable internal rate of return (IRR) and improved overall economic performance. Furthermore, the process modifications and supporting test work have increased confidence in the technical basis of design, providing a solid foundation for the next phase of project development. Table 18.2 provides a detailed breakdown of the Process Facility and Infrastructure portion of the estimate in Table 18.1.

*Table 18.2: Detailed breakdown of process facility and infrastructure*

<b>Description</b>	<b>Total Cost (USD millions)</b>
Direct Field Costs	\$265.1
Indirect Field Costs	\$28.3
<b>Total Field Costs</b>	<b>\$293.4</b>
Home Office Costs	\$18.6
<b>Total Field and Office Costs</b>	<b>\$312.0</b>
Escalation	\$12.4
Contingency	\$46.8
Sales and Use Taxes	\$3.3
<b>February 2025 Class 4 – Indicated Total Cost</b>	<b>\$374.6</b>
Value Engineering and Process Refinements	(\$47.1)
<b>July 2025 Class 4 – Indicated Total Cost with Adjustment</b>	<b>\$327.5</b>

The capital estimate summary above reflects the outcome of a structured and disciplined development process. To support this estimate, a robust methodology was applied—grounded in industry best practices and tailored to the specific characteristics of the LSBF Project. The following section outlines the basis of estimate, including the data sources, engineering inputs, pricing strategies, and assumptions that underpin the capital cost model.

#### 18.1.2 .Processing Facility and Infrastructure – Basis and Methodology

The capital estimate methodology integrates a combination of vendor budget pricing, historical cost data, and engineering-developed material take-offs (MTOs), and Fluor’s proprietary unit rate databases. Direct field costs were calculated using Fluor’s Standard Unit Effort Hours Catalog, adjusted for site-specific productivity factors derived from a proprietary algorithm that considers labor availability, climate, site logistics, and project complexity. Mechanical equipment pricing was based on a mix of formal vendor quotes and internal benchmarks from similar projects.

Figure 18.1: Summary of equipment pricing

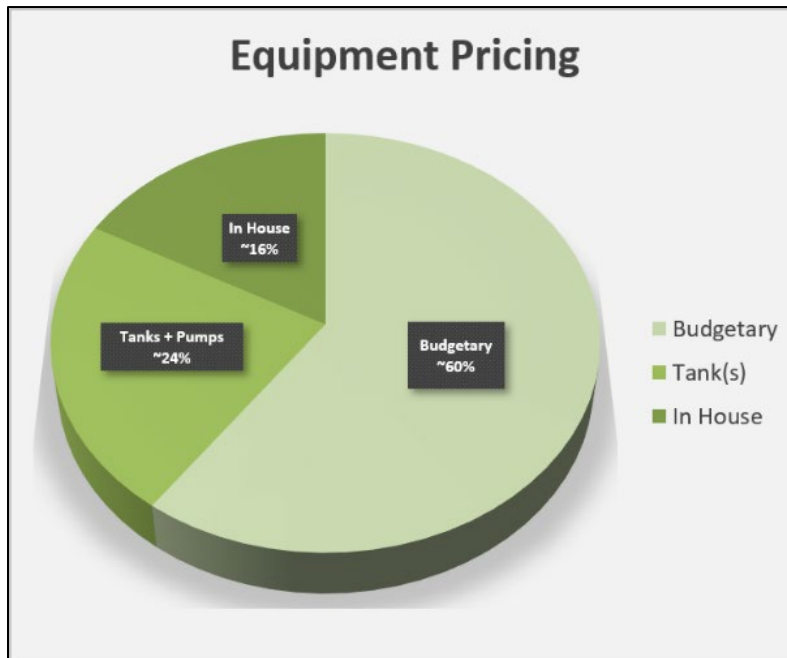


Table 18.3: Bid summary

Tier #	Equipment Description	Bid(s) Requested	Bid(s) Received
1	Crystallizer/Evaporator Package (including Heat Exchangers and Ancillaries)	3	3
1	Centrifuge Package	4	3
1	Filter Press Package	4	4
1	Belt Filter Package	4	3
1	Sedimentation Package (Clarifier/Thickeners)	4	4
1	Dryer/Cooler Packages (with Cyclones)	4	4
1	Chilled Water Package	1	1
1	Boiler System Package	1	1
1	Boric Acid Bagging System	In-house	N/A
1	Electric House Package	In-house	N/A

The estimate includes detailed cost modeling for civil works, concrete, structural steel, buildings, mechanical equipment, piping, electrical systems, instrumentation, and control systems. Indirect field costs, home office costs, and construction services were applied using historical percentages and industry norms. Allowances were included for material overbuy, construction waste, and MTO uncertainty. Escalation was applied at 4% from Q1 2025 forward, and a deterministic contingency of 15% was included to account for uncertainties within the defined scope.

The estimate assumes an EPCM execution strategy, with contractors providing construction labor, supervision, tools, and equipment. All costs are presented in U.S. dollars and reflect pricing as of Q1 2025. The capital estimate excludes owner's costs, permitting, land acquisition, environmental remediation, and other external factors. Owner's costs such as mine well development, insurance, commissioning, and infrastructure outside the battery limits are addressed separately.

The estimated accuracy range for this AACE Class 4 estimate is  $\pm 25\%$ , which is consistent with industry standards for projects at the PFS stage. This range reflects the typical level of definition at this phase and is not indicative of the quality of the estimate itself. Rather, it highlights the prudent approach taken to account for early-stage variables. To

further demonstrate the strength and maturity of the LSBF estimate, Table 18.4 benchmarks the project's deliverables against standard AACE Class 4 criteria. The estimate is supported by a comprehensive suite of engineering deliverables, including process flow diagrams, simulation and material balance data, equipment lists, and preliminary design documentation, all of which contribute to a well-substantiated capital cost basis. For further details on the capital basis of estimate refer to 5EAM-G1-PLN-310-00001.

Table 18.4: 5E project deliverables versus standard AACE Class 4 criteria

Estimate Accuracy & Deliverable Requirements Class 4			
Category	Estimate Items	AACE Class 4 (Typical)	5E PFS
Maturity Definition	Engineering % Complete	1-5%	2.5-5%
Project Definition	Plant Capacity	Preliminary	Defined
	Class of Facility	Preliminary	Defined
	Plant Location	Preliminary	Defined
	Soils Hydrology / Geotech	Preliminary	Semi Defined
	Project Master Schedule	Preliminary	Preliminary
	Construction Execution Strategy	Preliminary	Preliminary
	Procurement & Contracting Strategy	Preliminary	Semi Defined
	Engineering Design Criteria	Preliminary	Semi Defined
Engineering Deliverables	Process Flow Diagrams	Preliminary	Defined
	Plot Plans	Preliminary	Preliminary
	Mechanical Equipment List & Datasheets	Partial	Semi Defined
	Piping Line List & Line Classes	N/A	Preliminary
	Piping Specialty Item List	N/A	N/A
	Electrical Equipment List	Preliminary	Semi Defined
	Instrument Index	N/A	N/A
	Material Specifications	N/A	Preliminary
Bulks Quantification	Equipment Envelope	Cost Factor	Equipment Modelling / Layout
	Civil	Cost Factor	100% Eng MTO
	Concrete	Cost Factor	50% Eng MTO / 50% Est MTO
	Steel	Cost Factor	85% Eng MTO / 15% Est MTO
	Piping	Cost Factor	65% Eng MTO / 35% Est MTO
	Electrical	Cost Factor	25% Eng MTO / 75% Est MTO
	Infrastructure	Cost Factor	100% Eng MTO
Material Pricing Basis	Mechanical Equipment	100%	60% Budgetary / 40% Inhouse
	Electrical Equipment	Budgetary or Inhouse	
	DCS / Control System	Inhouse	
	Pipe & Pipe Fabrication	Cost Factor	In-House Prices from nearby representative project firm pricing
	Fabricated Structural Steel		
	Bulk Electrical & Instruments		
Contract Pricing Basis	Civil / Site Prep / Piling	Cost Factor	In-House Prices
	Concrete		In-House Prices
	Buildings		In-House Prices
	Steel		In-House Prices
	Mechanical		Cost Factor
	Piping		In-House Prices
	Electrical & Instrumentation		In-House Prices
	Insulation & Paint		Cost Factor
	Module Fabrication		N/A
	Logistics Cost		Cost Factor
Construction Inputs	Temp Facilities & Services (incl. Man camp)	Cost Factor	Preliminary; Historical DFC and IFC Factored Average Rates Used
	Construction Equipment Utilization plan		
	Heavy Haul & Heavy Lift plan		
	CM Staffing Plan		
	Site Assignment Policy		



Estimate Accuracy & Deliverable Requirements Class 4			
Category	Estimate Items	AACE Class 4 (Typical)	5E PFS
	Area Market Labor Analysis	N/A	
Estimate Accuracy	AACE (18R-97)	L: -15% to -30% / H: +20% to +50%	+/-25%
	Typical Contingency	20% to 30%	15%

### 18.1.3 Capital Cost Estimate – Evaporative Ponds

The capital cost estimate for the solar evaporation pond system was developed by Ad-Infinity who are recognized in the industry as one of the global leaders in evaporative pond design and execution. The estimate is in alignment with AACE Class 4 standards and is a culmination of a FEL-2 specific study commissioned by 5E.

This estimate supports the development of a new greenfield solar evaporative pond system encompassing a total of 37 acres including a scope taking into site and environmental parameters (topography, evaporation rates, temperature, wind, and radiation) developing steady-state mass and energy balances, and geometric and operational sizing of the ponds and berms, as well as developing a salt harvesting plan.

The capital estimate methodology integrates a combination of vendor and area subcontractor budget and material pricing, historical cost data, and engineering-developed material take-offs (MTOs). A contingency of 15% was included to account for uncertainties within the defined scope. All costs are presented in U.S. dollars and reflect pricing as of Q2 2025.

### 18.1.4 Capital Cost Estimate – Cogeneration Combined Power & Heat (CHP) Plant

A capital cost estimate for the Combined Power & Heat Plant (CHP) was derived from competitive budgetary bid quotations received from recognized global Tier 1 OEM vendors suppliers. The total direct and indirect packages installation cost was established by using a Lang factor which is a process industry standard methodology that utilizes a multiplier that represents the ratio of the total installed cost (TIC) to the total equipment cost (TEC).

### 18.1.5 Capital Cost Estimate – Wellfield

The operation is an owner operated mining operation. A third-party contractor will perform drilling of the in-situ injection recovery well field and a third-party OEM has designed and will manufacture the artificial lift system. As detailed in Section 13, the wellfield calls for the installation of 27 horizontal wells and jet pumps for artificial lift. Table 18.5 below provides a summary of the wellfield capital cost. The cost for the wellfield includes the following: drill pad construction, 3<sup>rd</sup> party drilling, downhole material (casing, production tubing, and cement), and artificial lift (jet pumps and jet pump triplex surface pumps).

Table 18.5 Mining capital cost estimate

Description	Total Cost (USD \$ millions)
Site Works	\$1.9
Well Materials	\$9.4
Drilling	\$5.6
Logging	\$2.0
Stimulation and Completions	\$2.1
Surface Facilities	\$3.7
Artificial Lift	\$6.1
<b>Wellfield Sub-total</b>	<b>\$30.8</b>
Contingency	\$4.6
<b>Total Wellfield</b>	<b>\$35.4</b>

### 18.1.6 Other Sustaining Capital

The wellfield is designed such that the quantity of wells is expected to be sufficient for the current life of mine and it is expected that overtime the extraction method will transition from injection of the mining fluid until the well becomes hydrostatic and then recovery of the fluid (i.e., “huff and puff” extraction) to complete reservoir flow and recovery. Using the current estimate of the wellfield as a basis, 5E assumed \$5.7 million is outlaid incrementally every five years as sustaining for major workovers and any additional necessary wells.

### 18.1.7 Wellfield Basis

The wellfield capital estimates were based on actual equipment purchased for the SSF, vendor bids, actual costs derived from the injection recovery wells for the small-scale facility and July 2025 drill program, and third-party quotes. The quantity of wells estimated to provide the chemical plant with PLS to achieve the stated design is based on engineering simulations, actual wellfield data from the SSF, and incorporates work from MSME.

Mining equipment, initial wells, and sustaining capital cost estimates were based on the following:

- All injection recovery wells were based on new casing, production tubing, screens, and well heads.
- Costs for drilling, auxiliary, and overhead were based on third-party estimates and work performed.
- Mining capital includes a 15% contingency.

### 18.1.8 Closure Costs

Closure costs have not been included in this estimate as the reserve and life of mine only account for 41% of the measured and indicated resource and it is assumed that expansion capital can be deployed in the future and the wellfield and mine plan can be updated to convert incremental resources to reserves.

### 18.1.9 Owner's Costs

Table 18.6 provides the breakout of Owner's Costs breakout and totals \$12.5 million. This estimate was provided by 5E. No formal contingency is applied to Owner's Cost.

*Table 18.6: Owner's cost breakdown*

Item	Cost (US \$ million)
Owner's team	\$4.2
Construction insurance	\$3.6
Taxes	\$4.7
<b>Total</b>	<b>\$12.5</b>

## 18.2 Operating Cost Estimates

Operating costs have been forecasted based on the material and energy balance provided by Fluor. Operating costs are segregated as variable operating costs and fixed operating costs in the financial model. Variable operating costs include packaging, logistics, and raw materials such as natural gas, hydrochloric acid, sulfuric acid, and lime. Fixed operating costs include administrative labor, operating labor, general and administrative overhead, repair labor, repair materials, depreciation as well as taxes and insurance.

As with capital costs, operating costs are captured in US dollars and are estimated at an initial assessment level with an accuracy of approximately +/- 25%.

### 18.2.1 Variable Operating Cost

Variable operating costs are derived from a material balance with the following assumptions:

- Calcium-to-boron ratio of 1.2 calcium and sodium byproduct volumes and sulfuric acid consumption. This ratio is consistent with wellfield data obtained during operation of the SSF,
- 90% HCl efficiency rate with 10% HCl lost in the process, and
- 10.2% weight boric acid concentration in the PLS.

Variable materials and prices represented on the basis of cost per a produced short ton of boric acid are shown in Table 18.7. Cost figures include estimated freight to 5E. Pricing for raw materials is based on historical costs over the last 12 months.

*Table 18.7 Variable materials cost*

Material	Units	Cost US\$/short ton
HCl 36% solution basis	1,416.7 lb. /short ton H <sub>3</sub> BO <sub>3</sub>	\$158.61
Sulfuric acid	1,180.6 lb. /short ton H <sub>3</sub> BO <sub>3</sub>	\$124.13
Lime	423 lb. /short ton H <sub>3</sub> BO <sub>3</sub>	\$197.47

The basis for packaging and logistics included the following:

- \$18 per short ton of boric acid for packaging based on actual packaging for SSF.
- \$113.50 per short ton of boric acid for shipping and freight delivered to customers based on actual quotes received and paid by third-party logistic carriers.

The basis for utilities included the following:

- Natural gas consumption to operate COGEN facility consuming 1,791,477 MMBTU per year or 12.25 MMBTU per short ton of boric acid derived from the energy balance. Pricing for natural gas is based on a 12-month average of \$3.19 per MMBTU based on California City Gate pricing.

### 18.2.2 Fixed Operating Cost

Fixed operating costs include the following:

- Operating labor
- Site administrative labor
- Site general overhead
- Repair labor and materials
- Taxes and insurance
- Depreciation

Operating labor was derived from a principle first plan of operations with 80 operators and 30 employees for site administrative labor. Cost per person was estimated at \$86,680 and the basis for fixed overhead was derived by the current overhead rate of spend for 5E which is approximately \$150,000 per quarter and this is assumed to double for the LSBF. Repair labor and maintenance is estimated to be 3.0% of cumulative capital including sustaining capital. Taxes and insurance are assumed to be 1.5% of cumulative capital including sustaining capital. Depreciation assumes a 10-year useful life for initial capital and any sustaining capital is depreciated in the year incurred.

### 18.2.3 Other Operating Costs

Other operating costs include costs and credits associated with the material balance and process flow sheet which includes a byproduct credit for gypsum and calcium chloride and costs associated with metals precipitation waste. Gypsum is assumed to be net neutral cost and sold in the market at cost. Table 18.8 provides the breakdown of units

and cost associated with other operating costs and Figure 19.2 provides the total operating costs and credits over life of mine.

Table 18.8 Other operating costs

Material	Units	Cost US\$
Metals precipitation waste	\$ per short ton	\$ 45
Gypsum	\$ per short ton	\$ 12
Calcium chloride	\$ per short ton	\$ 55

#### 18.2.4 Basis for Operating Cost Estimates

Operating assumptions were based on the following assumptions:

- Year 1 operates at 64% capacity, 7,000 hours and produces 13.37 short tons of boric acid per hour.
- Year 2 operates at 88.9% capacity, 8,000 hours and produces 16.25 short tons of boric acid per hour.
- Year 3 operates at 93.3% capacity, 8,000 hours and produces 17.06 short tons per hour.
- Utilizations are based on mass and energy balances.
- Input costs use historical pricing over the last 12 months, third-party vendor quotes or actual inputs based on real time purchases at the SSF.

## 19 Economic Analysis

### 19.1 General Description

5E prepared a cash flow model to evaluate the Project's reserves on a real basis. This model was prepared on an annual basis from the reserve effective date to the exhaustion of mineral reserves for the current mine plan. As discussed in previous sections, additional resources could be converted to additional reserves with expansion of the wellfield or mine plan in the future. This section presents the main assumptions used in the cash flow model and the resulting indicative economics. The model results are presented in U.S. dollars US\$, unless otherwise stated.

All results in this section are presented on a 100% basis. As with the capital and operating forecasts, the economic analysis is inherently a forward-looking exercise. These estimates rely upon a range of assumptions and forecasts that are subject to change depending upon macroeconomic conditions, operating strategy and new data collected through operation of the small-scale facility.

### 19.2 Basic Model Parameters

Key criteria used in the analysis are presented throughout this section. Basic model parameters are summarized in Table 19.1.

Table 19.1 Basic model parameters

Description	Value
<b>Time Zero Start Date</b>	July 1, 2025
<b>Mine Life</b>	40 years with partial last year using Proven and Probable Reserve.
<b>Chemical Plant Start-up</b>	2028
<b>Discount Rate</b>	7%

All costs incurred prior to the model's start date are considered sunk costs. The potential impact of these costs on the economics of the operation is not evaluated. This includes contributions to depreciation and the small-scale facility as these items are assumed to have a zero balance at model start. The selected discount rate is 7% given the Projects risk profile, U.S. jurisdiction, permitting status, capability to secure U.S.-agency financing and was chosen as a reasonable cost for funding based on review of comparable projects in the development phase of the mining cycle. Additionally,

economic analysis is performed on a real basis that does not capture the nominal aspects of inflation, thus driving a slightly lower discount rate than would traditionally be captured on a nominal basis.

### 19.3 External Factors

#### 19.3.1 Pricing

Modeled prices are based on the prices developed in the Market Studies and Contracts section of this report Section 16 (see Figure 16.3) and were developed on a real basis. 5E engaged Kline to perform a preliminary market study and the assumptions and inputs for revenue in the financial model were based on the preliminary market study. A sensitivity analysis is performed below, and the financial model is most sensitive to boric acid pricing and this forecast is a material assumption. The prices are modeled as:

- Boric Acid: \$1,248 F.O.B. per short ton when production is forecasted to commence
- Gypsum: \$32.66 per short ton is held flat on a real basis throughout the model
- Calcium Chloride: \$174.18 per short ton is held flat on a real basis throughout the model

All products produced by the operation are modeled based on independent pricing forecasts as described in Section 16 and were prepared as part of a preliminary market study performed by Kline. Kline built a regression pricing model forecast for boric acid on a real basis with key inputs and drivers of the forecast utilization of supply and demand, sulfuric acid pricing, and cost of freight. The material driver to the pricing forecast is supply and demand utilization whereby the boric acid market is forecasted to grow at 5.5% as disclosed in Section 16 but supply is forecasted to fall short. Gypsum pricing was based on actual 2024 real pricing and the model assumes 5E handles freight and logistics. The netback price for gypsum is \$20.66 per short ton. Calcium chloride pricing was based on actual 2024 real pricing to the end market customers. This price was further discounted in the model to assume 5E would sell to distribution at bulk and the model assumes 5E handles freight and logistics. The netback price for calcium chloride is \$119.64.

#### 19.3.2 Taxes and Royalties

As modeled, the operation is subject to a combined 27.98% federal and state income tax rate. This tax rate is derived from 5E Boron Americas LLC tax rate as of June 30, 2025, the most recent fiscal year end. The model does not include any tax loss carryforwards and no existing depreciation pools are accounted for in the model. Any application of tax loss carryforwards would reduce the tax burden of the operation. The capital for the project is subject to depreciation over a 10-year period and sustaining capital is depreciated in the year incurred for purposes of financial modeling. There are no royalties to account for currently. The project is being evaluated as a standalone entity for this initial assessment without a corporate structure. As such, tax calculations presented here may differ significantly from the actual incurred by 5E.

#### 19.3.3 Working Capital

The assumptions used for working capital in this analysis are as follows:

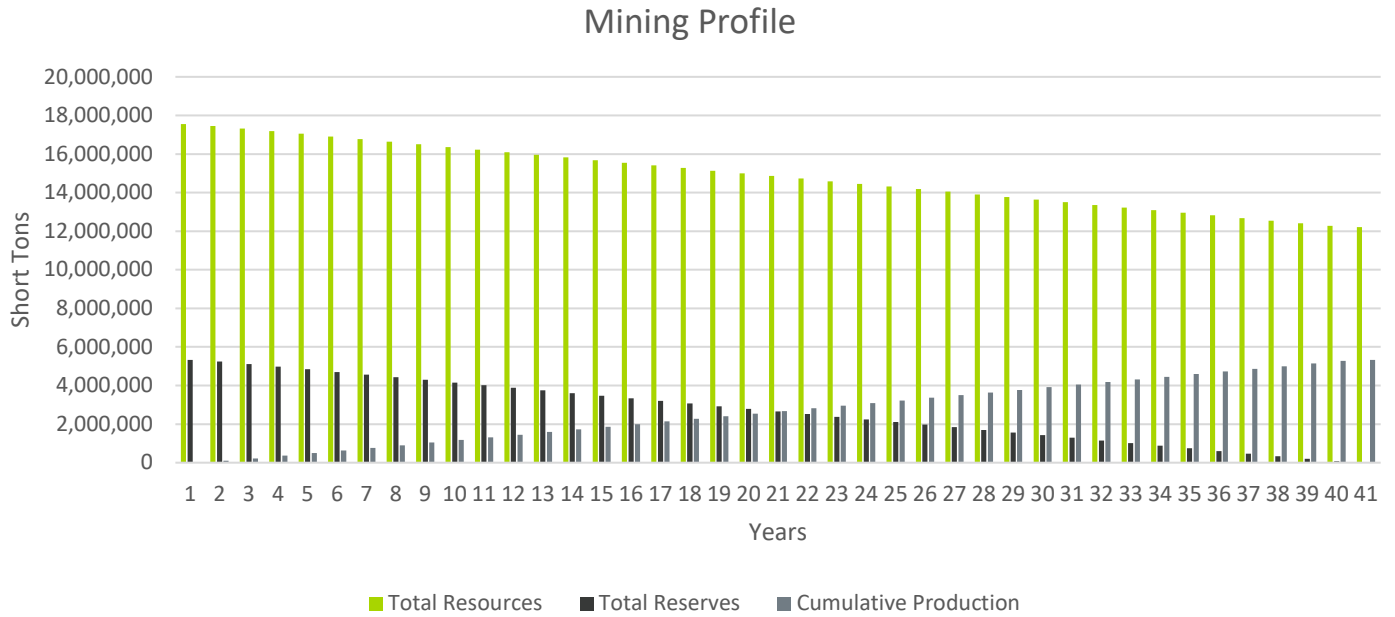
- Accounts Receivable: 30 days
- Accounts Payable: 30 days
- Zero opening balance for accounts receivable and payable

### 19.4 Technical Factors

#### 19.4.1 Mining and Production Profile

The modeled mining profile was developed by 5E. The details of the mining profile are presented previously in this report. No modifications were made to the profile for use in the economic model. The modeled profile is presented in Figure 19.1.

Figure 19.1: Resource Extraction Profile



A summary of the modeled mine life profile is presented in Table 19.2 Life of Mine Summary.

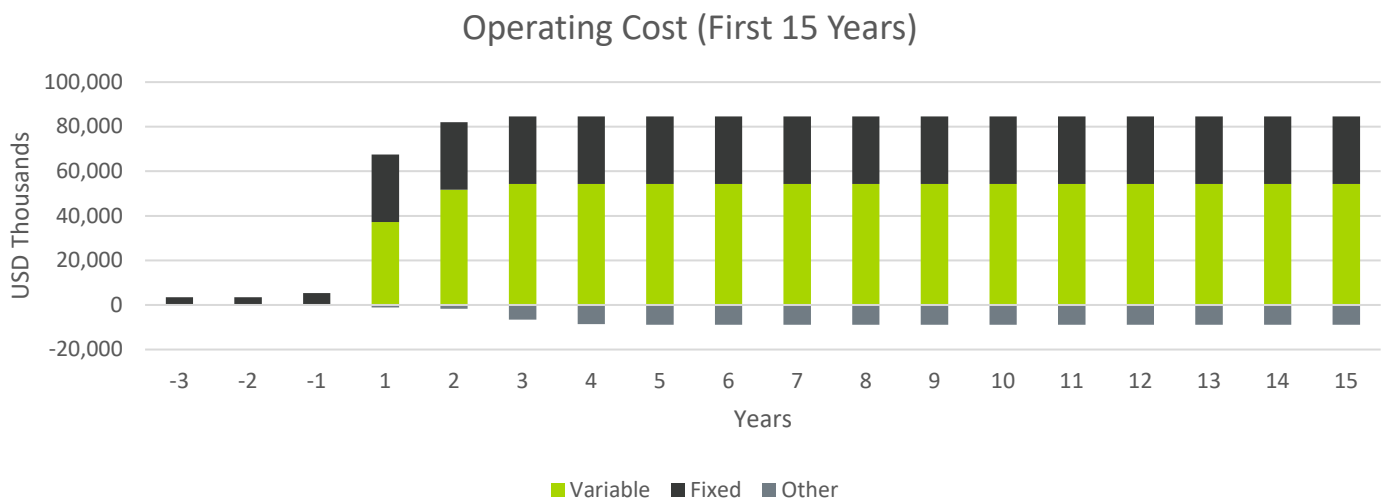
Table 19.2: Life of mine summary

Description	Unit	Value
Life of mine	Years	39.5
Reserves – Boric Acid	Short Tons	5.3 M
Quantity – Boric Acid Produced	Short Tons	11.4 M
Resources – Boric Acid	Short Tons	17.5 M

#### 19.4.2 Operating Costs

Operating costs modeled in US dollars can be categorized as variable, fixed and other operating costs credits. A summary of operating costs over the life of operation is presented in Figure 19.3 and Figure 19.4.

Figure 19.2: Operating costs (first ten years)





### 19.4.3 Variable Costs

Total variable operating costs over the life of mine are provided in Table 19.3 and Table 19.4.

*Table 19.3: Variable operating cost over life of mine*

<b>Variable operating cost:</b>	<b>Total US\$000's</b>
<b>Materials</b>	\$ 1,309,153
<b>Logistics</b>	605,539
<b>Natural gas</b>	208,214
<b>Total</b>	<u>\$ 2,122,906</u>

### 19.4.4 Fixed Costs

*Table 19.4: Total fixed operating cost over life of mine excluding depreciation*

<b>Fixed operating cost:</b>	<b>Total US\$000's</b>
<b>Administrative labor</b>	\$ 99,230
<b>Operating labor</b>	286,200
<b>General and administrative overhead</b>	51,000
<b>Repair labor</b>	214,757
<b>Repair materials</b>	300,659
<b>Taxes and insurance</b>	257,708
<b>Total</b>	<u>\$ 1,209,554</u>

### 19.4.5 Other operating costs / (credits)

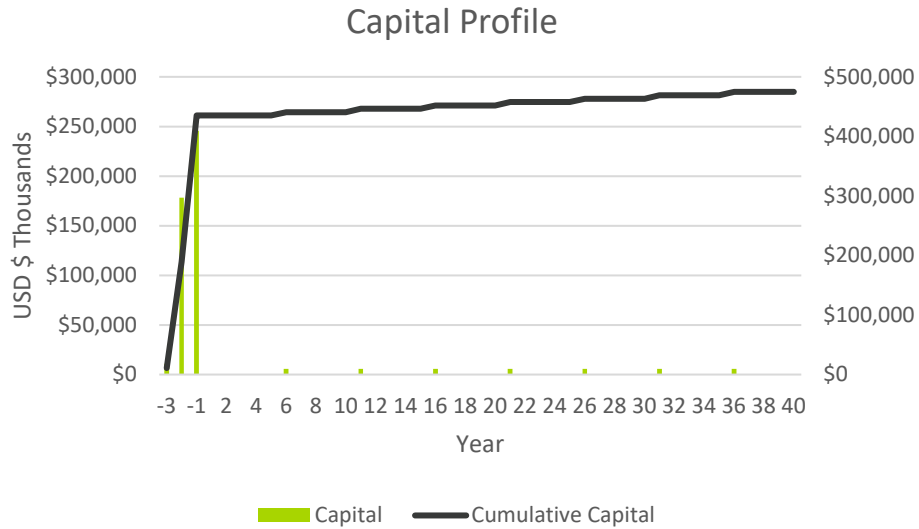
*Table 19.5: Total other operating costs / (credits) over life of mine*

<b>Other operating cost / credit</b>	<b>Total US\$000's</b>
<b>Calcium chloride</b>	\$ (265,530)
<b>Metals precipitation waste</b>	41,736
<b>Gypsum</b>	(109,368)
<b>Total</b>	<u>\$ (333,162)</u>

### 19.4.6 Capital Costs

Capital is modeled on an annual basis and is used in the model as developed in previous sections with 15% contingency. The modeled capital profile is presented in Figure 19.3.

Figure 19.3: Capital profile of the mine



#### 19.4.7 Infrastructure and Logistics

The economic analysis includes OSBL and ISBL capital, which includes a warehouse for boric acid storage and calcium chloride loadout station. Boric acid and calcium chloride transport will be serviced via truck with calcium chloride sold as a by-product credit in the local California market. Boric acid transport will be serviced via truck to local customers in the western United States, to the Los Angeles ports for shipment to Asia, and either shipped via truck to the eastern United States or shipped to rail for further transport. Capital includes a covered storage facility for gypsum which will be serviced via truck with gypsum sold as a by-product credit in the local California market. While revenue and by-product credits are captured in the economic model at F.O.B. pricing, freight and logistics are assumed as costs to 5E and included in operating costs estimates. Capital also includes an upgrade to the SoCal Edison service road that provides the main access to the Project. While a trade-off study is being performed, utility is assumed to be sourced via natural gas and main power delivered via gas COGEN. The capital estimate includes the cost and installation of the COGEN facility as well as a metering station and connection to the gas pipeline and all required piping to the COGEN facility. While it is common for similar projects to finance COGEN off-balance sheet and include as part of operating expenditure, the economic analysis assumes the COGEN is 5E operated and owned.

#### 19.4.8 Economic Results

The economic analysis metrics are prepared on an annual after-tax basis in U.S. dollars. The results of analysis are presented in Table 19.6. The annual project after tax cash flow is presented in Figure 19.4.

Figure 19.4: Cash flow projection

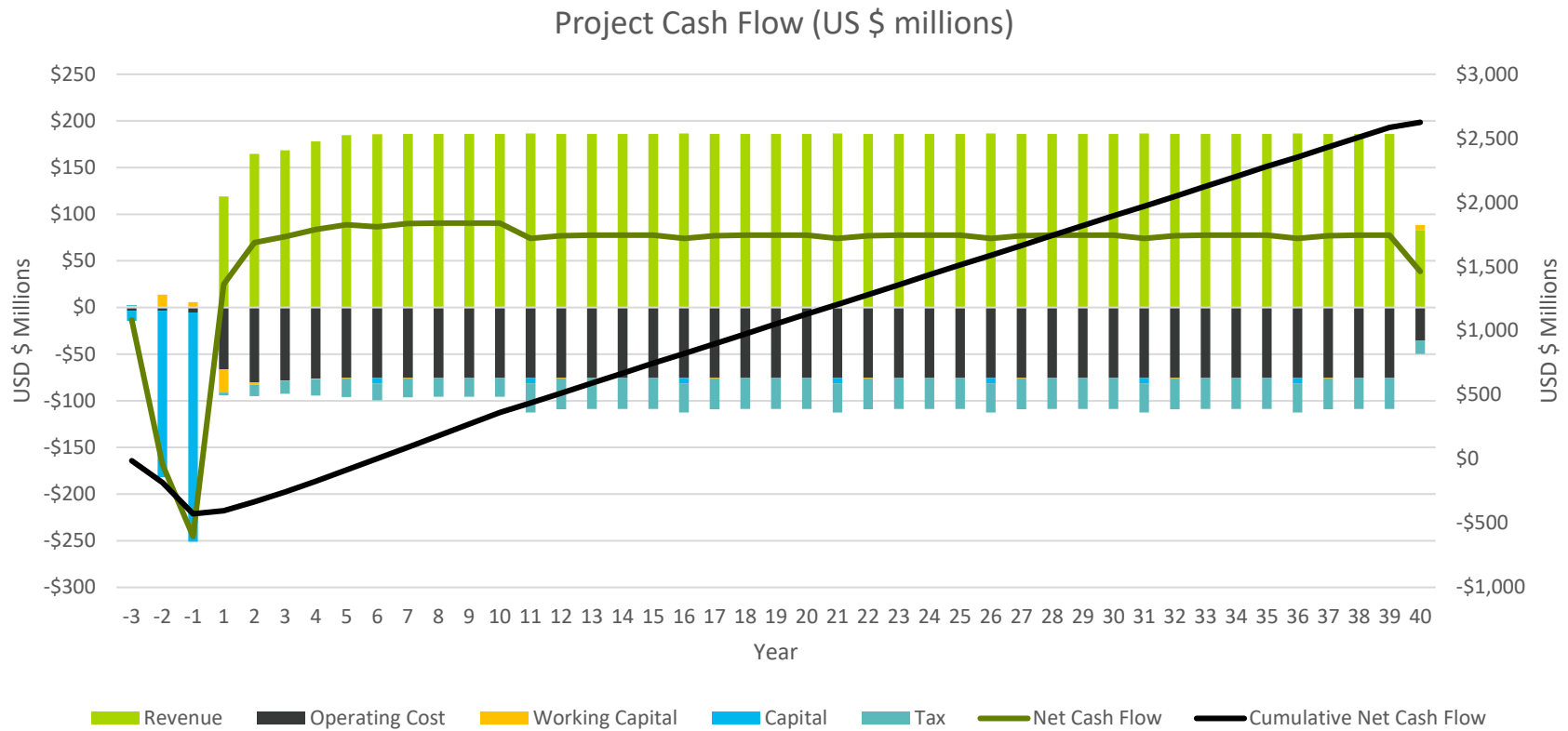


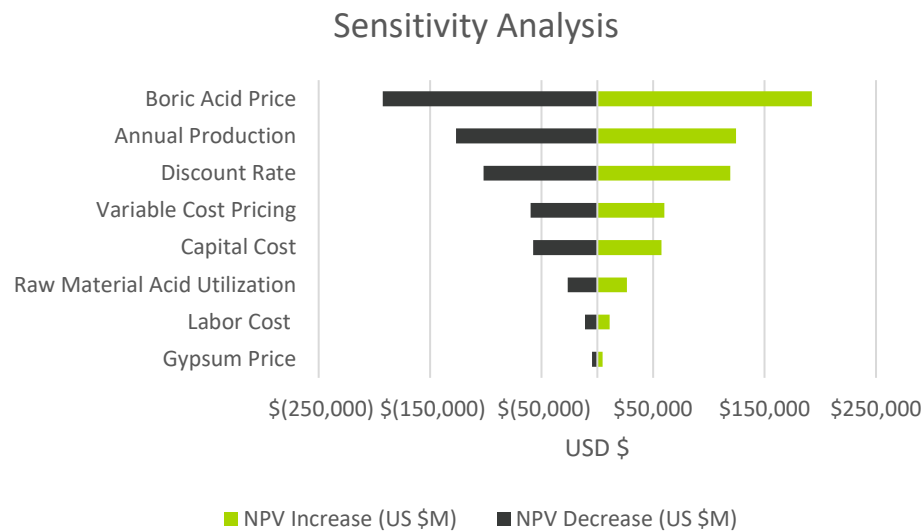
Table 19.6: Results of economic analysis

Life of Mine Cashflow	Units	Value
Total Revenue	US\$ Million	7,227.0
Operating Expenses	US\$ Million	2,999.3
Operating Margin Ratio	%	58.5
Capital Outlay	US\$ Million	474.8
Taxes Paid	US\$ Million	1,123.5
Depreciation	US\$ Million	474.8
Free Cash Flow	US\$ Million	2,625.4
NPV @ 7%	US\$ Million	724.8
IRR	%	19.2
Payback	Years	6.1

#### 19.4.9 Sensitivity Analysis

Sensitivity analysis for the financial model was performed based on changes to boric acid price, annual production, discount rate, variable cost pricing, gypsum price, labor cost per person, and raw material acid utilization. Using a  $\pm 10\%$  change for each variable, NPV<sub>7</sub> is plotted in real dollars for comparison and arranged in order of total variability in Figure 19.5.

Figure 19.5: Sensitivity analysis



#### 19.4.10 Cash Flow Snapshot

The annual cashflow, expressed in million U.S. dollars, is presented in Figure 19.6.

Table 19.7 Summary of annual cash flow, US\$ millions

			Pre-Production								Production											
			YR-3	YR-2	YR-1	YR1	YR2	YR3	YR4	YR5	YR6	YR7	YR8	YR9	YR10	YR11	YR12	YR13	YR14	YR15	YR16-40	
Description	LOM Total	Units	2026	2027	2028	2029	2030	2031	2032	2033	2034	2035	2036	2037	2038	2039	2040	2041	2042	2043	2044-2067	
Assumptions																						
Production Quantity	5,335.0	ST	-	-	-	93.6	130.0	136.5	136.5	136.5	136.5	136.5	136.5	136.5	136.5	136.5	136.5	136.5	136.5	136.5	3,336.9	
Boric Acid Price	\$1,354.6	\$/ST	-	-	-	\$1,273	\$1,266	\$1,234	\$1,305	\$1,353	\$1,360	\$1,364	\$1,364	\$1,364	\$1,364	\$1,364	\$1,364	\$1,364	\$1,364	\$1,364	\$1,364	
Income																						
Revenue	7,227.0	\$M	-	-	-	119.2	164.6	168.4	178.1	184.7	185.6	186.2	186.2	186.2	186.2	186.2	186.2	186.2	186.2	186.2	4,550.9	
Operating Expenditure																						
Variable	(2,122.9)	\$M	-	-	-	(37.2)	(51.7)	(54.3)	(54.3)	(54.3)	(54.3)	(54.3)	(54.3)	(54.3)	(54.3)	(54.3)	(54.3)	(54.3)	(54.3)	(54.3)	(1,327.8)	
Fixed	(1,209.6)	\$M	(3.5)	(3.5)	(5.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(30.3)	(742.5)	
Other (Operating)/Credit	333.2	\$M	-	-	-	1.2	1.6	6.6	8.5	8.9	8.9	8.9	8.9	8.9	8.9	8.9	8.9	8.9	8.9	8.9	217.3	
Total	(2,999.3)	\$M	(3.5)	(3.5)	(5.3)	(66.4)	(80.4)	(78.0)	(76.1)	(75.7)	(75.7)	(75.7)	(75.7)	(75.7)	(75.7)	(75.7)	(75.7)	(75.7)	(75.7)	(75.7)	(1,853.0)	
Working Capital Costs																						
Working Capital Costs	(3.9)	\$M	1.2	13.8	5.7	(25.0)	(2.6)	(0.5)	(1.0)	(0.6)	0.4	(0.5)	-	-	-	0.5	(0.5)	-	-	-	5.2	
Capital Costs																						
Initial	(435.0)	\$M	(10.9)	(178.3)	(245.7)	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	
Sustaining	(39.9)	\$M	-	-	-	-	-	-	-	-	(5.7)	-	-	-	-	(5.7)	-	-	-	-	(28.5)	
Total Capital	(474.8)	\$M	(10.9)	(178.3)	(245.7)	-	-	-	-	-	(5.7)	-	-	-	-	(5.7)	-	-	-	-	(28.5)	
Pre-Tax Cash Flow																						
Pre-Tax Cash Flow	3,749.0	\$M	(13.2)	(168.1)	(245.4)	27.8	81.6	89.9	101.1	108.4	104.6	109.9	110.4	110.4	110.4	105.2	110.0	110.4	110.4	110.4	2,674.6	
Income Tax																						
Income Tax	(1,123.6)	\$M	-	-	-	(2.8)	(12.2)	(14.0)	(17.5)	(19.5)	(18.1)	(20.0)	(20.0)	(20.0)	(20.0)	(31.3)	(33.0)	(33.0)	(33.0)	(33.0)	(796.5)	
After-Tax Cash Flow																						
After-Tax Cash Flow	2,625.4	\$M	(13.2)	(168.1)	(245.4)	25.0	69.5	75.9	83.6	88.9	86.5	89.9	90.5	90.5	90.5	73.9	77.0	77.5	77.5	77.5	1,878.0	

## 20 Adjacent Properties

Elementis operates their hectorite mine adjacent to the west side of the Project. The mine produces hectorite, a specialty clay mineral used in ceramics, cosmetics, and other specialties requiring high viscosity or high thermal stability. While the mine is adjacent to the Project it produces a product that does not compete with 5E.

Land status around the Project area includes the following:

- To the west are the patented and unpatented lands of the Elementis hectorite mine as well as public lands managed by the U.S. Department of Interior, Bureau of Land Management. Both Elementis and BLM land are included within the EIS boundary. While Elementis has placer claims over the 5E deposit, 5E has staked and filed lode claims. 5E has completed extensive diligence with third-party geologists, counsel, and mineral experts and it has been determined that as colemanite is a mudstone with the appropriate claim to establish mineral tenure being a lode claim.
- BLM land is to the north and east of the Project.
- Lands south of the Project area are part of the U.S. Marine Corps Twentynine Palms Marine Base. Figure 3.2 Property Ownership shows the mineral tenure for the project.

## 21 Other Relevant Data and Information

There is currently no other relevant information or data to present.

## 22 Interpretation and Conclusions

This pre-feasibility study provides substantial updates to sections 10, 12, 13, 14, 18, and 19. This report is a work product of 18-months of actual in-situ mining, over 12-months of operating 5E's SSF, comprehensive testing with various OEMs on specific pieces of equipment that have been incorporated into the design, and over 15,000 engineering hours. The LSBF mine plan includes 27 directional wells feeding a chemical plant designed by Fluor with pregnant leach solution at a feed rate of 25.6 short tons per hour with a boric acid head grade of 10.2% weight. The head grade in the plant feed plays a critical role for process control and for the sizing of the plant's equipment, piping and instrumentation. Variations in the in-situ mining conditions can drive a variable range of boric acid head grades with boric acid solubility, HCl concentration and temperature being drivers to head grade. The head grade assumption reflects both what is realistically achievable as demonstrated by the SSF and an optimal value for equipment design to meet the stated production goals of 130,000 short tons of boric acid and achieving a 95.1% recovery rate in the chemical plant. Byproducts produced include gypsum and calcium chloride, with the production rate of gypsum being 129,000 short tons per annum on a dry basis and the projected rate of calcium chloride being 60,000 short tons per annum in solution (38% weight).

Crystallization is a pivotal step in achieving purity and meeting customer specifications and represents a major capital investment due to the complexity and material requirements of the equipment. Kemetco performed a comprehensive metallurgical test program and was critical in further understanding process behavior and optimizing the overall design. The testing confirmed that two-stage crystallization leaves behind too many impurities, necessitating a selective dissolution and recrystallization phase where boric acid slurry is filtered, washed, redissolved, and then recrystallized. This approach enables tighter control over crystal growth and significantly improves product quality. The impurity removal process is another critical component, particularly for managing magnesium levels, which are highly pH dependent. Precise control of sequential pH adjustments is essential to selectively precipitating and removing impurities while minimizing boron losses and this step is vital for maintaining the integrity of the in-situ mining process as recycled process streams are re-injected into the wellfield. Inadequate removal of impurities could negatively impact boron leaching efficiencies and this purification step supports the downstream process and refinement of the byproducts.

Given the high temperature and aridity of the local climate, the most cost-effective approach to concentrate the calcium rich return brine is by maximizing the use of evaporation ponds.

The total capital estimate for the project is \$435 million and economic analysis yields an NPV of \$724.8 million and project IRR of 19.2%. Based on the economic analysis, mineral resources and mineral reserves have been estimated and reported using a cut-off grade of 2.0%  $B_2O_3$ . Measured, Indicated, and Inferred resources for the Project total 135.8 Mt of ore, 18.1 Mt of boric acid and 0.2 Mt of lithium carbonate equivalent. Proven reserves total 1.4 Mt of  $H_3BO_3$  and probable reserves total 4.0 short tons of  $H_3BO_3$ .

5E has an established mineral holding through ownership of fee lands and unpatented placer and lode claims. The property has undergone prior exploration primarily conducted in the 1980's along with more recent drilling conducted in 2017 which validated previous exploration and expanded known mineral occurrences. Drilling completed on the Project is sufficient for the delineation of a mineral resource estimate and economic analysis has provided justification for establishing mineral reserves.

Geologic interpretation of the deposit describes mineralization as lacustrine evaporite sediments containing colemanite, a hydrated calcium borate mineral. The deposit also contains appreciable quantities of lithium. Geologic modeling based on drilling and sampling results depicts an elongate deposit of lacustrine evaporite sediments containing colemanite. The deposit is approximately 2.1 mi. long by 0.6 mi. wide, and ranges in thickness from 70 to 262 ft. with mineralization that has been defined in four distinct horizons defined by changes in lithology and  $B_2O_3$  analyses.

In conclusion, there are reasonable prospects for economic extraction for the mineral resources and reserves estimated and presented in this pre-feasibility study. 5E has been diligent in validating the work completed by the previous operators and further expanding the size and classification assurance of the deposit. Current and previous evaluations of mining methods indicate a deposit well suited for ISL solution mining as a preferred method for economic extraction. Progression to FEL-3 or FEED engineering will further define the accuracy and optimization of the capital cost estimates for the chemical processing plant and some additional exploration and in-fill drilling can further bolster the resource and reserve. Using the samples produced from the SSF, 5E is positioned to secure bankable offtake agreements for commercialization. Once these steps are completed, the Company is well positioned to update this prefeasibility study to a feasibility study.

## 23 Recommendations

The QP's have made the following recommendations:

- Stage-gate to FEL-3 engineering. FEL-3 engineering and relevant required testing are estimated to cost approximately \$6.6M. Additional details of the work to be performed include the following:
  - Further test work to optimize the crystallizer design is required for optimizing crystal growth and particle size distribution which are specification requirements. Factors such as residence time, slurry density, supersaturation, type of cooling, cooling rate, level of agitation, and mixing rate, should all be evaluated and considered for controlling crystal size.
  - Completion of additional locked cycle testing be conducted on the crystallization process during FEL-3 to better simulate steady-state operation and assess long-term process stability. This test will help identify potential impurity buildup and equipment fouling to validate product quality over multiple cycles, and support more accurate mass balance and equipment design decisions.
  - The harsh nature of the pregnant leach solution necessitates that a robust and quantitative materials of construction coupon testing program be completed. This is critical to ensure that compatible materials are selected for equipment, piping, and instrumentation. Improper material selection may cause safety, production, and/or quality issues.



- Further test work on fluid and slurry flow characteristics including density (carrier fluid and solids for slurries), particle size distributions, solids weight percents, and viscosity.
- Completion of a detailed heat integration study and an optimized water balance to help to reduce both capital and operating expenditures as well as reduction in the environmental resource requirements.
- More detailed studies on environmental impact should be performed in the next engineering phase, specifically emissions (gaseous and particulate), scrubber efficiencies, gypsum stockpiles, wastewater discharge, solids waste handling (clay and metal impurities), biodiversity and habitat impact.
- Completion of a Reliability, Availability, and Maintainability (RAM) analysis to evaluate the long-term performance and operational efficiency of critical systems. This analysis helps identify potential bottlenecks, optimize maintenance strategies, and improve overall system uptime, ultimately supporting more accurate cost estimates and design decisions.
- Investigate setting up purchasing agreements with reagent suppliers to ensure that there will be adequate availability and that the costs are fully understood.
- A thickener for the PLS feed to the plant is not considered due to the low solids content seen in the PLS feed to the SSF. It is recommended to perform test work to confirm the solids content that will come from the wellfield.
- Continued operation of the SSF to gain a more in-depth understanding of the performance of the horizontal wells, including artificial lift (jet pump) and integrating a dedicated steam injection well. Through operation of existing horizontal and directional wells, confirm residence time and length of injection – recovery cycles with reconciliation to commercial recovery rates. Injection cycle volume should target volume required to produce desired feed rate to LSBF plus contingency volume required due to mining efficiency and void space created by previous cycles. Injection rates need to balance with expected residence time to achieve desired PLS concentration versus expected recovery production rates. Cost is estimated at \$1.6 million.

## 24 References

5E SSF high frequency wellfield instrumentation results via SSF DCS

5E SSF Injection Schedule and Results

5E July 2025 Horizontal Drill Program ICP results

Ardent Technologies, Test Work Report – Consolidated Ardent Testing Data

Bartlett, R.W., 1998. Solution Mining: Leaching and Fluid Recovery of Materials, Second Edition, Routledge Publishing.

Confluence Water Resources, LLC 2019. 2019 Fault B Program Results, Technical Report, March 2019.

Confluence Water Resources, LLC 2022. Shallow Groundwater Characterization Report Mining Block 2 Near Pisgah Fault, June 2022.

Confluence Water Resources, LLC 2023. Results from OW-3A and MW3B Hydraulic Testing, Technical Memorandum, March 2023.

Core Laboratories, Inc, 1981. Boron Analysis of Core Leachings Well SMT-1, San Bernadino County by D. Burnett, July 1981.

Fort Cady California Corporation, 2019. Revised 2019 Mining/Land Reclamation Plan and Plan of Operations. Revised April 2019.

Haliburton Micro-deformation instrumentation results

Hazen Research, Inc, 2019. Recovery and Purification of Boric Acid from Colemanite Leach Liquor using Solvent Extraction – Report 12574, Sep. 2019.

Hydro-Engineering, 1996. Aquifer Characteristics and potential well field geometry, by G Hoffman & E Sandberg, Feb. 1996.

Kemetco Research, Inc., Test Work Report – Scoping Boric Acid Production Testing: T0903 Report

Kline Preliminary Market Study, June 2025

Simon Hydro-Search, 1993. Fort Cady Mineral Corporation Solution Mining Project Feasibility Report, San Bernardino County, California. Prepared for Southern California Edison by Simon Hydro-Search. October 22, 1993.

Swenson Technology, Inc. 2019. Test Report – Crystallization of Boric Acid by J Majors, April 2019.

Wilkinson & Krier, 1985. Geological Summary – Duval Corp. internal review, by P Wilkinson and Krier N, Jan 1985.

## 25 Reliance on Information Provided by the Registrant

SE has provided the external QP's with a variety of materials for the preparation of this report. These materials include the following:

- Drilling records from the 2017 drilling program completed by APBL, which includes drilling locations, drill logs, sampling records, analytical results/certificates, geophysical logs, and core photos.
- Drilling records from Duval and FCMC, which include drill logs, sampling records, analytical results/certificates, and geophysical logs.
- Historical drilling maps and testing records.
- Third-party laboratory reports related to process test work based on synthetic brine.
- Testing performed by Kemetco on crystallization.
- Commodity pricing forecasts and a preliminary market study performed by Kline.
- Historic solution mine information from MSME and Duval.